### Compressible Flow - TME085 Lecture 4

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## Chapter 3 One-Dimensional Flow



## Addressed Learning Outcomes

- 4 **Present** at least two different formulations of the governing equations for compressible flows and **explain** what basic conservation principles they are based on
- 5 Explain how thermodynamic relations enter into the flow equations
- 8 Derive (marked) and apply (all) of the presented mathematical formulae for classical gas dynamics
  - 1D flow with heat addition\*
  - d 1D flow with friction\*

inviscid flow with friction?!

#### Roadmap - One-dimensional Flow



# Chapter 3.8 One-Dimensional Flow with Heat Addition



Pipe flow:

- no friction
- 1D steady-state  $\Rightarrow$  all variables depend on x only
- q is the amount of heat per unit mass added between 1 and 2
- analyze by setting up a control volume between station 1 and 2

$$\rho_1 u_1 = \rho_2 u_2$$

$$\rho_1 u_1^2 + \rho_1 = \rho_2 u_2^2 + \rho_2$$

$$h_1 + \frac{1}{2} u_1^2 + \mathbf{q} = h_2 + \frac{1}{2} u_2^2$$

Valid for all gases! General gas  $\Rightarrow$  Numerical solution necessary Calorically perfect gas  $\Rightarrow$  analytical solution exists

Calorically perfect gas ( $h = C_{\rho}T$ ):

$$C_{\rho}T_{1} + \frac{1}{2}u_{1}^{2} + \mathbf{q} = C_{\rho}T_{2} + \frac{1}{2}u_{2}^{2}$$
$$\mathbf{q} = \left(C_{\rho}T_{2} + \frac{1}{2}u_{2}^{2}\right) - \left(C_{\rho}T_{1} + \frac{1}{2}u_{1}^{2}\right)$$
$$C_{\rho}T_{0} = C_{\rho}T + \frac{1}{2}u^{2} \Rightarrow$$
$$\mathbf{q} = C_{\rho}(T_{02} - T_{01})$$

*i.e.* heat addition increases T<sub>o</sub> downstream

Momentum equation:

$$p_2 - p_1 = \rho_1 u_1^2 - \rho_2 u_2^2$$

$$\left\{ \rho u^2 = \rho a^2 M^2 = \rho \frac{\gamma \rho}{\rho} M^2 = \gamma \rho M^2$$

$$p_2 - \rho_1 = \gamma \rho_1 M_1^2 - \gamma \rho_2 M_2^2 \Rightarrow$$

$$\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$$

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Ideal gas law:

$$T = \frac{\rho}{\rho R} \Rightarrow \frac{T_2}{T_1} = \frac{\rho_2}{\rho_2 R} \frac{\rho_1 R}{\rho_1} = \frac{\rho_2}{\rho_1} \frac{\rho_1}{\rho_1}$$

Continuity equation:

$$\rho_1 U_1 = \rho_2 U_2 \Rightarrow \frac{\rho_1}{\rho_2} = \frac{U_2}{U_1}$$

$$\frac{M_2}{M_1} = \frac{M_2 a_2}{M_1 a_1} = \frac{\sqrt{\gamma R T_2}}{\sqrt{\gamma R T_1}} \Rightarrow \frac{\rho_1}{\rho_2} = \frac{M_2}{M_1} \sqrt{\frac{T_2}{T_1}}$$
$$\frac{T_2}{T_1} = \left(\frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}\right)^2 \left(\frac{M_2}{M_1}\right)^2$$

Calorically perfect gas, analytic solution:

$$\frac{T_2}{T_1} = \left[\frac{1+\gamma M_1^2}{1+\gamma M_2^2}\right]^2 \left(\frac{M_2}{M_1}\right)^2$$

$$\frac{\rho_2}{\rho_1} = \left[\frac{1+\gamma M_2^2}{1+\gamma M_1^2}\right] \left(\frac{M_1}{M_2}\right)^2$$

$$\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$$

Calorically perfect gas, analytic solution:

$$\frac{D_{O_2}}{D_{O_1}} = \left[\frac{1+\gamma M_1^2}{1+\gamma M_2^2}\right] \left(\frac{1+\frac{1}{2}(\gamma-1)M_2^2}{1+\frac{1}{2}(\gamma-1)M_1^2}\right)^{\overline{\gamma-1}} \\
\frac{T_{O_2}}{T_{O_1}} = \left[\frac{1+\gamma M_1^2}{1+\gamma M_2^2}\right] \left(\frac{M_2}{M_1}\right)^2 \left(\frac{1+\frac{1}{2}(\gamma-1)M_2^2}{1+\frac{1}{2}(\gamma-1)M_1^2}\right)^{\frac{\gamma}{\gamma-1}}$$

#### Initially subsonic flow (M < 1)

- ► the Mach number, *M*, increases as more heat (per unit mass) is added to the gas
- ► for some limiting heat addition  $q^*$ , the flow will eventually become sonic M = 1

#### Initially supersonic flow (M > 1)

- the Mach number, *M*, decreases as more heat (per unit mass) is added to the gas
- for some limiting heat addition  $q^*$ , the flow will eventually become sonic M = 1

Note: The (\*) condition in this context is not the same as the "critical" condition discussed for isentropic flow!!!

$$\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$$

Calculate the ratio between the pressure at a specific location in the flow p and the pressure at sonic conditions  $p^*$ 

$$p_1 = p, M_1 = M, p_2 = p^*$$
, and  $M_2 = 1$ 

$$\frac{p^*}{p} = \frac{1 + \gamma M^2}{1 + \gamma}$$

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$$\frac{T}{T^*} = \left[\frac{1+\gamma}{1+\gamma M^2}\right]^2 M^2 \qquad \qquad \frac{\rho_0}{\rho_0^*} = \left[\frac{1+\gamma}{1+\gamma M^2}\right] \left(\frac{2+(\gamma-1)M^2}{(\gamma+1)}\right)^2$$
$$\frac{\rho}{\rho^*} = \left[\frac{1+\gamma M^2}{1+\gamma}\right] \left(\frac{1}{M^2}\right) \qquad \qquad \frac{T_0}{T_0^*} = \frac{(\gamma+1)M^2}{(1+\gamma M^2)^2} (2+(\gamma-1)M^2)$$
$$\frac{\rho}{\rho^*} = \frac{1+\gamma}{1+\gamma M^2}$$
see Table A.3

 $\frac{\gamma}{\gamma-1}$ 

#### Amount of heat per unit mass needed to choke the flow:

$$\boldsymbol{q}^* = C_{\rho}(\boldsymbol{T}_{o}^* - \boldsymbol{T}_{o}) = C_{\rho}\boldsymbol{T}_{o}\left(\frac{\boldsymbol{T}_{o}^*}{\boldsymbol{T}_{o}} - 1\right)$$



#### Rayleigh curve



see Figure 3.13

And now, the million-dollar question ...



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Removing heat seems to reduce the entropy. Isn't that a violation of the second law of thermodynamics?!



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Answer: if the heat source or sink would have been included in the system studied, the system entropy would increase both when adding and removing heat.

- M < 1: Adding heat will
- ▶ increase M
- ▶ decrease *p*
- increase  $T_o$
- decrease  $p_o$
- increase s
- increase u
- decrease  $\rho$

#### Flow loss - not isentropic process

#### M > 1: Adding heat will

- ► decrease M
- ► increase p
- increase  $T_o$
- decrease p<sub>o</sub>
- ▶ increase s
- decrease u
- increase  $\rho$

Relation between added heat per unit mass (q) and heat per unit surface area and unit time ( $\dot{q}_{wall}$ )



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#### Roadmap - One-dimensional Flow



# Chapter 3.9 One-Dimensional Flow with Friction



Pipe flow:

- adiabatic (q = 0)
- cross section area A is constant
- average all variables in each cross-section  $\Rightarrow$  only x-dependence
- analyze by setting up a control volume between station 1 and 2

Wall-friction contribution in momentum equation

$$\iint_{\partial\Omega} \tau_w dS = b \int_0^L \tau_w dx$$

where *L* is the tube length and *b* is the circumference

$$\rho_{1}u_{1} = \rho_{2}u_{2}$$

$$\rho_{1}u_{1}^{2} + \rho_{1} - \frac{4}{D}\int_{0}^{L}\tau_{w}dx = \rho_{2}u_{2}^{2} + \rho_{2}$$

$$h_{1} + \frac{1}{2}u_{1}^{2} = h_{2} + \frac{1}{2}u_{2}^{2}$$
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or

 $\tau_{\rm W}$  varies with the distance x and thus complicating the integration

Solution: let L shrink to dx and we end up with relations on differential form

$$d(\rho u^2 + \rho) = -\frac{4}{D}\tau_w dx$$

$$\frac{d}{dx}(\rho u^2 + \rho) = -\frac{4}{D}\tau_w$$

From the continuity equation we get

$$\rho_1 u_1 = \rho_2 u_2 = \text{const} \Rightarrow \frac{d}{dx}(\rho u) = 0$$

Writing out all terms in the momentum equation gives

$$\frac{d}{dx}(\rho u^2 + p) = \rho u \frac{du}{dx} + u \underbrace{\frac{d}{dx}(\rho u)}_{=0} + \frac{dp}{dx} = -\frac{4}{D}\tau_w$$

and thus

$$\rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{4}{D} \tau_{w}$$

Common approximation for  $\tau_W$ :

$$\tau_{W} = f \frac{1}{2} \rho u^{2} \Rightarrow \rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{2}{D} \rho u^{2} f$$

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Energy conservation:

$$h_{o_1} = h_{o_2} \Rightarrow \frac{d}{dx} h_o = 0$$



Summary:

$$\frac{d}{dx}(\rho u) = 0$$

$$\rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{2}{D}\rho u^2 f$$

$$\frac{d}{dx}h_0 = 0$$

Valid for all gases!

General gas  $\Rightarrow$  Numerical solution necessary

Calorically perfect gas  $\Rightarrow$  analytical solution exists (for constant *f*)

Calorically perfect gas:

$$\int_{x_1}^{x_2} \frac{4f}{D} dx = \left[ -\frac{1}{\gamma M^2} - \frac{\gamma + 1}{2\gamma} \ln \left( \frac{M^2}{1 + \frac{\gamma - 1}{2} M^2} \right) \right]_{M_1}^{M_2}$$
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Calorically perfect gas:

$$\frac{T_2}{T_1} = \frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2}$$

$$\frac{\rho_2}{\rho_1} = \frac{M_1}{M_2} \left[ \frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2} \right]^{1/2}$$

$$\frac{\rho_2}{\rho_1} = \frac{M_1}{M_2} \left[ \frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2} \right]^{-1/2}$$

$$\frac{\rho_{o_2}}{\rho_{o_1}} = \frac{M_1}{M_2} \left[ \frac{2 + (\gamma - 1)M_2^2}{2 + (\gamma - 1)M_1^2} \right]^{\frac{\gamma + 1}{2(\gamma - 1)}}$$

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#### Initially subsonic flow ( $M_1 < 1$ )

- $M_2$  will increase as L increases
- ► for a critical length  $L^*$ , the flow at point 2 will reach sonic conditions, *i.e.*  $M_2 = 1$

#### Initially supersonic flow ( $M_1 > 1$ )

M<sub>2</sub> will decrease as *L* increases for a critical length  $L^*$ , the flow at point 2 will reach sonic conditions, *i.e.*  $M_2 = 1$ 

Note: The (\*) condition in this context is not the same as the "critical" condition discussed for isentropic flow!!!

$$\frac{T}{T^*} = \frac{(\gamma+1)}{2+(\gamma-1)M^2}$$
$$\frac{\rho}{\rho^*} = \frac{1}{M} \left[ \frac{\gamma+1}{2+(\gamma-1)M^2} \right]^{1/2}$$
$$\frac{\rho}{\rho^*} = \frac{1}{M} \left[ \frac{2+(\gamma-1)M^2}{\gamma+1} \right]^{1/2}$$
$$\frac{\rho_o}{\rho_o^*} = \frac{1}{M} \left[ \frac{2+(\gamma-1)M^2}{\gamma+1} \right]^{\frac{\gamma+1}{2(\gamma-1)}}$$

see Table A.4

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and

$$\int_0^{L^*} \frac{4f}{D} dx = \left[ -\frac{1}{\gamma M^2} - \frac{\gamma + 1}{2\gamma} \ln \left( \frac{M^2}{1 + \frac{\gamma - 1}{2} M^2} \right) \right]_M^1$$

where  $L^*$  is the tube length needed to change current state to sonic conditions

Let  $\overline{f}$  be the average friction coefficient over the length  $L^* \Rightarrow$ 

$$\frac{4\bar{t}\boldsymbol{L}^*}{D} = \frac{1-M^2}{\gamma M^2} + \frac{\gamma+1}{2\gamma} \ln\left(\frac{(\gamma+1)M^2}{2+(\gamma-1)M^2}\right)$$

Turbulent pipe flow  $ightarrow ar{t} \sim 0.005$  (Re  $> 10^5$  , roughness  $\sim 0.001$ D)



#### M < 1: Friction will

- ▶ increase M
- ▶ decrease *p*
- ▶ decrease T
- decrease p<sub>o</sub>
- increase s
- increase u
- decrease  $\rho$

#### Flow loss - non-isentropic flow

#### M > 1: Friction will

- ► decrease M
- ▶ increase *p*
- ► increase T
- decrease  $p_o$
- increase s
- ► decrease *u*
- increase  $\rho$

#### Roadmap - One-dimensional Flow

