

LARGE EDDY SIMULATION OF HEAT TRANSFER IN  
BOUNDARY LAYER AND BACKSTEP FLOW USING  
PANS [4]  
LARS DAVIDSON

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## PANS LOW REYNOLDS NUMBER MODEL [7]

$$\frac{\partial k_u}{\partial t} + \frac{\partial(k_u U_j)}{\partial x_j} = \frac{\partial}{\partial x_j} \left[ \left( \nu + \frac{\nu_u}{\sigma_{ku}} \right) \frac{\partial k_u}{\partial x_j} \right] + (P_u - \varepsilon_u)$$

$$\frac{\partial \varepsilon_u}{\partial t} + \frac{\partial(\varepsilon_u U_j)}{\partial x_j} = \frac{\partial}{\partial x_j} \left[ \left( \nu + \frac{\nu_u}{\sigma_{\varepsilon u}} \right) \frac{\partial \varepsilon_u}{\partial x_j} \right] + C_{\varepsilon 1} P_u \frac{\varepsilon_u}{k_u} - C_{\varepsilon 2}^* \frac{\varepsilon_u^2}{k_u}$$

$$\nu_u = C_\mu f_\mu \frac{k_u^2}{\varepsilon_u}, C_{\varepsilon 2}^* = C_{\varepsilon 1} + \frac{f_k}{f_\varepsilon} (C_{\varepsilon 2} f_2 - C_{\varepsilon 1}), \sigma_{ku} \equiv \sigma_k \frac{f_k^2}{f_\varepsilon}, \sigma_{\varepsilon u} \equiv \sigma_\varepsilon \frac{f_k^2}{f_\varepsilon}$$

$C_{\varepsilon 1}$ ,  $C_{\varepsilon 2}$ ,  $\sigma_k$ ,  $\sigma_\varepsilon$  and  $C_\mu$  same values as [1].  $f_\varepsilon = 1$ .  $f_2$  and  $f_\mu$  read

$$f_2 = \left[ 1 - \exp\left(-\frac{y^*}{3.1}\right) \right]^2 \left\{ 1 - 0.3 \exp\left[-\left(\frac{R_t}{6.5}\right)^2\right] \right\}$$

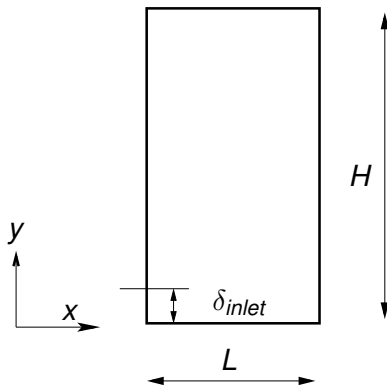
$$f_\mu = \left[ 1 - \exp\left(-\frac{y^*}{14}\right) \right]^2 \left\{ 1 + \frac{5}{R_t^{3/4}} \exp\left[-\left(\frac{R_t}{200}\right)^2\right] \right\}$$

- Baseline model:  $f_k = 0.4$ .

# NUMERICAL METHOD

- Incompressible finite volume method
- Pressure-velocity coupling treated with fractional step
- Differencing scheme for momentum eqns:
  - ▶ 95%  $2^{nd}$  order **central** and 5%  $2^{nd}$  order **upwind** differencing scheme (baseline) **OR**
  - ▶ 100%  $2^{nd}$  order **central** differencing
- Hybrid **1<sup>st</sup> order upwind**/ $2^{nd}$  order central scheme  $k$  &  $\varepsilon$  eqns.
- **$2^{nd}$ -order** Crank-Nicholson for time discretization

# BOUNDARY LAYER FLOW: DOMAIN

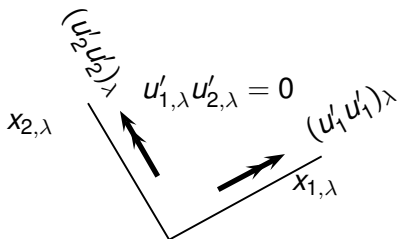


- Inlet:  $\delta_{inlet} = 1$  (covered by 45 cells),  $Re_{\theta} = 3600$ ,  $U_{in} = \rho = 1$ .  
Stretching 1.12 up to  $y/\delta \simeq 1$ .
- Domain:  $L/\delta_{in} = 3.2$ ,  $H/\delta_{in} = 15.6$ ,  $Z_{max} = 1.5\delta_{in}$
- Resolution:  $\Delta z_{in}^+ \simeq 27$ ,  $\Delta x_{in}^+ \simeq 54$
- Grid:  $66 \times 96 \times 64$  ( $x, y, z$ )

# ANISOTROPIC SYNTHETIC FLUCTUATIONS: I [3, 2, 5]

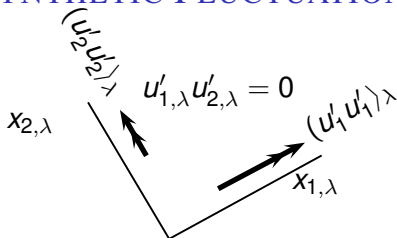
- Prescribe an homogeneous Reynolds tensor,  $\overline{u_i u_j}$  (here from DNS)
- 
-

# ANISOTROPIC SYNTHETIC FLUCTUATIONS: I [3, 2, 5]



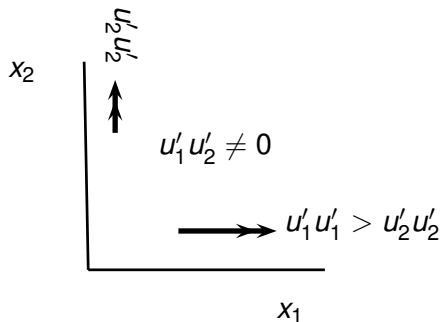
- Prescribe an homogeneous Reynolds tensor,  $\overline{u_i u_j}$  (here from DNS)
- isotropic fluctuations in principal directions,  $(u'_1 u'_1)_\lambda = (u'_2 u'_2)_\lambda$ ,  $u'_{1,\lambda} u'_{2,\lambda} = 0$
-

# ANISOTROPIC SYNTHETIC FLUCTUATIONS: I [3, 2, 5]



- Prescribe an homogeneous Reynolds tensor,  $\overline{u_i u_j}$  (here from DNS)
- isotropic fluctuations in principal directions,  $(u'_1 u'_1)_\lambda = (u'_2 u'_2)_\lambda$ ,  $u'_{1,\lambda} u'_{2,\lambda} = 0$
- re-scale the normal components,  $(u'_1 u'_1)_\lambda > (u'_2 u'_2)_\lambda$ , using the eigenvalues  $u'_{1,\lambda} u'_{2,\lambda} = 0$

# ANISOTROPIC SYNTHETIC FLUCTUATIONS: II



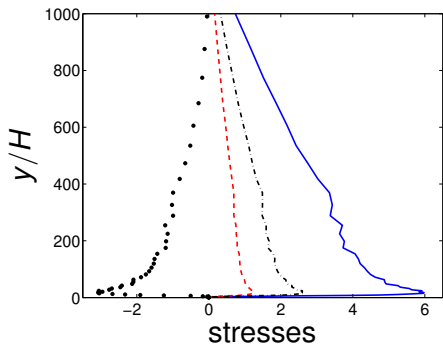
- Transform from  $(x_{1,\lambda}, x_{2,\lambda})$  to  $(x_1, x_2)$
- $\frac{u_1'^2}{u_2'^2} = 23, \frac{u_1'^2}{u_3'^2} = 5$  from  $(u_1' u_1')_{peak}$  in DNS channel flow,  $Re_\tau = 500$



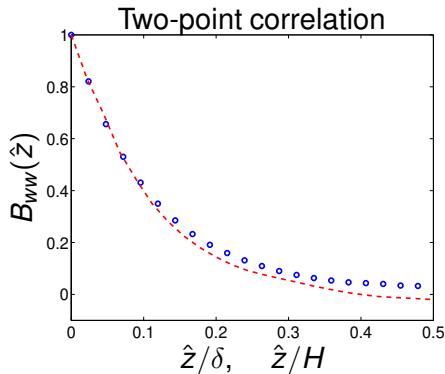
## INLET CONDITIONS FOR $k_u$ AND $\varepsilon_u$ AS IN [6]

- A pre-cursor RANS simulation using the AKN model (i.e. PANS with  $f_k = 1$ ) is carried out. At  $Re_\theta = 3600$ ,  $U_{RANS}$ ,  $V_{RANS}$ ,  $k_{RANS}$  are taken.
- $\bar{u}_{in} = U_{RANS} + u'_{synt}$ ,  $\bar{v}_{in} = V_{RANS} + v'_{synt}$ ,  $\bar{w}_{in} = w'_{synt}$
- Anisotropic synthetic fluctuations are used. The fluctuations are scaled with  $k_u/k_{u,max}$ .
- $k_{u,in} = f_k k_{RANS}$ ,  $\varepsilon_{u,in} = C_\mu^{3/4} k_{u,in}^{3/2} / \ell_{sgs}$ ,  $\ell_{sgs} = C_s \Delta$ ,  $\Delta = V^{1/3}$ ,  
 $C_s = 0.05$

# INLET TURB. FLUCTUATION, TWO-POINT CORRELATIONS



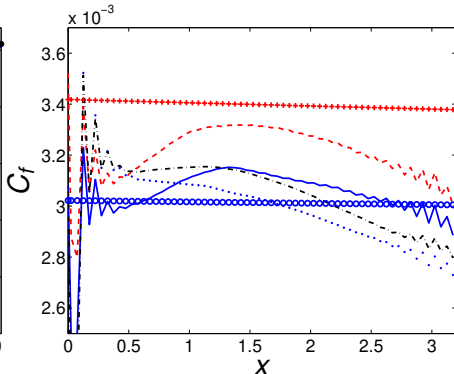
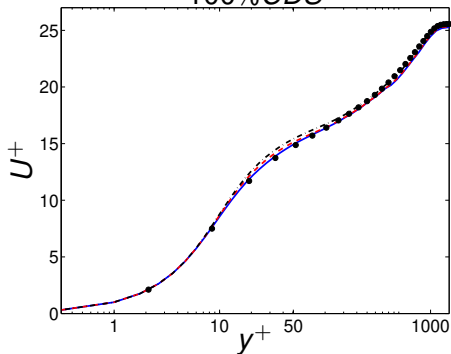
— :  $u_{rms}^+$ , - - - :  $v_{rms}^+$ , - - - :  $w_{rms}^+$   
 ··· :  $\langle u'v' \rangle^+$



○ : inlet; - - - :  $x = 3\delta_{in}$

# BOUNDARY LAYER: VELOCITY AND SKIN FRICTION

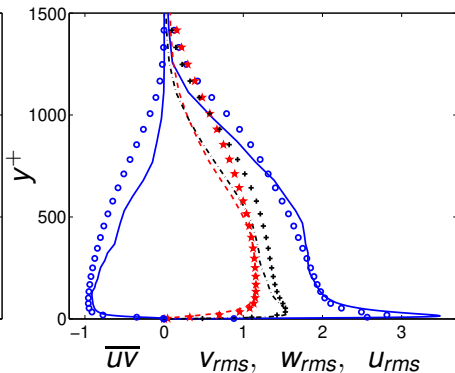
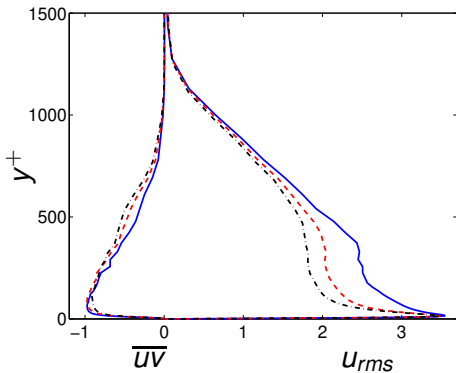
100% CDS



— :  $x = \delta_{in}$ ; - - - :  $x = 2\delta_{in}$ ; - · - · :  $x = 3\delta_{in}$ ; ■ : DNS [8]

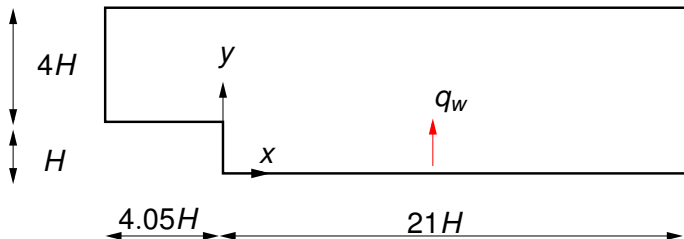
— : 100% CDS; - - - : 100% CDS,  $U_{in}$  from AKN; - · - · : 25% larger inlet fluct.; ···· : 25% larger inlet fluct.,  $C_s = 0.07$ ; markers:  $0.37 (\log_{10} Re_x)^{-2.584}$  (+ : AKN; o : DNS);

# REYNOLDS STRESSES



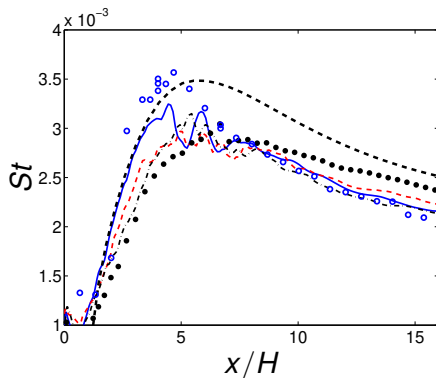
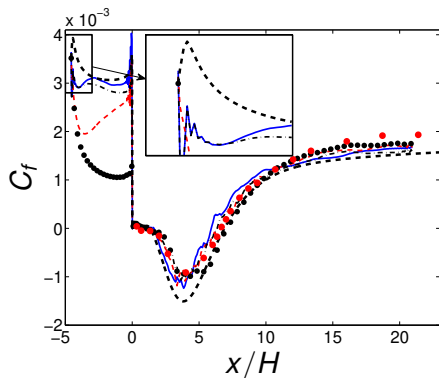
— :  $x = \delta_{in}$ ; - - - :  $x = 2\delta_{in}$ ; - · - · :  $x = 3\delta_{in}$ ; Markers: DNS [8]  
 $x = 3\delta_{in}$ .

## BACKWARD FACING STEP: DOMAIN



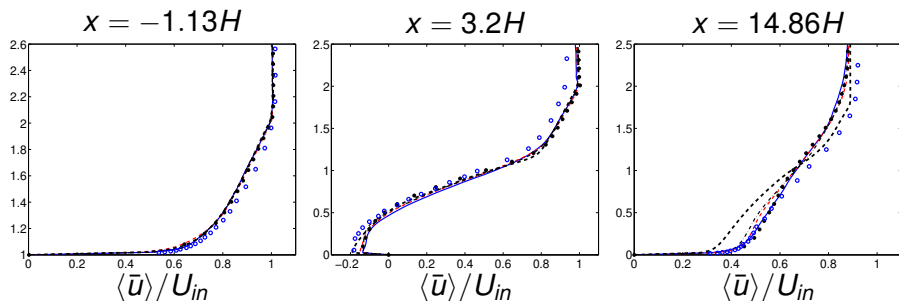
- $Re_H = 28\,000$  Experiments by Vogel & Eaton [9]
- Mean inlet profiles from RANS (same as in boundary layer)
- Grid:  $336 \times 120$  in  $x \times y$  plane.  $Z_{max} = 1.6H$ ,  $N_k = 64$ ,  $\Delta z_{in}^+ = 31$ .
- Anisotropic synthetic fluctuations,  $u'$ ,  $v'$ ,  $w'$  (same as for boundary layer flow); no fluctuations for  $t'$
- Constant heat flux,  $q_w$ , on lower wall.

# BACKSTEP FLOW. SKIN FRICTION AND STANTON NUMBER



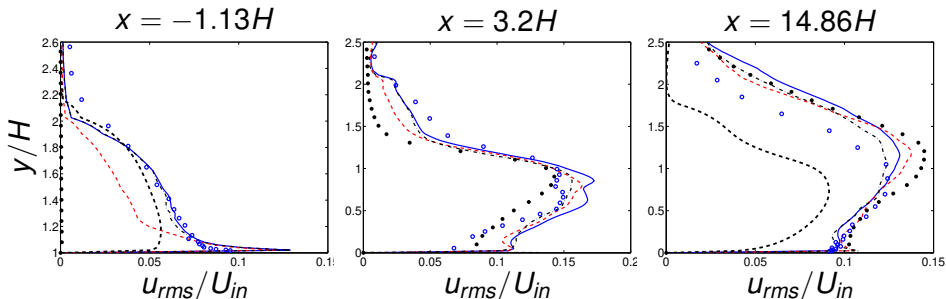
— : PANS; - - - : PANS, 50% smaller inlet fluctuations; - - - : WALE; ● : PANS, no inlet fluctuations; - - - : 2D RANS; ○, ● : experiments [9].

# BACKSTEP FLOW: VELOCITIES.



— : PANS; - - - : PANS, 50% smaller inlet fluctuations; - - - : WALE;  
● : PANS, no inlet fluctuations; - - - : 2D RANS; ○ : experiments [9].

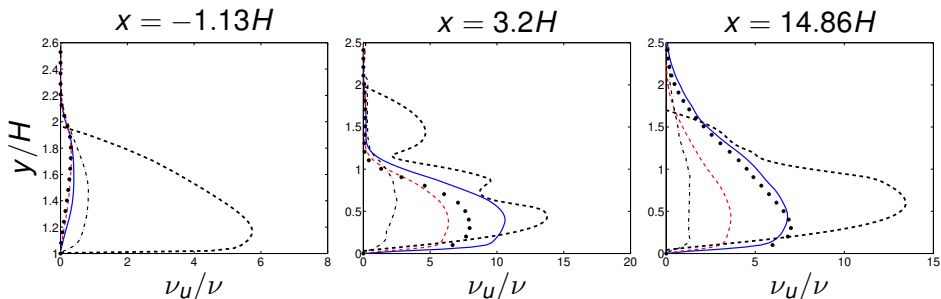
# BACKSTEP FLOW: RESOLVED STREAMWISE STRESS.



— : PANS; - - - : PANS, 50% smaller inlet fluctuations; · · · : WALE;  
● : PANS, no inlet fluctuations; - - - : 2D RANS; ○ : experiments [9].



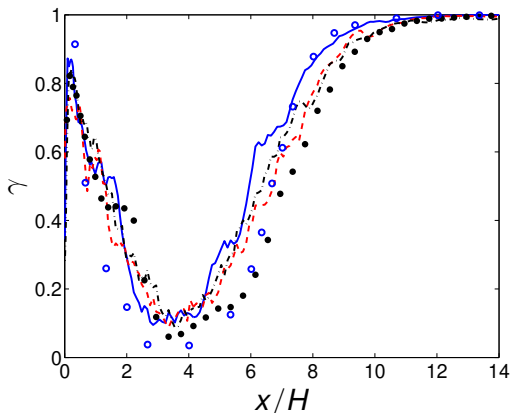
# BACKSTEP FLOW: TURBULENT VISCOSITIES.



— : PANS; - - - : PANS, 50% smaller inlet fluctuations; - - - : WALE;  
● : PANS, no inlet fluctuations; - - - : 2D RANS/10;

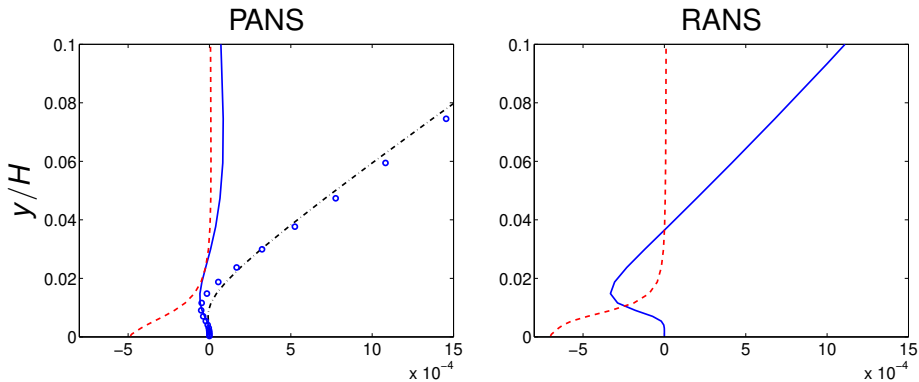
# FORWARD/BACKWARD FLOW

- Fraction of time,  $\gamma$ , when the flow along the bottom wall is in the downstream direction.



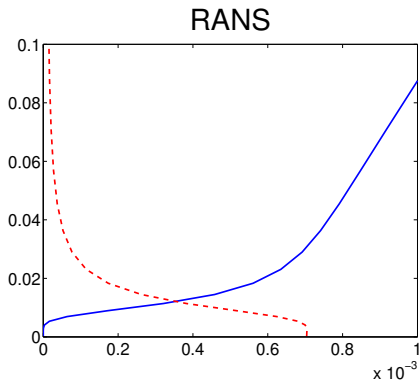
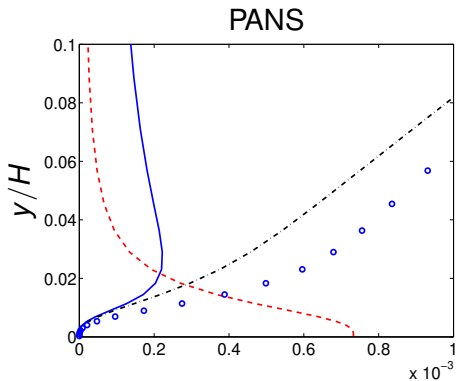
— : PANS; - - - : PANS, 50% smaller inlet fluctuations; ··· : WALE;  
● : PANS, no inlet fluctuations; ○ : experiments [9].

# SHEAR STRESSES. $x = 3.2H$



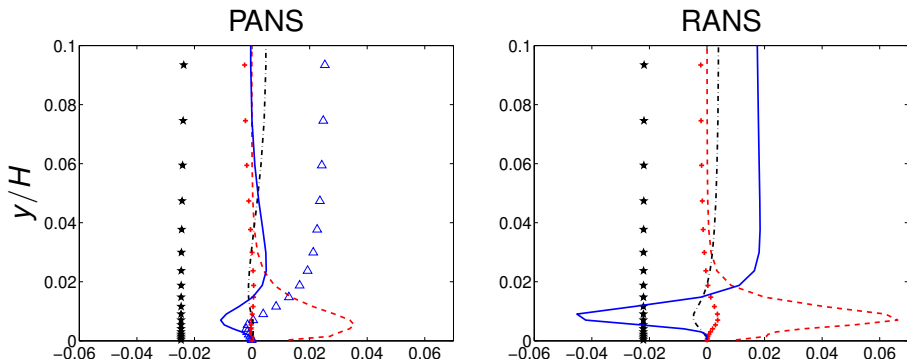
— :  $2\langle \nu_t \bar{s}_{12} \rangle$ ; 
 - - - :  $\nu \frac{\partial \langle \bar{u} \rangle}{\partial y}$ ; 
 - - - :  $-\langle \bar{u}\bar{v} \rangle$ ; 
 o :  $2\langle \nu_t \bar{s}_{12} \rangle - \langle \bar{u}\bar{v} \rangle$ .

# SHEAR STRESSES. $x = 14.86$



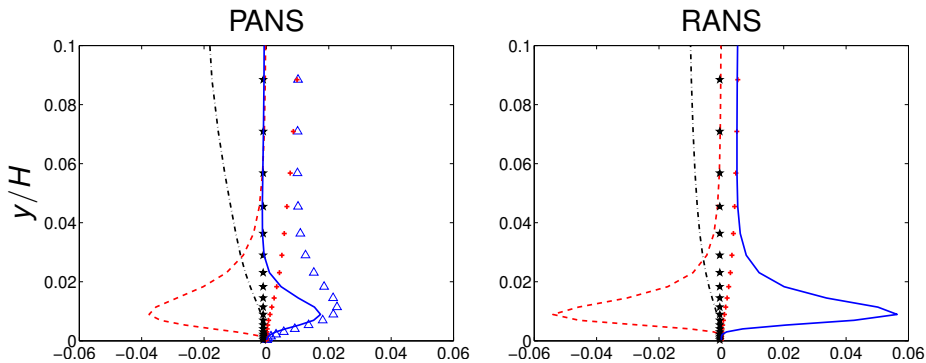
— :  $2\langle \nu_t \bar{s}_{12} \rangle$ ; 
 - - - :  $\nu \frac{\partial \langle \bar{u} \rangle}{\partial y}$ ; 
 - - - :  $-\langle \bar{u}\bar{v} \rangle$ ; 
 ○ :  $2\langle \nu_t \bar{s}_{12} \rangle - \langle \bar{u}\bar{v} \rangle$ .

# TERMS IN THE $\langle \bar{u} \rangle$ EQUATION. $x = 3.2H$



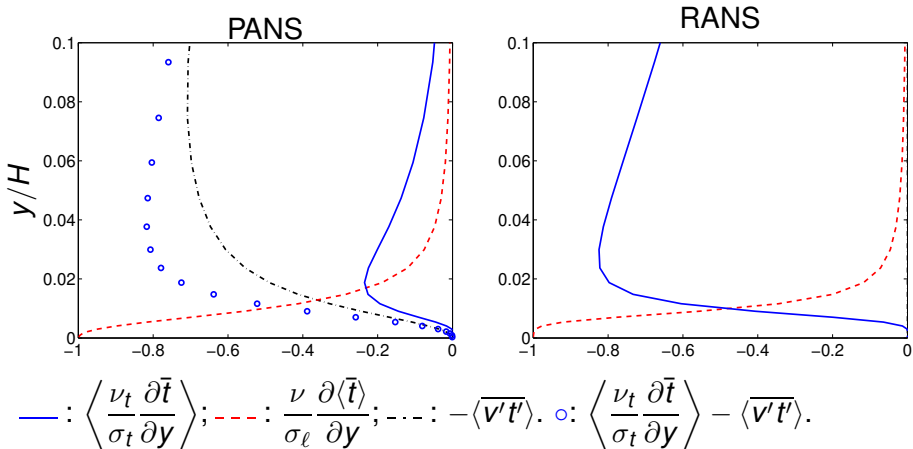
$$\begin{aligned}
 \text{—} &: \frac{\partial}{\partial y} (2\langle \nu_t \bar{s}_{12} \rangle); & \text{---} &: \nu \frac{\partial^2 \langle \bar{u} \rangle}{\partial y^2}; & \text{-.-.} &: -\frac{\partial \langle \bar{u} \rangle \langle \bar{u} \rangle}{\partial x}; & \text{+} &: -\frac{\partial \langle \bar{u} \rangle \langle \bar{v} \rangle}{\partial y}; & \text{*} &: \\
 \text{-} &: \frac{\partial \langle \bar{p} \rangle}{\partial x}, & \text{\triangle} &: -\frac{\partial \langle \bar{u} \bar{v} \rangle}{\partial y}.
 \end{aligned}$$

# TERMS IN THE $\langle \bar{u} \rangle$ EQUATION. $x = 14.86H$

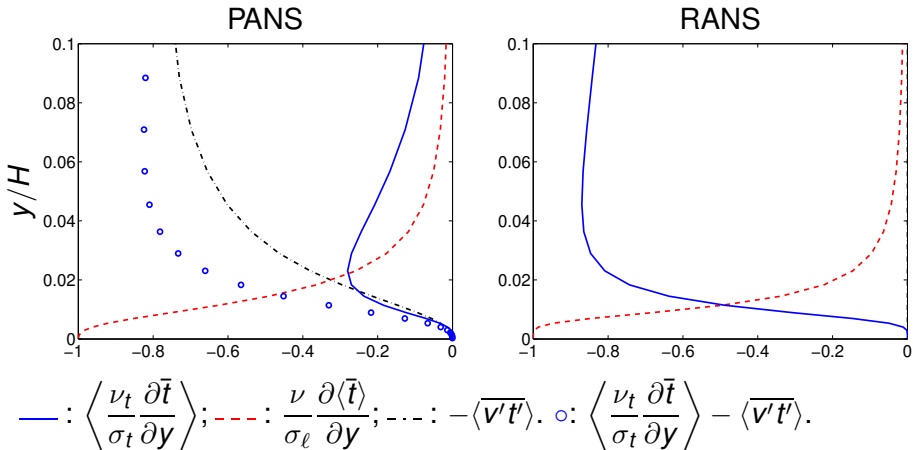


$$\begin{aligned}
 \text{—} &: \frac{\partial}{\partial y} (2\langle \nu_t \bar{s}_{12} \rangle); & \text{---} &: \nu \frac{\partial^2 \langle \bar{u} \rangle}{\partial y^2}; & \text{-.-.} &: -\frac{\partial \langle \bar{u} \rangle \langle \bar{u} \rangle}{\partial x}; & \text{+} &: -\frac{\partial \langle \bar{u} \rangle \langle \bar{v} \rangle}{\partial y}; & \text{*} &: \\
 \text{-} &: \frac{\partial \langle \bar{p} \rangle}{\partial x}, & \text{\triangle} &: -\frac{\partial \langle \bar{u} \bar{v} \rangle}{\partial y}.
 \end{aligned}$$

# HEAT FLUXES. $x = 3.2H$

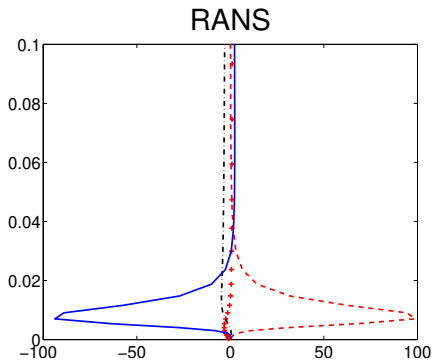
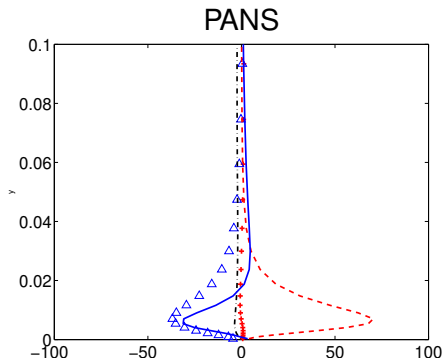


# HEAT FLUXES. $x = 14.86H$



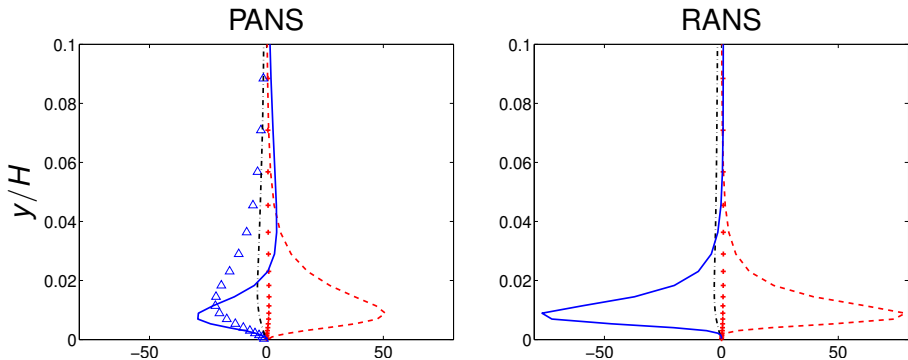


# TERMS IN THE $\langle \bar{t} \rangle$ EQUATION. $x = 3.2H$



$$\begin{aligned}
 \text{—} &: \frac{\partial}{\partial y} \left( \frac{\nu_t}{\sigma_t} \frac{\partial \langle \bar{t} \rangle}{\partial y} \right); \text{---} &: \frac{\nu}{\sigma_l} \frac{\partial^2 \langle \bar{t} \rangle}{\partial y^2}; \text{---} &: - \frac{\partial \langle \bar{u} \rangle \langle \bar{t} \rangle}{\partial x}; + &: - \frac{\partial \langle \bar{v} \rangle \langle \bar{t} \rangle}{\partial y}; \Delta &: \\
 \text{---} &: \frac{\partial \langle \bar{v}'t' \rangle}{\partial y}.
 \end{aligned}$$

# TERMS IN THE $\langle \bar{t} \rangle$ EQUATION. $x = 14.86H$



$$\begin{aligned}
 \text{—} &: \frac{\partial}{\partial y} \left( \frac{\nu_t}{\sigma_t} \frac{\partial \langle \bar{t} \rangle}{\partial y} \right); \quad \text{---} &: \frac{\nu}{\sigma_l} \frac{\partial^2 \langle \bar{t} \rangle}{\partial y^2}; \quad \text{- - -} &: - \frac{\partial \langle \bar{u} \rangle \langle \bar{t} \rangle}{\partial x}; \quad + &: - \frac{\partial \langle \bar{v} \rangle \langle \bar{t} \rangle}{\partial y}; \quad \Delta &: \\
 & - \frac{\partial \langle \bar{v}'t' \rangle}{\partial y}.
 \end{aligned}$$

# CONCLUDING REMARKS

- Developing boundary layer
  - ▶ Synthetic fluctuations give **fully developed conditions** after a **couple** of boundary layer thicknesses
  - ▶ 5% upwinding dampens resolved fluctuations; can be compensated by 25% larger inlet fluctuations
- Backstep flow
  - ▶ Very **good** agreement with experiments
  - ▶ 2D RANS predicts turbulent diffusion surprisingly well
  - ▶ Synthetic inlet fluctuations give an improved Stanton number; otherwise small effect in the recirculation region
  - ▶ LRN PANS and WALE equally good
  - ▶ 5% upwinding has a negligible effect in the recirculation region

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