

Lecture 4

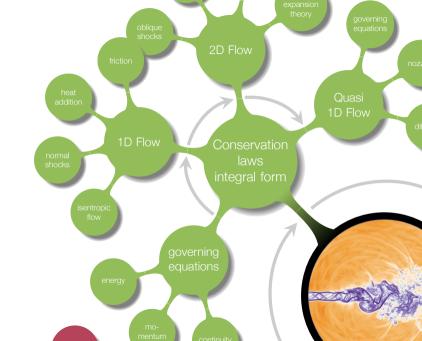
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Overview

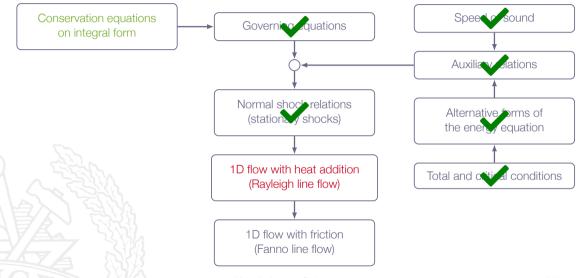


Learning Outcomes

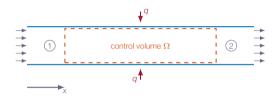
- 4 Present at least two different formulations of the governing equations for compressible flows and explain what basic conservation principles they are based on
- 5 Explain how thermodynamic relations enter into the flow equations
- 6 Define the special cases of calorically perfect gas, thermally perfect gas and real gas and explain the implication of each of these special cases
- 8 Derive (marked) and apply (all) of the presented mathematical formulae for classical gas dynamics
 - a 1D isentropic flow*
 - b normal shocks*
 - c 1D flow with heat addition*
 - d 1D flow with friction*

one-dimensional flows - isentropic and non-isentropic

Roadmap - One-dimensional Flow



Chapter 3.8 One-Dimensional Flow with Heat Addition



Pipe flow:

- no friction
- ▶ 1D steady-state \Rightarrow all variables depend on x only
- $\triangleright q$ is the amount of heat per unit mass added between 1 and 2
- analyze by setting up a control volume between station 1 and 2

$$\rho_1 u_1 = \rho_2 u_2$$

$$\rho_1 u_1^2 + \rho_1 = \rho_2 u_2^2 + \rho_2$$

$$h_1 + \frac{1}{2} u_1^2 + \mathbf{q} = h_2 + \frac{1}{2} u_2^2$$

Valid for all gases!

General gas ⇒ Numerical solution necessary

Calorically perfect gas ⇒ can be solved analytically

Calorically perfect gas $(h = C_p T)$:

$$C_{\rho}T_{1} + \frac{1}{2}u_{1}^{2} + \mathbf{q} = C_{\rho}T_{2} + \frac{1}{2}u_{2}^{2}$$

$$\mathbf{q} = \left(C_{\rho}T_{2} + \frac{1}{2}u_{2}^{2}\right) - \left(C_{\rho}T_{1} + \frac{1}{2}u_{1}^{2}\right)$$

$$C_{\rho}T_{0} = C_{\rho}T + \frac{1}{2}u^{2} \Rightarrow$$

$$\mathbf{q} = C_{\rho}(T_{o_{2}} - T_{o_{1}})$$

i.e. heat addition increases T_o downstream

Momentum equation:

$$p_{2} - p_{1} = \rho_{1}u_{1}^{2} - \rho_{2}u_{2}^{2}$$

$$\left\{\rho u^{2} = \rho a^{2}M^{2} = \rho \frac{\gamma p}{\rho}M^{2} = \gamma \rho M^{2}\right\}$$

$$p_{2} - p_{1} = \gamma p_{1}M_{1}^{2} - \gamma p_{2}M_{2}^{2} \Rightarrow$$

$$\frac{p_{2}}{\rho_{1}} = \frac{1 + \gamma M_{1}^{2}}{1 + \gamma M_{2}^{2}}$$

Ideal gas law:

$$T = \frac{\rho}{\rho R} \Rightarrow \frac{T_2}{T_1} = \frac{\rho_2}{\rho_2 R} \frac{\rho_1 R}{\rho_1} = \frac{\rho_2}{\rho_1} \frac{\rho_1}{\rho_2}$$

Continuity equation:

$$\rho_1 u_1 = \rho_2 u_2 \Rightarrow \frac{\rho_1}{\rho_2} = \frac{u_2}{u_1}$$

$$\frac{u_2}{u_1} = \frac{M_2 a_2}{M_1 a_1} = \frac{M_2 \sqrt{\gamma R T_2}}{M_1 \sqrt{\gamma R T_1}} \Rightarrow \frac{\rho_1}{\rho_2} = \frac{M_2}{M_1} \sqrt{\frac{T_2}{T_1}}$$
$$\frac{T_2}{T_1} = \left(\frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}\right)^2 \left(\frac{M_2}{M_1}\right)^2$$

Calorically perfect gas, analytic solution:

$$\frac{T_2}{T_1} = \left[\frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}\right]^2 \left(\frac{M_2}{M_1}\right)^2$$

$$\frac{\rho_2}{\rho_1} = \left[\frac{1 + \gamma M_2^2}{1 + \gamma M_1^2}\right] \left(\frac{M_1}{M_2}\right)^2$$

$$\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$$

Calorically perfect gas, analytic solution:

$$\frac{\rho_{o_2}}{\rho_{o_1}} = \left[\frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}\right] \left(\frac{1 + \frac{1}{2}(\gamma - 1)M_2^2}{1 + \frac{1}{2}(\gamma - 1)M_1^2}\right)^{\frac{\gamma}{\gamma - 1}}$$

$$\frac{T_{O_2}}{T_{O_1}} = \left[\frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}\right] \left(\frac{M_2}{M_1}\right)^2 \left(\frac{1 + \frac{1}{2}(\gamma - 1)M_2^2}{1 + \frac{1}{2}(\gamma - 1)M_1^2}\right)^{\frac{\gamma}{\gamma - 1}}$$

Initially subsonic flow (M < 1)

- ▶ the Mach number, M, increases as more heat (per unit mass) is added to the gas
- ightharpoonup for some limiting heat addition q^* , the flow will eventually become sonic M=1

Initially supersonic flow (M > 1)

- \triangleright the Mach number, M, decreases as more heat (per unit mass) is added to the gas
- for some limiting heat addition q^* , the flow will eventually become sonic M=1

Note! The (*) condition in this context <u>is not</u> the same as the "critical" condition discussed for isentropic flow

$$\frac{\rho_2}{\rho_1} = \frac{1 + \gamma M_1^2}{1 + \gamma M_2^2}$$

Calculate the ratio between the pressure at a specific location in the flow p and the pressure at sonic conditions p^*

$$p_1 = p$$
, $M_1 = M$, $p_2 = p^*$, and $M_2 = 1$

$$\frac{p^*}{p} = \frac{1 + \gamma M^2}{1 + \gamma}$$

$$\frac{T}{T^*} = \left[\frac{1+\gamma}{1+\gamma M^2}\right]^2 M^2$$

$$\frac{\rho}{\rho^*} = \left[\frac{1+\gamma M^2}{1+\gamma}\right] \left(\frac{1}{M^2}\right)$$

$$\frac{\rho}{\rho^*} = \frac{1+\gamma}{1+\gamma M^2}$$

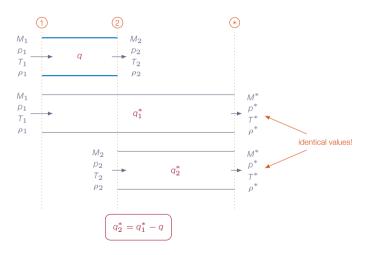
$$\frac{\rho_o}{\rho_o^*} = \left[\frac{1+\gamma}{1+\gamma M^2}\right] \left(\frac{2+(\gamma-1)M^2}{(\gamma+1)}\right)^{\frac{\gamma}{\gamma-1}}$$

$$\frac{T_o}{T_o^*} = \frac{(\gamma + 1)M^2}{(1 + \gamma M^2)^2} (2 + (\gamma - 1)M^2)$$

Amount of heat per unit mass needed to choke the flow:

$$q^* = C_p(T_o^* - T_o) = C_p T_o \left(\frac{T_o^*}{T_o} - 1\right)$$





Note! for a given flow, the starred quantities are constant values

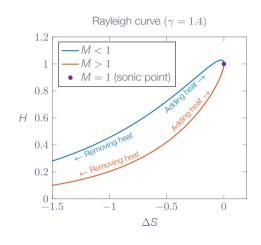


Lord Rayleigh 1842-1919 Nobel prize in physics 1904

Note! it is theoretically possible to heat an initially subsonic flow to reach sonic conditions and then continue to accelerate the flow by cooling

$$\Delta S = \frac{\Delta s}{C_p} = \ln \left[M^2 \left(\frac{\gamma + 1}{1 + \gamma M^2} \right)^{\frac{\gamma + 1}{\gamma}} \right]$$

$$H = \frac{h}{h^*} = \frac{C_p T}{C_p T^*} = \frac{T}{T^*} = \left[\frac{(\gamma + 1)M}{1 + \gamma M^2}\right]^2$$



And now, the million-dollar question ...



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Removing heat seems to reduce the entropy. Isn't that a violation of the second law of thermodynamics?!

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Answer: if the heat source or sink would have been included in the system studied, the system entropy would increase both when adding and removing heat.

M < 1: Adding heat will

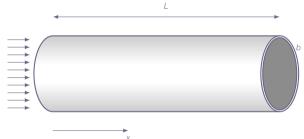
M > 1: Adding heat will

increase Mdecrease pincrease T_o decrease p_o increase sincrease udecrease p

decrease Mincrease pincrease T_o decrease p_o increase p_o increase p_o increase p_o

Note! the flow is not isentropic, there will always be losses

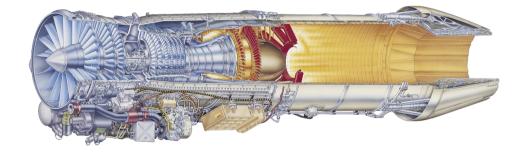
Relation between added heat per unit mass (q) and heat per unit surface area and unit time (\dot{q}_{wall})



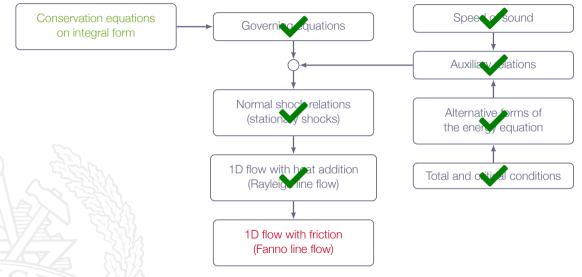
Pipe with arbitrary cross section (constant in x):

mass flow through pipe \dot{m} axial length of pipe \dot{m} circumference of pipe \dot{m} \dot{m}

$$q = \frac{Lb\dot{q}_{wa}}{\dot{m}}$$



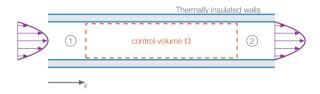
Roadmap - One-dimensional Flow



Chapter 3.9 One-Dimensional Flow with Friction

inviscid flow with friction?!





Pipe flow:

- ightharpoonup adiabatic (q=0)
- cross section area A is constant
- ightharpoonup average all variables in each cross-section \Rightarrow only x-dependence
- analyze by setting up a control volume between station 1 and 2

Wall-friction contribution in momentum equation

$$\iint\limits_{\partial\Omega}\tau_{w}dS=b\int_{0}^{L}\tau_{w}dx$$

where L is the tube length and b is the circumference

$$\rho_1 u_1 = \rho_2 u_2$$

$$\rho_1 u_1^2 + \rho_1 - \frac{4}{D} \int_0^L \tau_W dx = \rho_2 u_2^2 + \rho_2$$

$$h_1 + \frac{1}{2} u_1^2 = h_2 + \frac{1}{2} u_2^2$$

 τ_{w} varies with the distance x and thus complicating the integration

Solution: let L shrink to dx and we end up with relations on differential form

$$d(\rho u^{2} + \rho) = -\frac{4}{D}\tau_{w}dx \Leftrightarrow \frac{d}{dx}(\rho u^{2} + \rho) = -\frac{4}{D}\tau_{w}$$

From the continuity equation we get

$$\rho_1 u_1 = \rho_2 u_2 = const \Rightarrow \frac{d}{dx}(\rho u) = 0$$

Writing out all terms in the momentum equation gives

$$\frac{d}{dx}(\rho u^2 + p) = \rho u \frac{du}{dx} + u \underbrace{\frac{d}{dx}(\rho u)}_{=0} + \frac{dp}{dx} = -\frac{4}{D}\tau_{w} \Rightarrow \rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{4}{D}\tau_{w}$$

Common approximation for τ_w :

$$\tau_W = f \frac{1}{2} \rho u^2 \Rightarrow \rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{2}{D} \rho u^2 f$$

Energy conservation:

$$h_{O_1} = h_{O_2} \Rightarrow \frac{d}{dx} h_O = 0$$



Summary:

$$\frac{d}{dx}(\rho u) = 0$$

$$\rho u \frac{du}{dx} + \frac{dp}{dx} = -\frac{2}{D}\rho u^2 f$$

$$\frac{d}{dx}h_o = 0$$

Valid for all gases!

General gas ⇒ Numerical solution necessary

Calorically perfect gas \Rightarrow Can be solved analytically (for constant f)

Calorically perfect gas:

$$\int_{x_1}^{x_2} \frac{4f}{D} dx = \left[-\frac{1}{\gamma M^2} - \frac{\gamma + 1}{2\gamma} \ln \left(\frac{M^2}{1 + \frac{\gamma - 1}{2} M^2} \right) \right]_{M_1}^{M_2}$$

Calorically perfect gas:

$$\frac{T_2}{T_1} = \frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2}$$

$$\frac{\rho_2}{\rho_1} = \frac{M_1}{M_2} \left[\frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2} \right]^{-1/2}$$

$$\frac{\rho_2}{\rho_1} = \frac{M_1}{M_2} \left[\frac{2 + (\gamma - 1)M_1^2}{2 + (\gamma - 1)M_2^2} \right]^{1/2}$$

$$\frac{p_{o_2}}{p_{o_1}} = \frac{M_1}{M_2} \left[\frac{2 + (\gamma - 1)M_2^2}{2 + (\gamma - 1)M_1^2} \right]^{\frac{\gamma + 1}{2(\gamma - 1)}}$$

Initially subsonic flow ($M_1 < 1$)

- $ightharpoonup M_2$ will increase as L increases
- for a critical length L^* , the flow at point 2 will reach sonic conditions, i.e. $M_2 = 1$

Initially supersonic flow ($M_1 > 1$)

- $ightharpoonup M_2$ will decrease as L increases
- for a critical length L^* , the flow at point 2 will reach sonic conditions, i.e. $M_2 = 1$

Note! The (*) condition in this context <u>is not</u> the same as the "critical" condition discussed for isentropic flow

$$\frac{T}{T^*} = \frac{(\gamma+1)}{2+(\gamma-1)M^2}$$

$$\frac{\rho}{\rho^*} = \frac{1}{M} \left[\frac{2 + (\gamma - 1)M^2}{\gamma + 1} \right]^{1/2}$$

$$\frac{\rho}{\rho^*} = \frac{1}{M} \left[\frac{\gamma + 1}{2 + (\gamma - 1)M^2} \right]^{1/2} \qquad \frac{\rho_0}{\rho_0^*} = \frac{1}{M} \left[\frac{2 + (\gamma - 1)M^2}{\gamma + 1} \right]^{\frac{\gamma + 1}{2(\gamma - 1)}}$$

$$\frac{D_0}{D_0^*} = \frac{1}{M} \left[\frac{2 + (\gamma - 1)M^2}{\gamma + 1} \right]^{\frac{\gamma + 1}{2(\gamma - 1)}}$$

see Table A.4

and

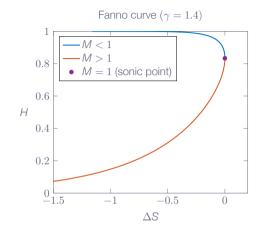
$$\int_0^{L^*} \frac{4f}{D} dx = \left[-\frac{1}{\gamma M^2} - \frac{\gamma + 1}{2\gamma} \ln \left(\frac{M^2}{1 + \frac{\gamma - 1}{2} M^2} \right) \right]_M^T$$

where L* is the tube length needed to change current state to sonic conditions

Let \bar{f} be the average friction coefficient over the length $L^* \Rightarrow$

$$\frac{4\bar{f}L^*}{D} = \frac{1 - M^2}{\gamma M^2} + \frac{\gamma + 1}{2\gamma} \ln\left(\frac{(\gamma + 1)M^2}{2 + (\gamma - 1)M^2}\right)$$

Turbulent pipe flow \rightarrow $\bar{\it f} \sim 0.005$ (Re $> 10^5$, roughness ~ 0.001 D)



$$H = \frac{h}{h_o} = \frac{C_p T}{C_p T_o} = \frac{T}{T_o} = \left[1 + \frac{\gamma - 1}{2} M^2\right]^{-1}$$

$$\Delta S = \frac{\Delta S}{C_D} = \ln \left[\left(\frac{1}{H} - 1 \right)^{\frac{\gamma - 1}{2\gamma}} \left(\frac{2}{\gamma - 1} \right)^{\frac{\gamma - 1}{2\gamma}} \left(\frac{\gamma + 1}{2} \right)^{\frac{\gamma + 1}{2\gamma}} (H)^{\frac{\gamma + 1}{2\gamma}} \right]$$

M < 1: Friction will

M > 1: Friction will

increase Mdecrease pdecrease Tdecrease sincrease sincrease sdecrease s

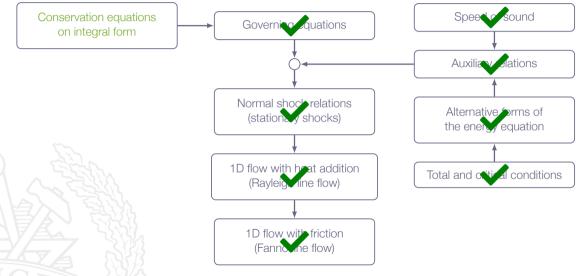
decrease Mincrease pincrease Tdecrease p_0 increase p_0 increase p_0 increase p_0

Note! the flow is not isentropic, there will always be losses

One-Dimensional Flow with Friction - Pipeline



Roadmap - One-dimensional Flow



What if you somehow managed to make a stereo travel at twice the speed of sound, would it sound backwards to someone who was just casually sitting somewhere as it flies by?

-Tim Currie

Yes.

Technically, anyway. It would be pretty hard to hear.

The basic idea is pretty straightforward. The stereo is going faster than its own sound, so it will reach you first, followed by the sound it emitted one second ago, followed by the sound it emitted two seconds ago, and so forth.



The problem is that the stereo is moving at Mach 2, which means that two seconds ago, it was over a kilometer away. It's hard to hear music from that distance, particularly when your ears were just hit by (a) a sonic boom, and (b) pieces of a rapidly disintegrating stereo.

Wind speeds of Mach 2 would messily disassemble most consumer electronics. The force of the wind on the body of the stereo is roughly comparable to that of a dozen people standing on it:

