

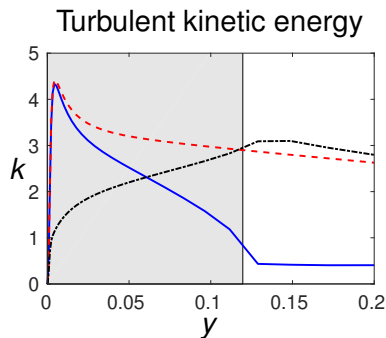
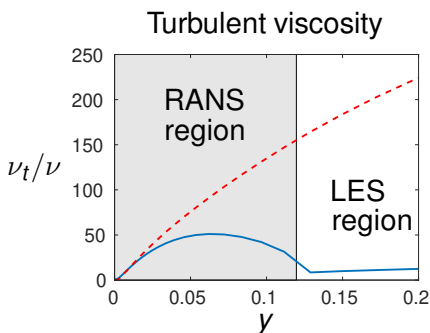
S-ZDES: ZONAL DETACHED EDDY SIMULATION COUPLED WITH STEADY RANS IN THE WALL REGION

Lars Davidson, www.tfd.chalmers.se/~lada

DES — DETACHED-EDDY SIMULATIONS

● Problem:

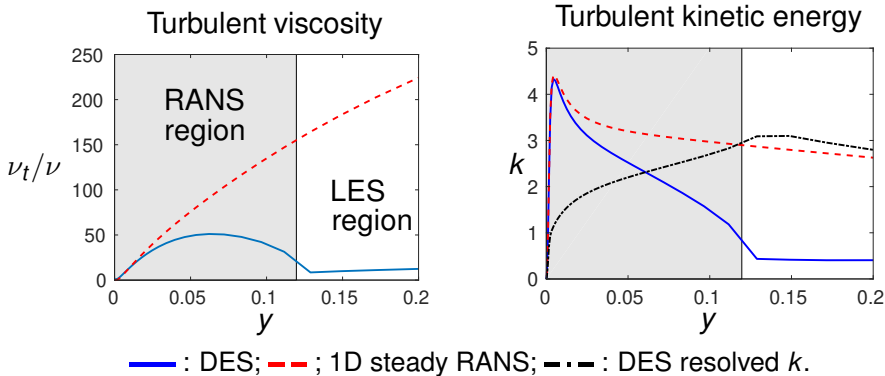
- ▶ the flow in the RANS region is highly unsteady (i.e. **URANS**)
- ▶ this means that RANS turbulence models (developed for **steady** flow) are not accurate



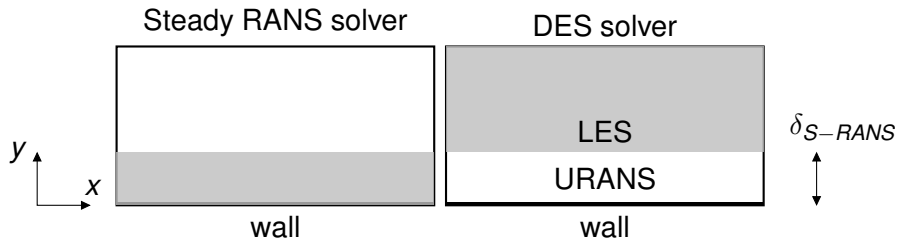
— : DES; - - - : 1D steady RANS; - - - : DES resolved k .

DES — DETACHED-EDDY SIMULATIONS

- Problem:
 - ▶ the flow in the RANS region is highly unsteady (i.e. **URANS**)
 - ▶ this means that RANS turbulence models (developed for **steady** flow) are not accurate
- Solution:
 - ▶ solve the **steady** equations in the RANS region



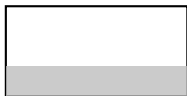
TWO SOLVERS IN THE ENTIRE DOMAIN



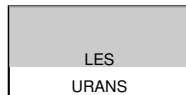
Grey color indicates the solver that drives the flow

DRIFT TERMS ARE ADDED IN WHITE REGIONS

Steady RANS solver



DES solver



$$S_i^{RANS} = \frac{\langle v_i^{LES} \rangle_T - \langle v_i^{RANS} \rangle_T}{\Delta t}$$

$$S_i^{LES} = \frac{\langle v_i^{RANS} \rangle_T - \langle \bar{v}_i^{LES} \rangle_T}{\Delta t},$$

Subscript T indicates integration over time T

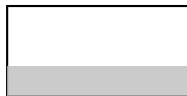
$$\langle \phi(t) \rangle_T = \frac{1}{T} \int_{-\infty}^t \phi(\tau) \exp(-(t-\tau)/T) d\tau \Rightarrow$$

$$\langle \phi \rangle_T^t \equiv \langle \phi \rangle_T = a \langle \phi \rangle_T^{t-\Delta t} + (1-a) \phi^t$$

$$a = \exp(-\Delta t/T).$$

WHY IS THE RANS SOLVER STEADY?

Steady RANS solver



$$S_i^{RANS} = \frac{\langle v_i^{RANS} \rangle_T - \langle v_i^{RANS} \rangle_{T-\Delta t}}{\Delta t}$$

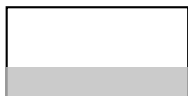
- The RANS solver is called every 10^{th} timestep (can probably be called less often)
- The solution in the RANS solver stays steady when the drift term, S_i^{RANS} is steady (constant in time)
- If the integration time T is too small, there will slightly different steady RANS flow every 10^{th} timestep
 - ▶ Solution: make the steady RANS solver unsteady but use the large timestep, i.e. $10\Delta t_{DES}$

PREVIOUS WORK

- The present method is similar to those in [1, 2, 3]. The main differences are that
 - ▶ In [1, 3] they use one **additional** drift terms in the LES momentum equations to control resolved Reynolds stresses
 - ▶ They include drift terms also in the k and ε equations [1] or the k equation [3].
 - ▶ In [1, 3] they include **five** tuning constants in all drift terms. I have **one** (T).

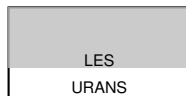
TURBULENCE MODELS

Steady RANS solver



- EARSM (Explicit Algebraic Stress Model) [4] coupled to Wilcox $k - \omega$ model [5]

DES solver



- DES $k - \omega$ model
- Lengthscale in dissipation term of the k eq. is taken from the IDDES model [6, 7]

RANS and DES turbulence models

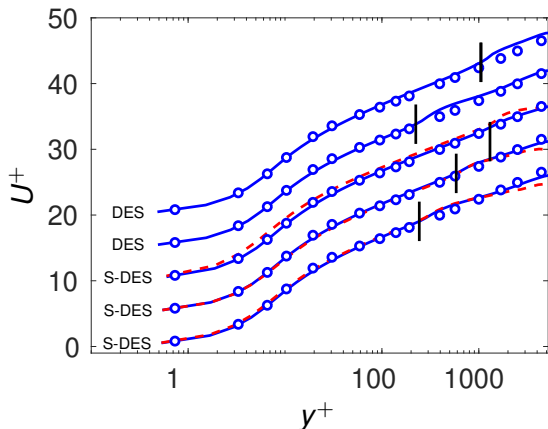
NUMERICAL METHOD: CALC-LES & CALC-BFC

- CALC-LES [8]: DES solver
 - ▶ Incompressible finite volume method
 - ▶ Pressure-velocity coupling treated with fractional step
 - ▶ Central differencing scheme for momentum eqns
 - ▶ Hybrid 1st order upwind/2nd order central scheme k & ω eqns.
 - ▶ 2nd-order Crank-Nicholson for time discretization
- CALC-BFC [9]: RANS solver, called every 10th timestep
 - ▶ Incompressible finite volume method
 - ▶ SIMPLEC
 - ▶ MUSCL: 2nd order bounded upwind scheme for momentum eqns
 - ▶ Hybrid 1st order upwind/2nd order central scheme k & ω eqns.

FIRST TEST CASE: CHANNEL FLOW

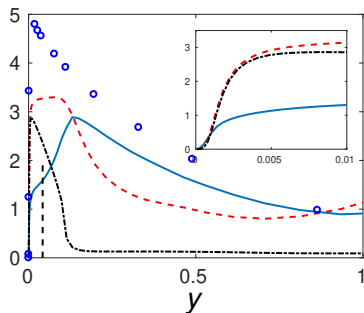
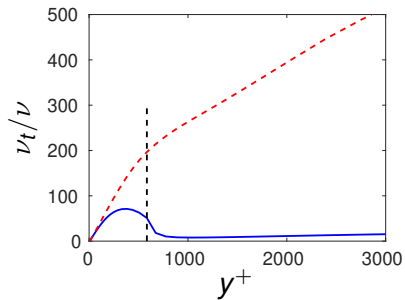
- Reynolds number is $Re_\tau = 5200$.
- A $32 \times 96 \times 32$ mesh is used
- $x_{max} = 3.2$, $z_{max} = 1.6$, 15% stretching in y direction

CHANNEL FLOW: VELOCITY



$T = 50\delta/U_b$ — : DES; - - : RANS; ○ : DNS. Vertical black lines show DES interface.

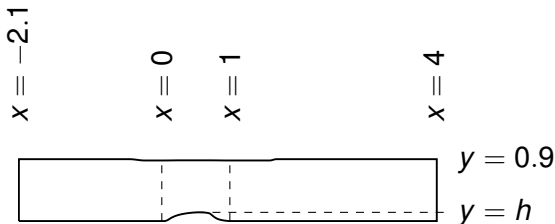
CHANNEL FLOW: TURBULENT QUANTITIES



○ : DNS [10]; - - - : DES, resolved turbulence

— : DES solver; - - - : RANS solver. Vertical black lines show DES interface.

SECOND TEST CASE: HUMPS FLOW



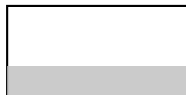
The domain of the hump. $z_{max} = 0.2$.

- The Reynolds number of the hump flow is $Re_c = 936\,000$.
- The mesh has $386 \times 120 \times 32$ cells (x, y, z)
- Grid from NASA workshop.¹
- Inlet is located at $x = -2.1$ and the outlet at $x = 4.0$,

¹https://turbmodels.larc.nasa.gov/nasahump_val.html

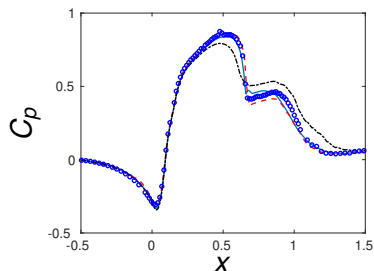
HUMP FLOW: NUMERICAL ISSUES

Steady RANS solver

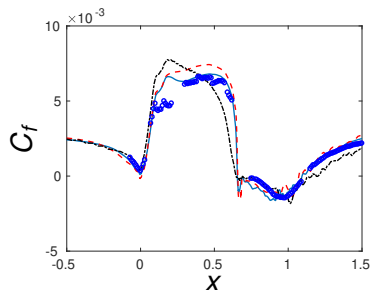


- The drift term in the RANS solver in the LES region (white region) causes unphysical oscillations in the skinfriction
- The problem was traced to the source term in the pressure correction equation, the continuity error \dot{m}
- Hence, \dot{m} was set to zero in the LES region.
- As a consequence, the RANS velocity field is driven by the drift term, but the RANS pressure is not correct in this region

HUMP FLOW: C_p & C_f



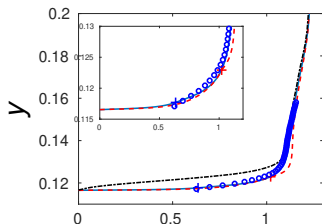
(A) Pressure coefficient.



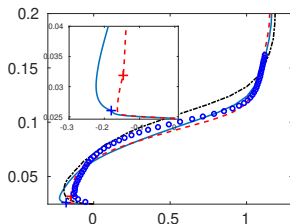
(B) Skinfriction.

$T = 20h/U_{in}$. — : S-DES, $j_0 = 33$; - - : S-DES, $j_0 = 53$; ··· : DES

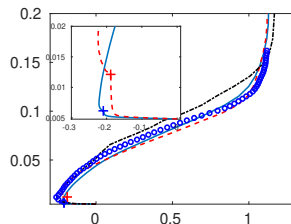
HUMP FLOW: VELOCITIES



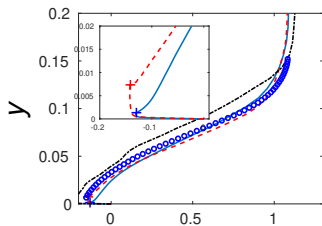
(A) $x = 0.65$



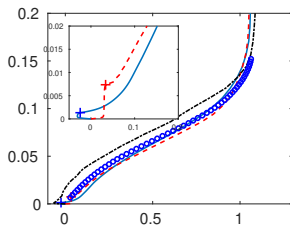
(B) $x = 0.8$



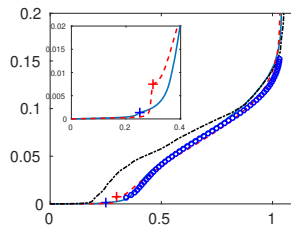
(C) $x = 0.9$



(D) $x = 1.0$



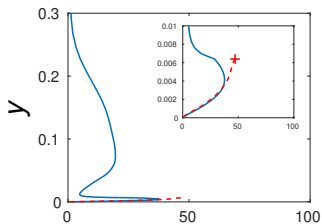
(E) $x = 1.1$



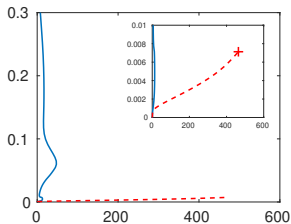
(F) $x = 1.3$

— : S-ZDES, $j_0 = 33$; - - : S-ZDES, $j_0 = 53$; ··· : DES; ○ : exp [11, 12];
+, + : DES interface.

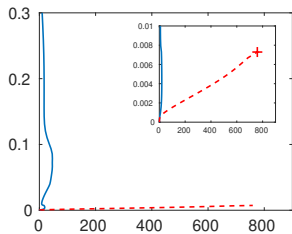
TURBULENT VISCOSITY (EARSM). S-ZDES, $j_0 = 53$



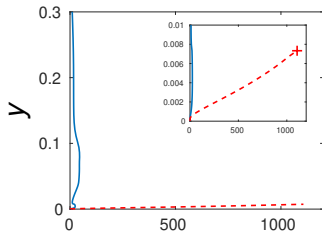
(A) $x = 0.65$



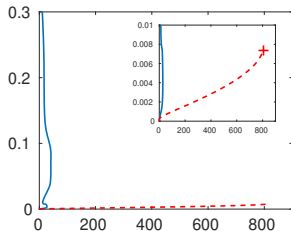
(B) $x = 0.8$



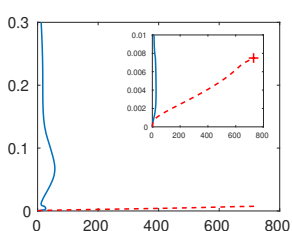
(C) $x = 0.9$



(D) $x = 1.0$



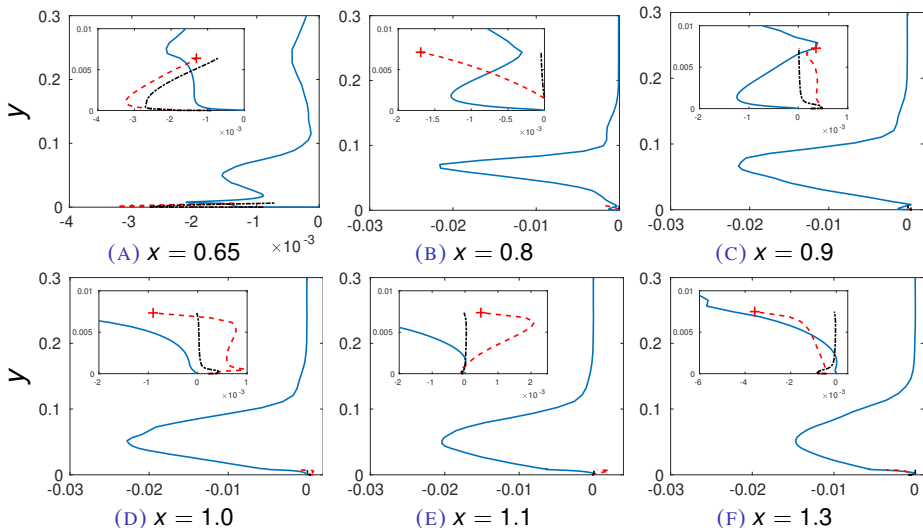
(E) $x = 1.1$



(F) $x = 1.3$

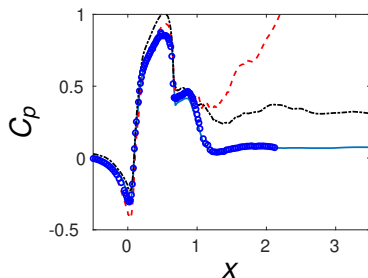
— : DES solver; - - : RANS solver; + : DES interface.

HUMP FLOW: SHEAR STRESSES. S-ZDES, $j_0 = 53$



— : DES solver, resolved; - - - : RANS solver; - · - · : DES solver, modeled.

HUMP FLOW: WRONG p IN RANS REGION



Pressure coefficient. — : LES; - - : RANS, $j_0 = 53$; - - - : RANS, $j_0 = 33$

CONCLUSIONS

- A new **steady** RANS coupled to **DES (S-ZDES)** is proposed.
- Very good results . . .
- but the hump results are maybe/probably contaminated by a numerical fix
- Drawback: it is dependent on the **lower limit** of integration time, T for the hump flow
 - ▶ $T = 10h/U_{in}$ too small (h is hump height)
 - ▶ $T = 20$ and 50 give identical results
 - ▶ For $T = 100$ we must more than double developing+sampling time to $345 + 345$ ($7.3 + 7.3$ throughflow times)

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