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CFD WITH OPENSOURCE SOFTWARE

A COURSE AT CHALMERS UNIVERSITY OF TECHNOLOGY
TAUGHT BY HÅKAN NILSSON

Implementation of a Monodisperse Population Balance Model in laminar combustion model

Developed for OpenFOAM-v2006

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Disclaimer: This is a student project work, done as part of a course where OpenFOAM and some other OpenSource software are introduced to the students. Any reader should be aware that it might not be free of errors. Still, it might be useful for someone who would like learn some details similar to the ones presented in the report and in the accompanying files. The material has gone through a review process. The role of the reviewer is to go through the tutorial and make sure that it works, that it is possible to follow, and to some extent correct the writing. The reviewer has no responsibility for the contents.

January 26, 2023

Learning outcomes

The main requirements of a tutorial in the course is that it should teach the four points: How to use it, The theory of it, How it is implemented, and How to modify it. Therefore the list of learning outcomes is organized with those headers.

The reader will learn:

How to use it:

- how to use `laminarSoot` combustion model with `reactingFoam`
- how to set up cases that can be used with `laminarSoot` to simulate soot formation in combustion or pyrolysis of hydrocarbons

The theory of it:

- how the proposed monodisperse population balance model (MPBM) describes soot evolution
- how the soot model impacts the production/destruction rate of species

How it is implemented:

- how a combustion model communicates with `reactingFoam` solver
- how to calculate soot inception, growth, oxidation and coagulation rates within `laminarSoot` library and utilize them to solve transport equations of tracked fields

How to modify it:

- how the reaction rates and heat release obtained from gas chemistry should be modified to account for the production/consumption of species mass and energy by soot inception, growth and oxidation

Prerequisites

The reader is expected to know the following in order to get maximum benefit out of this report:

- Fundamental knowledge of fluid mechanics, combustion, chemistry, and soot structure and composition.
- Familiarity with computational fluid dynamics (CFD) and transport equation of physical properties
- A good knowledge of structure of solvers and libraries of OpenFOAM ^{1, 2}
- Understanding C++ syntax and accessing the object properties and methods
- How to create, modify and run OpenFOAM cases ^{3, 4}

¹<https://www.openfoam.com/documentation/guides/v2112/doc/>

²<http://www.tfd.chalmers.se/~hani/kurser/OS.CFD/>

³<https://www.openfoam.com/documentation/tutorial-guide/1-introduction>

⁴<https://www.openfoam.com/documentation/user-guide>

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Nomenclature

Acronyms

CFD	Computational Fluid Dynamics
DEM	Discrete Element Modelling
HACA	Hydrogen abstraction carbon addition
MPBM	Monodisperse Population Balance Model
SPBM	Sectional Population Balance Model

English symbols

Av	Avogadro's number	$6.02214076 \times 10^{23} \text{ 1/mol}$
C_{tot}	Carbon content of soot particles	mol/kg
d	diameter	m
d_g	Gyratation diameter	m
d_m	Mobility diameter	m
d_p	Primary particle diameter	m
H_{tot}	Hydrogen content of soot particles	mol/kg
k	reaction rate constant	$\text{m}^3/\text{mol} - \text{s}$
k_B	Boltzmann constant	$1.3806488 \times 10^{-23} \text{ m}^2\text{kg/s}^2 - \text{K}$
m	mass	kg
n_p	Number of primary particles	
N_{agg}	Number density of agglomerates	mol/kg
N_{pri}	Number density of primary particles	mol/kg
T	Temperature	K
W	Molecular weight	kg

Greek symbols

β	Collision frequency	m^3/s
λ	Mean free path	m
ν	Gas kinematic viscosity	m^2/s
ω	The rate of production/consumption of species	$\text{mol/m}^3 - \text{s}$
ρ	Gas density	kg/m^3
ρ_{soot}	Soot density	kg/m^3

Subscripts

ad	Adsorption
agg	Agglomerate
coag	Coagulation
cont	Continuum
fm	Free molecular
fw	forward
FWD	forward
g	Gyratation

grow	Surface growth
inc	Inception
m	Mobility
ox	Oxidation
pri	Primary particle
rc	reactive
REAC	reactive
REV	reverse
rv	reverse

Chapter 1

Introduction

1.1 Background

Soot (black carbon) is a major air pollutant, and the third strongest contributor to climate change [1]. Carbon black (CB) with similar synthesis process and properties to soot is the largest industrially produced nanomaterial by value and volume (15 megatons per year with a value of \$17B) with applications as a reinforcing agent in rubber [2] and conductive additive in lithium-ion batteries [3]. Controlling properties of these particles is essential to determine functional properties of CB and environmental effects of soot, but it is challenging due to the complexity of soot formation, its coupling with gas phase chemistry [4], and fluid dynamic effects. So, accurate predictive models are required to describe fluid flow, gas chemistry and different steps of soot formation and evolution in a coupled manner.

Soot morphology can be described accurately by mesoscale simulations, such as Discrete Element Modeling (DEM) [5], but they are computationally expensive and difficult to interface with the computational fluid dynamic (CFD) methods. So, sectional population balance models (SPBM) coupled with power-laws are used in flow reactors [6] and laminar flames [7]. However, their computational cost grows exponentially by increasing the number of sections.

Monodisperse population balance models (MPBM) are alternative modelling approaches that describe average particle properties by tracking their total concentration, mass and area [8], but their accuracy depends on the assumptions about particle morphology (e.g. approximating agglomerates as monodisperse and perfect spheres). However, when inception and surface growth are short [9] and high particle (number) concentrations are formed [10], they lead to rapid attainment of self-preserving size distributions (SPSD) and agglomerates having asymptotic structure [11]. In these conditions, a MPBM can achieve accuracies on par with DEM [5], SPBM [12] and experimental data [8].

Due to high computational costs of the detailed description of gas chemistry, pseudo one-dimensional approaches are often used with detailed reaction mechanisms for prediction of species and soot in laminar flames and flow reactors [13]. However, one dimensional assumption is not valid when probes disturb the fluid flow or gravity effects are significant in flames [14] or when recirculation occurs in flow reactors. They may alter the chemistry of the gas and thereby change the soot formation. Capturing these effect requires a soot model coupled with chemistry solver and fluid dynamics. So, a combustion model that links reacting mixture solver to chemistry can provide an effective framework for the implementation of soot model.

1.2 Laminar combustion model

The main role of a combustion model in `reactingFoam` is to calculate (i) the net production rate of species contributes that appears as a source term in the transport equation of mass fraction Y and (ii) the net heat release from reaction that acts as a source term in conservation of enthalpy

he (this will be further investigated in Sec. 3.8). A full list of available combustion models in OpenFOAM can be found in the source directory under `$FOAM_SRC/combustionModels`. However, only `laminar` and `EDC` model are used in tutorial examples. These two models differ in how they treat the net production rate, R , and heat release Q_{dot} . `laminar` model uses Arrhenius form expressions to calculate reaction rates neglecting the effect of turbulent fluctuations on reaction rates, which proves accurate for laminar flames, while `EDC` incorporates the turbulence quantities in calculation of reaction rate and heat release.

1.3 Objectives

This project aims to extend `laminar` combustion model to develop a new library, `laminarSoot`, which incorporates a MPBM for modelling soot formation by

- adding four additional transport equations to track the number density of primary particles (N_{pri}) and agglomerates (N_{agg}), total carbon (C_{tot}) and hydrogen (H_{tot}) content of soot particles
- implementing new functionalities to calculate contribution of inception, growth, coagulation and oxidation of soot to source terms of each transport equation
- modifying the production rates and rate of heat release to satisfy the conservation of species mass and energy.

Finally, `laminarSoot` is utilized with `reactingFoam` in a simple test case to test the performance of new library and evaluate the results.

Chapter 2

Theory

In this chapter, an overview of mathematical basic of the soot model is presented, which includes the transport equations, characterization of soot morphology and calculation of source terms corresponding to each step of soot evolution. All equations will be used to implement the soot model in `laminarSoot` library.

2.1 Transport equations

MPBM relies on the Eulerian description of particles where certain physical properties representative of particle population such as number density, mass or surface area are treated as continuous quantities that can be described by solving scalar transport equations. The formulation of soot model used in this project follows MPBM proposed by Kholghy and Kelesidis [8] based on number density of agglomerates, total carbon content and total surface area of particles. Here, we modify the original model by tracking the number density of primary particles (N_{pri}) and agglomerates (N_{agg}), total carbon (C_{tot}) and hydrogen (H_{tot}) content of soot particles by solving the following transport equations

$$\frac{\partial}{\partial t}(\rho N_{agg}) + \nabla \cdot (\rho u N_{agg}) + \nabla^2(\rho D N_{agg}) = \rho (S_{inc}^N + S_{coag}^N), \quad (2.1)$$

$$\frac{\partial}{\partial t}(\rho N_{pri}) + \nabla \cdot (\rho u N_{pri}) + \nabla^2(\rho D N_{pri}) = \rho S_{inc}^N, \quad (2.2)$$

$$\frac{\partial}{\partial t}(\rho C_{tot}) + \nabla \cdot (\rho u C_{tot}) + \nabla^2(\rho D C_{tot}) = \rho (S_{inc}^C + S_{grow}^C + S_{ox}^C), \quad (2.3)$$

$$\frac{\partial}{\partial t}(\rho H_{tot}) + \nabla \cdot (\rho u H_{tot}) + \nabla^2(\rho D H_{tot}) = \rho (S_{inc}^H + S_{grow}^H + S_{ox}^H). \quad (2.4)$$

In Equations (2.1)-(2.4), S represents the source terms where superscripts indicates the transport equation and subscripts denotes the process the source term is associated with. For example, S_{grow}^C accounts for the addition of carbon to soot particles via surface growth.

2.2 Morphology

Soot particles are formed as agglomerates of spherical primary particles. Incipient soot has spherical shape, and collision and attachment of these spheres results in fractal-like agglomerate. Hereafter, the word "*particle*" refers to soot both in spherical and agglomerate shape. The morphology of soot agglomerates are characterized by primary particle, mobility, and gyration diameters. These diameters can be related to each other by number of primary particles using power-laws. Mobility and gyration diameters are the diameter of the sphere with the same translational and rotational

properties of an agglomerate, respectively. Figure 2.1 illustrates the schematics of sample soot agglomerates with 12 primary particles and depicted d_p , d_m , d_g .

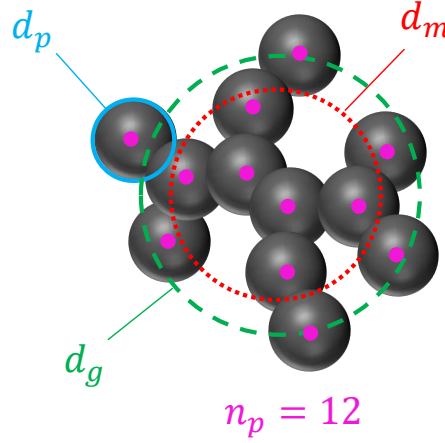


Figure 2.1: The schematics of a soot agglomerates with 12 primary particles ($n_p = 12$). Primary particle (d_p), mobility (d_m), and gyration (d_g) are shown.

n_p is the number of primary particles in each agglomerate that can be obtained by dividing the number density of primary particles by that of agglomerates,

$$n_p = \frac{N_{pri}}{N_{agg}}. \quad (2.5)$$

Primary particle diameter, d_p , can be obtained from total carbon and number density of primary particles using

$$d_p = \left(\frac{6}{\pi} \frac{C_{tot} \cdot W_{carbon}}{\rho_{soot}} \frac{1}{N_{pri} \cdot Av} \right)^{1/3}. \quad (2.6)$$

The DEM-derived power-laws relate d_m and d_g to d_p and n_p as

$$d_m = d_p \cdot n_p^{0.45}, \quad (2.7)$$

$$d_g = \begin{cases} d_m / (n_p^{-0.2} + 0.4), & \text{if } n_p > 1.5 \\ d_m / 1.29, & \text{if } n_p \leq 1.5 \end{cases} \quad (2.8)$$

d_m and d_g are used to calculate the collision and attachment rate of soot agglomerates that accounts for the coagulation source term.

2.3 Diffusion of soot particles

The diffusion coefficient of soot particle, D , used in Equations (2.1)-(2.4) is calculated as

$$D = \frac{k_B T}{f}, \quad (2.9)$$

where f is the friction factor of particles in gas, and it is calculated for free molecular to continuum regimes as

$$f = \frac{3\pi\mu d_m}{C}, \quad (2.10)$$

$$C = 1 + \frac{2\lambda}{d_m} \left(1.21 + 0.4 \exp\left(\frac{-0.78d_m}{\lambda}\right) \right), \quad (2.11)$$

where λ is the mean free path of gas given as:

$$\lambda = \frac{\mu}{\rho} \sqrt{\frac{\pi W_{gas}}{2k_B A v T}}. \quad (2.12)$$

2.4 Coagulation

Coagulation is the process during which solid and hard soot particles collide and attach at point of contact leading to larger agglomerates. This process conserves the soot mass and composition and number density of primary particles, so coagulation only affects N_{agg} (Equation (2.1)). S_{coag}^N accounts for the decay rate of N_{agg} by the binary collision of soot particles by

$$S_{coag}^N = -\frac{1}{2} \beta N_{agg}^2, \quad (2.13)$$

where β is harmonic mean of collision frequency in the continuum (β_{cont}) and free molecular (β_{fm}) regimes enhanced by %82 accounting for the polydispersity of particles [15] using the following relations

$$\beta = 1.82 \frac{\beta_{fm} \beta_{cont}}{\beta_{fm} + \beta_{cont}}, \quad (2.14)$$

$$\beta_{fm} = 4 \sqrt{\frac{\pi k_b T}{m_{agg}}} d_g^2, \quad (2.15)$$

$$\beta_{cont} = 8 \frac{k_b T}{3\mu} \left(1 + \frac{2\lambda}{d_m} \left[1.21 + 0.4 e^{-\frac{0.78d_m}{\lambda}} \right] \right). \quad (2.16)$$

2.5 Surface growth via HACA

Hydrogen abstraction carbon addition (HACA) is a major pathway for soot mass growth where active reaction sites on particles form bonds with acetylene molecule (C_2H_2). HACA mechanism [16] is described by a set of elementary with a given rates that are listed in Table 2.1. The HACA rate is defined as the absolute rate change of concentration of C_2H_2 ($\omega_{c_2h_2}$) via HACA mechanism as

$$\omega_{c_2h_2} = \alpha k_{f4} [C_2H_2] [C_{soot}^*], \quad (2.17)$$

$$\frac{d}{dt} [C_2H_2] = -\omega_{c_2h_2}. \quad (2.18)$$

In Equation (2.17), k_{f4} refers to forward reaction rate constant of 4th reaction in reaction 4 in Table 2.1. The contribution of HACA to growth source terms can be computed from HACA rate considering the number of carbon atoms in C_2H_2 and number of arm-chair and zig-zag hydrogenated sites on soot particle [17] using

$$S_{grow|HACA}^C = 2\omega_{c_2h_2} / \rho, \quad (2.19)$$

$$S_{grow|HACA}^H = 0.25\omega_{c_2h_2} / \rho. \quad (2.20)$$

In Equation (2.17), α is the surface reactivity of soot defined by an empirical relation [16] as

$$\alpha = \tanh \left(\frac{12.56 - 0.00563 \cdot T}{\log_{10} \left(\frac{\rho_{soot} \frac{\pi}{6} d_p^3 \cdot Av}{W_{carbon}} \right)} - 1.38 + 0.00068 \cdot T \right). \quad (2.21)$$

Table 2.1: Rate coefficients for the various surface reactions in Arrhenius form $k = AT^n \cdot e^{-E/RT}$

No.	Reaction	A	$\left[\frac{m^3}{mol \cdot s}\right]$	n	$\frac{E}{R} [K]$
1	$C_{soot-H} + H \rightleftharpoons C_{soot^\circ} + H_2$	f	4.17×10^7	0	6542.52
		r	3.9×10^6	0	5535.98
2	$C_{soot-H} + OH \rightleftharpoons C_{soot^\circ} + H_2O$	f	10^4	0.734	719.68
		r	3.68×10^2	1.139	8605.94
3	$C_{soot^\circ} + H \longrightarrow C_{soot} + H_2O$	f	10^4	0.734	719.68
4	$C_{soot^\circ} + C_2H_2 \longrightarrow C_{soot-H}$	f	80	1.56	1912.43
5	$C_{soot^\circ} + O_2 \longrightarrow 2 CO$	f	2.2×10^6	0	3774.53
6	$C_{soot-H} + OH \longrightarrow CO + \frac{1}{2} H_2$	f	0.13	0	0

$[C_{soot^\circ}]$ is the concentration of dehydrogenated site on soot particle computed by

$$[C_{soot^\circ}] = A_{tot} \frac{\rho}{Av} \chi_{soot^\circ}. \quad (2.22)$$

A_{tot} is the total surface area of soot particles obtained as

$$A_{tot} = N_{pri} Av \cdot \pi d_p^2, \quad (2.23)$$

χ_{soot° is the number of active reaction sites per unit surface area of particles.

$$\chi_{soot^\circ} = \frac{k_{f1}[H] + k_{f2}[OH]}{k_{r1}[H_2] + k_{r2}[H_2O] + k_{f3}[H] + k_{f4}[C_2H_2] + k_{f5}[O_2] + k_{f1}[H] + k_{f2}[OH]} \chi_{soot_{CH}}, \quad (2.24)$$

where $\chi_{soot_{CH}} = 2.3 \times 10^{19} m^{-2}$. In Equation (2.24), k_{r1} denotes the reverse rate of the first reaction in Table 2.1, and the rest of reaction rates follow the same naming convention.

2.6 Oxidation via HACA

The carbon atoms on the surface of soot are oxidized via reaction with O_2 molecules and OH radicals which decreases total carbon of soot and releases CO and H_2 molecules to gas mixture. The oxidation process is described by HACA mechanism. Here, we assume that oxidation does not change the hydrogen content of soot particles. The absolute rate change of O_2 molecules (ω_{o2}) and OH radicals (ω_{oh}) by oxidation is calculated as

$$\omega_{o2} = \alpha k_{f5}[O_2][C_{soot^\circ}], \quad (2.25)$$

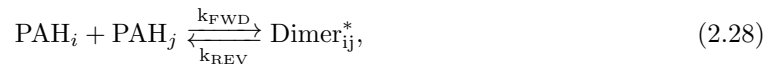
$$\omega_{oh} = \alpha k_{f6}[OH] N_{agg} \rho. \quad (2.26)$$

The oxidation source term is calculated considering the number of carbon atoms removed from soot through each oxidation pathway by

$$S_{ox}^C = -(2\omega_{o2} + \omega_{oh})/\rho, \quad (2.27)$$

2.7 Inception

The inception is described using reactive dimerization of polycyclic aromatic hydrocarbons (PAHs) [18] where collision of two PAH molecules form physically-bonded dimers followed by their carbonization that results in new soot particles. This two step process can be described as



$$\text{Dimer}_{ij}^* \xrightarrow{k_{REAC}} \text{Dimer}_{ij}. \quad (2.29)$$

In Equation (2.28), k_{FWD} is the forward rate of physical dimerization and computed as

$$k_{FWD} = 2.2 \cdot 0.1 \cdot Av \cdot d_{ij}^2 \sqrt{\frac{8\pi k_B T}{m_{ij}}}, \quad (2.30)$$

where $d_{ij} = 2d_i d_j / (d_i + d_j)$ and $m_{ij} = m_i m_j / (m_i + m_j)$ are reduced diameter and mass of PAH molecules in the dimer, respectively. The mass of PAH is calculated by dividing the molecular weight by Avogadro's number. The diameter is estimated by assuming a sphere with the mass of one PAH molecule and an estimated density [19] using

$$m_{PAH} = \frac{W_{PAH}}{Av}, \quad (2.31)$$

$$\rho_{PAH} = 171943.5197 \frac{n_{C,PAH} W_{carbon} + n_{H,PAH} W_{hydrogen}}{n_{C,PAH} + n_{H,PAH}}, \quad (2.32)$$

$$V_{PAH} = \frac{m_{PAH}}{\rho_{PAH}}, \quad (2.33)$$

$$d_{PAH} = \left(\frac{6V_{PAH}}{\pi} \right)^{1/3}. \quad (2.34)$$

The reverse rate of physical dimerization, k_{REV} , is calculated from k_{FWD} and equilibrium coefficient of physical dimerization as

$$k_{REV} = k_{FWD} 10^{-b} e^{-a\epsilon \ln(10)/(RT)}, \quad (2.35)$$

$$\epsilon = cW_{ij} - d, \quad (2.36)$$

where $W_{ij} = W_i W_j / (W_i + W_j)$ is the reduced molecular mass of dimer, $a = 0.115$ (obtained from pyrere dimerization data [20]) and $b = 1.8$ [18], $c = 933420$ j/kg, and $d = 34053$ j/mol [18].

The rate of chemical bond formation, k_{REAC} is defined in the Arrhenius form [6] as

$$k_{REAC} = 5 \times 10^6 \cdot e^{(-96232/RT)}. \quad (2.37)$$

Assuming a steady state condition for the physical dimers, $\partial[\text{Dimer}_{ij}^*]/\partial t = 0$, the formation of dimer can be obtained as

$$\omega_{dimer_{ij}} = k_{REAC} \frac{k_{FWD} [PAH_i][PAH_j]}{k_{REV} + k_{REAC}}. \quad (2.38)$$

The PAHs forming the dimer is removed from the gas mixture due to inception at the same rate as dimerization meaning that

$$\omega_{PAH_i} = \omega_{PAH_j} = -\omega_{dimer_{ij}}. \quad (2.39)$$

Here, we assume the smallest soot particle are 2 nm in diameter corresponding to a spherical particle with 378 carbon and 20 hydrogen atoms, respectively. The contribution of each dimer to number density (both agglomerates and primary particles), carbon and hydrogen content of particles is proportional to the mass, number of carbon and hydrogen atoms of that dimer, respectively, which is described by

$$S_{inc}^N = \sum_{i=1}^n \sum_{j=i}^n \frac{C_{ij}}{C_{min}} \omega_{dimer_{ij}}, \quad (2.40)$$

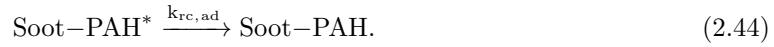
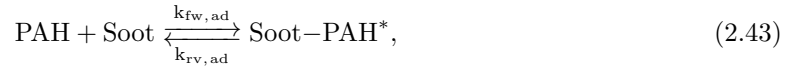
$$S_{inc}^C = \sum_{i=1}^n \sum_{j=i}^n C_{ij} \omega_{dimer_{ij}}, \quad (2.41)$$

$$S_{inc}^H = \sum_{i=1}^n \sum_{j=i}^n H_{ij} \omega_{dimer_{ij}}, \quad (2.42)$$

where C_{ij} and H_{ij} are number of carbon and hydrogen atoms in $dimer_{ij}$, respectively. n is the number of PAHs designated as soot precursors. Note that, Equation (2.40) approximates the mass of soot as mass of carbon atoms comprising the particle.

2.8 Surface growth via PAH adsorption

The adsorption of PAHs on the surface is a major mass growth pathway of soot particles. Here, a two-step process, similar to inception, is used to address the PAH adsorption. The collision of PAH molecule leads to physically bonded, Soot – PAH*, that is followed by chemical bond formation, and completes the adsorption process. The following reactions describes the process



The forward rate of physical adsorption, $k_{fw,ad}$, in Equation (2.45) is computed by harmonic mean of collision frequency of soot particles and PAH molecules in free molecular and continuum regime as

$$k_{fw,ad} = \frac{\beta_{fm,ad} \cdot \beta_{cont,ad}}{\beta_{fm,ad} + \beta_{cont,ad}} Av, \quad (2.45)$$

where $\beta_{fm,ad}$ is obtained [6] as

$$\beta_{fm,ad} = 2.2 \sqrt{\frac{\pi k_B T}{2} \left(\frac{1}{m_{agg}} + \frac{1}{m_{PAH}} \right)} (d_g + d_{PAH})^2, \quad (2.46)$$

where $m_{agg} = C_{tot} \cdot W_{carbon} / (N_{agg} \cdot Av)$ is the mass of soot agglomerate. $\beta_{cont,ad}$ is computed by

$$\beta_{cont,ad} = \frac{2k_B T}{3\mu} \left[\frac{C_s(d_m)}{d_g} + \frac{C_s(d_{PAH})}{d_{PAH}} \right] (d_g + d_{PAH}), \quad (2.47)$$

$$C_s(d) = 1 + \frac{2\lambda}{d} \left[1.21 + 0.4e^{(-0.78d/\lambda)} \right] (d_g + d_{PAH}). \quad (2.48)$$

The reverse rate of physical adsorption, $k_{rv,ad}$, is computed similar to reverse physical inception rate (Equation (2.35)) as

$$k_{rv,ad} = k_{fw,ad} 10^{-b} e^{-a\epsilon \ln(10)/(RT)}, \quad (2.49)$$

$$\epsilon = c \frac{MW_{soot} \cdot MW_{PAH}}{MW_{soot} + MW_{PAH}} - d, \quad (2.50)$$

where $MW_{soot} = C_{tot} \cdot W_{carbon} / N_{agg}$ is the equivalent molecular weight of soot, and a , b , c , and d have the same values as Equation (2.35).

The rate of chemical adsorption, $k_{rc,ad}$ is defined in the Arrhenius form [6] as

$$k_{rc,ad} = 2 \times 10^{10} \cdot e^{(-96232/RT)}. \quad (2.51)$$

The total adsorption rate can be calculated assuming a steady-state concentration for physically adsorbed PAH on soot, $\partial[Soot - PAH^*]/\partial t = 0$, similar to inception rate (Equation (2.39)) as

$$\omega_{pah,ad} = k_{rc,ad} \frac{k_{fw,ad}[\text{Soot}][\text{PAH}]}{k_{rv,ad} + k_{rc,ad}}, \quad (2.52)$$

$$[\text{Soot}] = \rho N_{agg}. \quad (2.53)$$

The contribution of PAH adsorption rate to particle carbon and hydrogen content is computed as

$$S_{grow|ad}^C = \sum_{i=1}^n C_{PAH,i} \cdot \omega_{pah,ad,i}, \quad (2.54)$$

$$S_{grow|ad}^H = \sum_{i=1}^n (H_{PAH,i} - 2) \cdot \omega_{pah,ad,i}. \quad (2.55)$$

The rate of removal of PAH from gas mixture due to adsorption is given as

$$\omega_{PAH,i} = -\omega_{pah,ad,i}. \quad (2.56)$$

The total growth rate is sum of growth due by HACA and adsorption as

$$S_{grow}^C = S_{grow|HACA}^C + S_{grow|ad}^C, \quad (2.57)$$

$$S_{grow}^H = S_{grow|HACA}^H + S_{grow|ad}^H. \quad (2.58)$$

Chapter 3

Implementation

3.1 Overview

This chapter gives general instructions on how to implement the new library and compile it into OpenFOAM combustion models. Note that, the included code was developed at the time of writing the report, and it might change in the future. The reader is encouraged to refer to github repository ¹ for updated version. The implementation steps (sections and subsections) are not designed in the sequential order, but rather in a manner that makes it easy for the reader to connect the parts of the code with different parts of the theory of soot model. Note that, the whole code is shown in the chapter. The symbol ... in the code listings means that part of code is skipped. Reader can refer to the supplementary material that accompanies this report to access the full code.

Let us clarify some of the naming conventions specific to this library. The member data that starts with **PAH** stores information of PAH (soot precursors). **dimer** indicate the member data related to dimer (combination of two PAH molecules). **species** refers to all species used in HACA, inception and adsorption. **index** refers to the index of species in the species list in the thermodynamic file provided by user in **constant** directory. **id** denotes either the index of a species in **speciesList_** (saved in **speciesIds_**) or index of a PAH in **PAH_Names_**.

Figure 3.1 illustrates the general workflow of **laminarSoot**. Black color indicates functions and data that exist in the original library and red color denotes the parts implemented by this work. The main procedures are added to **correct()** function, and the reaction rates and heat release are passed to **reactingFoam**.

3.2 Creating the base library

The implementation begins with making a copy of **laminar** directory and renaming it to **laminarSoot** in **\$FOAM_SRC/combustionModels** path, and modifying the library name using following commands

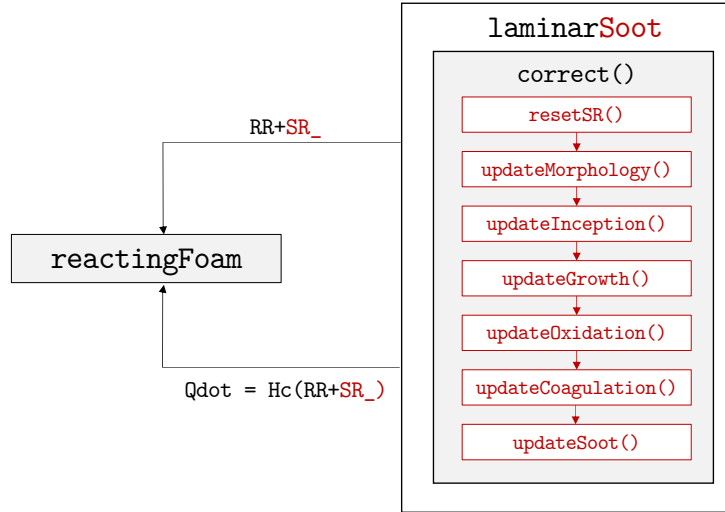
```
1 foam
2 mkdir $WM_PROJECT_USER_DIR/src/laminarSoot
3 cp -r $FOAM_SRC/combustionModels/laminar $WM_PROJECT_USER_DIR/src/laminarSoot
4 cd $WM_PROJECT_USER_DIR/src/laminarSoot
5 mv laminar.H laminarSoot.H
6 mv laminar.C laminarSoot.C
7 mv laminars.H laminarSoots.H
8 sed -i s/"laminar"/"laminarSoot"/g *.*
```

Note that, the new library should include a **Make/files** and **Make/options**

Make/files

```
1 laminarSoots.C
```

¹<https://github.com/mohammadadib-cu/laminarSoot>

Figure 3.1: The general procedure of how `laminarSoot` works and communicates with `reactingFoam`

```

2
3 LIB = $(FOAM_USER_LIBBIN)/liblaminarSoot

```

Make/options

```

1 EXE_INC = \
2   -I$(LIB_SRC)/finiteVolume/lnInclude \
3   -I$(LIB_SRC)/meshTools/lnInclude \
4   -I$(LIB_SRC)/transportModels/compressible/lnInclude \
5   -I$(LIB_SRC)/thermophysicalModels/basic/lnInclude \
6   -I$(LIB_SRC)/thermophysicalModels/specie/lnInclude \
7   -I$(LIB_SRC)/thermophysicalModels/reactionThermo/lnInclude \
8   -I$(LIB_SRC)/thermophysicalModels/chemistryModel/lnInclude \
9   -I$(LIB_SRC)/TurbulenceModels/turbulenceModels/lnInclude \
10  -I$(LIB_SRC)/TurbulenceModels/compressible/lnInclude \
11  -I$(LIB_SRC)/combustionModels/lnInclude \
12
13 LIB_LIBS = \
14   -lfiniteVolume \
15   -lmeshTools \
16   -lcompressibleTransportModels \
17   -lspecie \
18   -lfluidThermophysicalModels \
19   -lreactionThermophysicalModels \
20   -lchemistryModel \
21   -lturbulenceModels \
22   -lcompressibleTurbulenceModels

```

First, two necessary header files are added to `laminarSoot.C` using the `include` statement as

laminarSoot.C

```

1 #include "laminarSoot.H"
2 #include "fvnSup.H"
3 #include "localEulerDdtScheme.H"
4 //-additional header files
5 #include "IFstream.H"
6 #include "fvOptions.H"

```

"`IFstream.H`" is used to read thermodynamic file of reaction mechanism to extract PAH molecules information, and "`fvOptions.H`" is used in solving transport equations.

3.3 Model Constants

We declare the constants used in the soot model as static members of `laminarSoot` class in `laminarSoot.H` after the definition of the class

```

laminarSoot.H
1 template<class ReactionThermo>
2 class laminarSoot
3 :
4     public ChemistryCombustion<ReactionThermo>
5 {
6     // Static data
7     static const label pi_ = Foam::constant::mathematical::pi;
8     static const Foam::dimensionedScalar Av_;
9     static const Foam::dimensionedScalar kB_;
10    static const Foam::dimensionedScalar Ru_;
11    static const Foam::dimensionedScalar rho_soot_;
12    static const Foam::dimensionedScalar W_carbon_;
13    static const Foam::dimensionedScalar W_hydrogen_;
14    static const Foam::dimensionedScalar C_min_;
15    static const Foam::dimensionedScalar H_min_;
16    static const Foam::dimensionedScalar PAH_rho_const_;

```

The value and dimension of these constants are assigned in `laminarSoot.C`. For the sake of brevity only the definition of `Av_` and `kB_` is shown, which refers to Avogadro's number and Boltzmann constant, respectively. The rest of constants are defined the same way.

```

laminarSoot.C
1 // Static data
2 template<class ReactionThermo> const Foam::dimensionedScalar
3 Foam::combustionModels::laminarSoot<ReactionThermo>::Av_ =
4     Foam::dimensionedScalar(
5         "Av",
6         Foam::dimensionSet(0,0,0,0,-1,0,0),
7         scalar(6.0221409e+23)
8     );
9
10 template<class ReactionThermo> const Foam::dimensionedScalar
11 Foam::combustionModels::laminarSoot<ReactionThermo>::kB_ =
12     Foam::dimensionedScalar(
13         "kB",
14         Foam::dimensionSet(1,2,-2,-1,0,0,0),
15         scalar(1.38064852e-23)
16     );
17 ...

```

The mathematical symbol, static member name, value and unit for each model constant are listed in Table 3.1.

3.4 Soot Properties, PAHs, Dimers, and Species

The new library reads `sootProperties` from `constant` directory of the case. `sootProps_` is the member data referring to this dictionary declared in `laminarSoot.H` along with flags for turning on/off different functionalities in the soot model.

```

laminarSoot.H
1 // Soot properties dictionary
2 const IOdictionary sootProps_;
3 // Inception Flag
4 bool inception_enabled_;
5 // HACA Surface growth Flags
6 bool HACA_growth_enabled_;

```

Table 3.1: The description of model constants

Symbol	Static member	Value	Unit
π	pi_	C++ M_PI	-
A_v	Av_	6.0221409e+23	1/mol
k_B	kB_	1.38064852e-23	$\frac{\text{kg}\cdot\text{m}^2}{\text{s}^2\cdot\text{K}}$
R	Ru_	8.314462618	$\frac{\text{kg}\cdot\text{m}^2}{\text{s}^2\cdot\text{K}\cdot\text{mol}}$
ρ_{soot}	rho_soot_	1800	$\frac{\text{kg}}{\text{m}^3}$
W_{carbon}	W_carbon_	12.011e-3	$\frac{\text{kg}}{\text{mol}}$
W_{hydrogen}	W_hydrogen_	1.00784e-3	$\frac{\text{kg}}{\text{mol}}$
C_{min}	C_min_	378	-
H_{min}	H_min_	20	-
-	PAH_rho_const_	171943.5197	mol/m^3

```

7 // Surface oxidation Flag
8 bool HACA_oxidation_enabled_;
9 // PAH Surface growth Flags
10 bool PAH_growth_enabled_ ;
11 // Coagulation flag
12 bool coagulation_enabled_;
13 // Gas scrubbing flag
14 bool scrubbing_enabled_;

```

These member data are initialized in the definition of `laminarSoot` class in `laminarSoot.C` after `integrateReactionRate_`. The first argument of `IObject` determines the file name from `constant` directory. The soot flags are initialized by `getOrDefault` function, meaning that if the flag is not available in `sootProperties`, the default value provided as the second argument of `getOrDefault` is used (`true` in this case).

laminarSoot.C

```

1 sootProps_
2 (
3     IObject
4     (
5         "sootProperties",
6         this->mesh().time().constant(),
7         this->mesh(),
8         IObject::MUST_READ_IF_MODIFIED,
9         IObject::NO_WRITE
10    )
11 ),
12 inception_enabled_(sootProps_.getOrDefault("inception_enabled", true)),
13 HACA_growth_enabled_(sootProps_.getOrDefault("HACA_growth_enabled", true)),
14 HACA_oxidation_enabled_(sootProps_.getOrDefault("HACA_oxidation_enabled", true)),
15 PAH_growth_enabled_(sootProps_.getOrDefault("PAH_growth_enabled", true)),
16 coagulation_enabled_(sootProps_.getOrDefault("coagulation_enabled", true)),
17 scrubbing_enabled_(sootProps_.getOrDefault("scrubbing_enabled", true)),

```

The library also requires a list of precursor PAHs used in inception and PAH adsorption read from `sootProperties` under the keyword `PAHs` into `PAH_names_`. This keyword is mandatory and the names of species provided must be available in the species list in the chemistry file. `PAH_names_` is initialized in the definition of `laminarSoot` class in `laminarSoot.C`

laminarSoot.C

```

1 PAH_names_
2 (
3     sootProps_.lookup("PAHs")

```

```
4 ),
```

Three additional functions are called in the constructor after reading and checking the `integrateReactionRate_`, which is part of the original `laminar` library.

laminarSoot.C

```
1  if (integrateReactionRate_)
2  {
3      Info<< "    using integrated reaction rate" << endl;
4  }
5  else
6  {
7      Info<< "    using instantaneous reaction rate" << endl;
8  }
9  //- Additional functions
10 createPAHProps();
11 createDimerProps();
12 createSpeciesProps();
```

Note that, all of the function must be declared in the header file.

laminarSoot.H

```
1  virtual bool createPAHProps();
2  virtual void createDimerProps();
3  virtual void createSpeciesProps();
```

`createPAHProps` creates a dictionary, `thermoDict`, from the file given provided under `foamChemistryThermoFile` keyword loops through name in `PAH_names_`, and finds the names in `thermoDict` to determine number of carbon and hydrogen and specie's index and save them into `PAH_n_C_`, `PAH_n_H_`, `PAH_indicies_`, respectively.

laminarSoot.C

```
1  template<class ReactionThermo>
2  bool Foam::combustionModels::laminarSoot<ReactionThermo>::createPAHProps()
3  {
4      Info << "PAH names: " << PAH_names_ << endl;
5      PAH_n_C_.resize(PAH_names_.size());
6      PAH_n_H_.resize(PAH_names_.size());
7      PAH_indicies_.resize(PAH_names_.size());
8
9      const ReactionThermo& thermo = this->thermo();
10     const dictionary thermoDict = IFstream(fileName(thermo.lookup("foamChemistryThermoFile"))).expand()
11     ();
12
13     forAll(PAH_names_, i)
14     {
15         PAH_indicies_[i] = this->thermo().composition().species()[PAH_names_[i]];
16         const dictionary* elemsDict = thermoDict.subDict(PAH_names_[i]).findDict("elements");
17         wordList elemNames(elemsDict->toc());
18     }
```

`createDimerProps` creates possible dimer combinations from `PAH_names_` and saves number of carbon, and hydrogen atoms of each dimer as well as index and id of PAHs in the dimer.

laminarSoot.C

```
1  template<class ReactionThermo>
2  bool Foam::combustionModels::laminarSoot<ReactionThermo>::createDimerProps()
3  {
4      ...
5      for (int i = 0; i < PAH_names_.size(); i++) {
6          for (int j = i; j < PAH_names_.size(); j++) {
7              dimer_id += 1;
8              dimer_names_[dimer_id] = PAH_names_[i] + PAH_names_[j];
9              dimer_n_C_[dimer_id] = PAH_n_C_[i] + PAH_n_C_[j];
```

```

10     dimer_n_H[dimer_id] = PAH_n_H[i] + PAH_n_H[j];
11     dimer_PAH_1_index[dimer_id] = composition.species()[PAH_names_[i]];
12     dimer_PAH_2_index[dimer_id] = composition.species()[PAH_names_[j]];
13     dimer_PAH_1_id[dimer_id] = i;
14     dimer_PAH_2_id[dimer_id] = j;
15 }
16 }
17 ...

```

`createSpeciesProps` creates a list of all species, which is a combination of `PAH_Names_` and `HACASpeciesList_` (species used in HACA mechanism). It stores the name and id of species in `speciesList_` and `speciesIds_`, respectively. After that, it initializes `SR_`, which is a list of pointers to `volScalarFields` that store the rate removal/addition of species from/to gaseous mixture. The role of `SR_` is further explained in Section 3.8.

laminarSoot.C

```

1  template<class ReactionThermo>
2  void Foam::combustionModels::laminarSoot<ReactionThermo>::createSpeciesProps()
3  {
4      basicSpecieMixture& composition = this->thermo().composition();
5
6      forAll(PAH_names_, i){
7          speciesList_[i] = PAH_names_[i];
8      }
9      forAll(HACASpeciesList_, i){
10         label spid = i + PAH_names_.size();
11         speciesList_[spid] = HACASpeciesList_[i];
12     }
13     Info << "List of species: " << speciesList_ << endl;
14
15
16     forAll(speciesList_, i)
17     {
18         const label specieIndex = composition.species()[speciesList_[i]];
19         if (!composition.species().found(speciesList_[i]))
20         {
21             FatalIOErrorIn("laminarSoot::findIndices()", this->thermo())
22                 << speciesList_[i] << " is not found in available species "
23                 << composition.species() << exit(FatalIOError);
24         }
25         speciesIndices_.insert
26         (
27             speciesList_[i],
28             specieIndex
29         );
30         speciesIds_.insert
31         (
32             speciesList_[i],
33             i
34         );
35         Info << speciesList_[i] << " is found! Index= " << speciesIndices_[speciesList_[i]] << " Id: "
36             << speciesIds_(speciesList_[i]) << endl;
37     }
38
39     // Create the fields for the chemistry sources
40     forAll(SR_, fieldi)
41     {
42         SR_.set
43         (
44             fieldi,
45             new volScalarField::Internal
46             (
47                 IOobject
48                 (
49                     "SR." + speciesList_[fieldi],
50                     this->mesh().time().timeName(),

```

```

50         this->mesh(),
51         IOobject::NO_READ,
52         IOobject::NO_WRITE
53     ),
54     this->mesh(),
55     dimensionedScalar(dimMass/dimVolume/dimTime, Zero)
56 )
57 );
58 }
59 }

```

3.5 Tracked and Derived Fields

Here, we declare and initialize the four *tracked* fields, N_{agg} , N_{pri} , C_{tot} , H_{tot} , and fields *derived* from tracked fields and thermodynamic properties of gas mixture. These fields describe soot morphology (needs to be written at each time step) and source terms. The declaration are added to `laminarSoot.H` after the scrubbing flag.

`laminarSoot.H`

```

1  ...
2  // Soot tracked fields
3  volScalarField N_agg_;
4  volScalarField N_pri_;
5  volScalarField C_tot_;
6  volScalarField H_tot_;
7  // Morphology
8  volScalarField n_p_;
9  volScalarField d_p_;
10 volScalarField d_m_;
11 volScalarField d_g_;
12 volScalarField A_tot_;
13 // Source Terms
14 // Inception
15 volScalarField S_inc_N_;
16 volScalarField S_inc_C_tot_;
17 volScalarField S_inc_H_tot_;
18 // Surface growth
19 volScalarField S_grow_C_tot_;
20 volScalarField S_grow_H_tot_;
21 // Oxidation
22 volScalarField S_ox_C_tot_;
23 // Coagulation
24 volScalarField S_coag_N_agg_;
25 ...

```

The main tracked fields are read from the first time directory (0), so they are initialized using `MUST_READ` keyword. Here, only the definition of `N_agg_` (corresponds to N_{agg} in the model) is provided in the code below, and the rest of tracked fields are defined similarly.

`laminarSoot.C`

```

1  ...
2  N_agg_
3  (
4      IOobject
5      (
6          "N_agg",
7          this->mesh().time().timeName(),
8          this->mesh(),
9          IOobject::MUST_READ,
10         IOobject::AUTO_WRITE
11     ),
12     this->mesh()
13 ),

```

14 ...

However, the derived fields and source terms are only written in the time directories by running the case, so they are initialized using `NO_READ` keyword. Here, the initialization of `n_p_` (corresponds to n_p in the model) is given.

laminarSoot.C

```

1  ...
2  n_p_
3  (
4      IOobject
5      (
6          "n_p",
7          this->mesh().time().timeName(),
8          this->mesh(),
9          IOobject::NO_READ,
10         IOobject::AUTO_WRITE
11     ),
12     this->mesh(), dimensionedScalar("n_p", dimensionSet(0,0,0,0,0,0,0),1.0)
13 ),
14 ...

```

3.5.1 Tracked field functions

Four additional functions are defined in `laminarSoot.H` with similar names to tracked fields to return the tracked fields.

laminarSoot.H

```

1  //- Return the number concentration of agglomerates N_agg
2  // Units: mol/kg
3  virtual tmp<volScalarField> N_agg() const
4  {
5      return N_agg_;
6  };
7  //- Return the number concentration of primary particles N_pri
8  // Units: mol/kg
9  virtual tmp<volScalarField> N_pri() const
10 {
11     return N_pri_;
12 };
13 //- Return the carbon content of soot C_tot
14 // Units: mol/kg
15 virtual tmp<volScalarField> C_tot() const
16 {
17     return C_tot_;
18 };
19 //- Return the carbon content of soot H_tot
20 // Units: mol/kg
21 virtual tmp<volScalarField> H_tot() const
22 {
23     return H_tot_;
24 };

```

3.6 Gas properties

Some of member functions of `laminarSoot` are used to calculate additional gas properties used by the soot model. These functions are declared and defined in `laminarSoot.H`

3.6.1 W(index) function

This function receives the index of a specie and returns the molecular weight in kg/mol as a `dimensionedScalar`. Note that, `composition.W(index)` returns a scalar (non-dimensional) equal to molecular weight of a specie in kmol/kg.

```

laminarSoot.H
1  virtual dimensioned<scalar> W(label index)
2  {
3      basicSpecieMixture& composition = this->thermo().composition();
4      return composition.W(index) / 1000.0 * dimensionedScalar(dimensionSet(1,0,0,0,-1,0,0),
5      scalar(1));
6  }

```

3.6.2 C(index) function

This function takes the index of a specie as an argument and returns the concentration as a `tmp<volScalarField>` from mass fraction, `Y`, using the ideal gas law.

```

laminarSoot.H
1  virtual tmp<volScalarField> C(label index)
2  {
3      basicSpecieMixture& composition = this->thermo().composition();
4      return tmp<volScalarField>
5      (
6          new volScalarField
7          (
8              "C",
9              (composition.Y()[index] * this->thermo().rho() / W(index))
10         )
11     );
12 }
13

```

3.6.3 lambda_gas() function

This function calculates mean free path of gas (corresponding to Equation (2.12)).

```

laminarSoot.H
1  virtual tmp<volScalarField> lambda_gas() const
2  {
3      return tmp<volScalarField>
4      (
5          new volScalarField
6          (
7              max
8              (
9                  this->thermo().mu() / this->thermo().rho() * pow(pi_ * this->thermo().W() /
10 (2.0* kB_ * Av_ * this->thermo().T()), 0.5),
11                  dimensionedScalar(dimensionSet(0,1,0,0,0,0,0), SMALL)
12              )
13          );
14 }
15

```

3.7 PAH Characteristics

3.7.1 m_PAH(id) function

This function takes the id of a PAH and returns the mass of one PAH molecule according to Equation (2.31).

```

laminarSoot.H
1 Info<< "Reading field N_agg\n" << endl;
2     virtual dimensioned<scalar> m_PAH(label id)
3     {
4         label index = PAH_indicies_[id];
5         return W(index) / Av_;
6     };
7 }

```

3.7.2 d_PAH(id) function

This function takes the id of a PAH and returns diameter of one PAH molecule according to Equations 2.32-2.34.

```

laminarSoot.H
1     virtual dimensioned<scalar> d_PAH(label id)
2     {
3         const dimensionedScalar rho_PAH = PAH_rho_const_ * (W_carbon_ * PAH_n_C_[id] + W_hydrogen_
4         * PAH_n_H_[id]) / (PAH_n_C_[id] + PAH_n_H_[id]);
5         const dimensionedScalar V_PAH = m_PAH(id) / rho_PAH;
6         return pow(6.0 * V_PAH / pi_, 1.0/3.0);
7     };

```

3.8 Modifying R(Y) function

R(Y) takes the mass traction field of a specie, Y, as an argument and returns its production/consumption rate in $\text{kg.m}^{-3}.\text{s}$. We modified this function in such a way that it looks for the name of provided species (accessible through `Y.member()`) in `speciesList_`, and if available, `SR_` of that specie is added to `Su`. Note that, `RR()` return the rate of production/destruction of species calculated using the reactions defined in the chemistry file (reaction mechanism) in the Arrhenius form. However, soot inception, growth (via HACA and adsorption) and oxidation also transforms a fraction of species into soot mass or releases some species into gas mixture. In essence, `SR_` accounts for the rate of addition/removal of any specie involved in the soot formation.

```

laminarSoot.C
1 template<class ReactionThermo>
2 Foam::tmp<Foam::fvScalarMatrix>
3 Foam::combustionModels::laminarSoot<ReactionThermo>::R(volScalarField& Y) const
4 {
5     tmp<fvScalarMatrix> tSu(new fvScalarMatrix(Y, dimMass/dimTime));
6
7     fvScalarMatrix& Su = tSu.ref();
8
9     if (this->active())
10    {
11        const label specieI =
12            this->thermo().composition().species()[Y.member()];
13
14        Su += this->chemistryPtr_->RR(specieI);
15        // scrubbing rates are added
16        if (scrubbing_enabled_){
17            if (speciesList_.found(Y.member()))

```

```

18     {
19         label spid = speciesIds_[Y.member()];
20         Su += SR_[spid];
21     }
22 }
23 }
24
25 return tSu;
26 }

```

3.9 Modifying Qdot() function

Qdot calculates the rate of energy change by production/consumption of species due to chemical reactions. Here, we modify this function to incorporate the contribution of addition/removal of species by soot formation to energy release. The process is similar to modification of R(Y) function. The rate of energy change is calculated by multiplying chemical enthalpy (`this->thermo().composition().Hc(i)`) to sum of RR and SR_.

laminarSoot.C

```

1  template<class ReactionThermo>
2  Foam::tmp<Foam::volScalarField>
3  Foam::combustionModels::laminarSoot<ReactionThermo>::Qdot() const
4  {
5      tmp<volScalarField> tQdot
6      (
7          new volScalarField
8          (
9              IOobject
10             (
11                 this->thermo().phasePropertyName(typeName + ":Qdot"),
12                 this->mesh().time().timeName(),
13                 this->mesh(),
14                 IOobject::NO_READ,
15                 IOobject::NO_WRITE,
16                 false
17             ),
18             this->mesh(),
19             dimensionedScalar(dimEnergy/dimVolume/dimTime, Zero)
20         )
21     );
22
23     if (this->active())
24     {
25         if (scrubbing_enabled_){
26             scalarField& Qdot = tQdot.ref();
27             forAll(this->thermo().composition().Y(), i)
28             {
29                 if (speciesList_.found(this->thermo().composition().Y()[i].member()))
30                 {
31                     label spid = speciesIds_[this->thermo().composition().Y()[i].member()];
32                     forAll(Qdot, celli)
33                     {
34                         const scalar hi = this->thermo().composition().Hc(i);
35                         Qdot[celli] -= hi*(this->chemistryPtr_->RR(i)[celli]+SR_[spid][celli]);
36                     }
37                 }else{
38                     forAll(Qdot, celli)
39                     {
40                         const scalar hi = this->thermo().composition().Hc(i);
41                         Qdot[celli] -= hi*this->chemistryPtr_->RR(i)[celli];
42                     }
43                 }
44             }
45         }else{

```

```

46         tQdot.ref() = this->chemistryPtr_->Qdot();
47     }
48 }
49 return tQdot;
50 }

```

3.10 Modifying `correct()` function

`correct` function is called each time before solving the species concentration, `YEqn`, by `reactingFoam`. We add functions that needs to be called at each iteration to calculate the source terms and solves the soot equations. These functions must be called in the correct order to produced the precises results.

laminarSoot.C

```

1 Info<< "Reading field N_agg\n" << endl;
2 template<class ReactionThermo>
3 void Foam::combustionModels::laminarSoot<ReactionThermo>::correct()
4 {
5     ...
6     //- additional functions
7     resetSR();
8     updateMorphology();
9     updateInception();
10    updateGrowth();
11    updateOxidation();
12    updateCoagulation();
13    updateSoot();
14    ...
15 }

```

Note that, all of these functions must be declared in the header file.

laminarSoot.H

```

1 virtual void resetSR();
2 virtual void updateMorphology();
3 virtual void updateInception();
4 virtual void updateGrowth();
5 virtual void updateOxidation();
6 virtual void updateCoagulation();
7 virtual void updateSoot();

```

3.11 Resetting scrubbing rates by `resetSR()`

`resetSR` loops through fields inserted in `SR_`, and then iterates through cells of each fields and zeros the values of that field.

laminarSoot.C

```

1 template<class ReactionThermo>
2 void Foam::combustionModels::laminarSoot<ReactionThermo>::resetSR()
3 {
4     if (scrubbing_enabled){
5         forAll(SR_, fieldi){
6             forAll(SR_[fieldi], celli){
7                 SR_[fieldi][celli] = 0.0;
8             }
9         }
10    }
11 }

```

3.12 Updating soot morphology

3.12.1 V_agg() function

This function returns the volume of agglomerates.

```

laminarSoot.C
1  virtual tmp<volScalarField> V_agg()
2  {
3      return tmp<volScalarField>
4      (
5          new volScalarField
6          (
7              C_tot() * W_carbon_ / (rho_soot_ * N_agg() * Av_)
8          )
9      );
10 }
```

3.12.2 m_agg() function

This function returns the mass of agglomerates.

```

laminarSoot.C
1  virtual tmp<volScalarField> m_agg()
2  {
3      return tmp<volScalarField>
4      (
5          new volScalarField
6          (
7              C_tot() * W_carbon_ / (N_agg() * Av_)
8          )
9      );
10 }
```

3.12.3 updateMorphology() function

updateMorphology uses the tracked fields to calculate derived fields that characterize the soot morphology n_p , d_p , d_m , and d_n . Note that, `n_p.max(1.0)` enforces $n_p \geq 1$ condition. This function is related to Equations 2.5-2.8 in Section 2.2.

```

laminarSoot.C
1  template<class ReactionThermo>
2  void Foam::combustionModels::laminarSoot<ReactionThermo>::updateMorphology()
3  {
4      // number of primary particles
5      n_p_ = N_pri() / N_agg();
6      n_p_.max(1.0);
7      if (!coagulation_enabled_)
8      {
9          Info<< "enforcing n_p = 1\n" << endl;
10         n_p_.min(1.00000001);
11     }
12     // Primary particle diameter
13     d_p_ = pow (
14         (6.0 / pi_) *
15         (C_tot() * W_carbon_) / rho_soot_ *
16         1.0 / (N_pri() * Av_)
17         , 1.0/3.0
18     );
19     // Surface area of each primary particle
20     A_tot_ = N_pri() * Av_ * pi_ * d_p_ * d_p_;
21     // Mobility diameter
```

```

22 d_m_ = d_p_ * pow(n_p_, 0.45);
23 // Gyration Diameter
24 volScalarField n_p_lowerlimit (n_p_*0.0+1.5);
25 d_g_ = (n_p_ <= n_p_lowerlimit) * (d_m_ / 1.29) + (n_p_ > n_p_lowerlimit) * (d_m_ / (pow(n_p_,
26 -0.2)+0.4));
27 }

```

3.13 Updating Inception Source Term

3.13.1 updateInception() fuction

updateInception() function loops through the dimers and passes the id of PAHs in the dimer as arguments to dimerROP function to calculate the rate of formation of chemically-bonded dimer. Then, the contribution of each dimer to source terms, S_inc_N_, S_inc_C_tot_, and S_inc_H_tot_ is computed according to Equations 2.40-2.42. After that, the rate scrubbing rate of PAH and hydrogen (released by carbonization of dimer) is added to relevant fields in SR_.

laminarSoot.C

```

1 template<class ReactionThermo>
2 void Foam::combustionModels::laminarSoot<ReactionThermo>::updateInception()
3 {
4     S_inc_N_ *= 0.0;
5     S_inc_C_tot_ *= 0.0;
6     S_inc_H_tot_ *= 0.0;
7     if (inception_enabled_){
8         volScalarField rho = this->thermo().rho();
9         forAll(dimer_names_, i)
10         {
11             // PAH Index and Id
12             label id1 = dimer_PAH_1_id_[i];
13             label id2 = dimer_PAH_2_id_[i];
14             volScalarField dimerROPField(dimerROP(id1, id2));
15             // N_agg Source Term
16             S_inc_N_ += (dimer_n_C_[i] / C_min_) * dimerROPField / rho;
17             // C_tot Source Term
18             S_inc_C_tot_ += dimer_n_C_[i] * dimerROPField / rho;
19             // H_tot Source Term
20             S_inc_H_tot_ += dimer_n_H_[i] * dimerROPField / rho;
21             if (scrubbing_enabled_){
22                 // PAHs
23                 // species id
24                 label spid1 = speciesIds_[PAH_names_[id1]];
25                 label spid2 = speciesIds_[PAH_names_[id2]];
26                 // species index
27                 label spindex1 = speciesIndicies_[PAH_names_[id1]];
28                 label spindex2 = speciesIndicies_[PAH_names_[id2]];
29                 SR_[spid1] -= dimerROPField * W(spindex1);
30                 SR_[spid2] -= dimerROPField * W(spindex2);
31
32                 // H2
33                 label H2_id = speciesIds_["H2"];
34                 label H2_index = speciesIndicies_["H2"];
35                 SR_[H2_id] += dimerROPField * W(H2_index);
36             }
37         }
38     }
39 }

```

3.13.2 dimerROP(id1, id2) function

This function calculates the rate of formation of dimer chemically bonded dimer according to Equation (2.39). The rate of dimer formation cannot be negative, so `max` function is used to enforce this condition.

```

lamiarSoot.H
1  virtual tmp<volScalarField> dimerROP(label id1, label id2)
2  {
3      label index1 = PAH_indicies_[id1];
4      label index2 = PAH_indicies_[id2];
5      return tmp<volScalarField>
6      (
7          new volScalarField
8          (
9              "dimerROP",
10             max
11             (
12                 k_REAC() * k_FWD(id1, id2) * C(index1) * C(index2) / (k_REAC() + k_REV(id1,
13 id2)),
14                 dimensionedScalar(dimensionSet(0,-3,-1,0,1,0,0), scalar(0.0))
15             )
16         );
17     }

```

3.13.3 k_FWD(id1, id2) funtion

This function calculates the forward rate constant for physical dimerization of two PAHs according to Equation (2.30).

```

lamiarSoot.H
1  virtual tmp<volScalarField> k_FWD(label id1, label id2)
2  {
3      const volScalarField& T = this->thermo().T();
4      // reduced dimer diameter
5      const dimensionedScalar d_reduced = 2 * d_PAH(id1) * d_PAH(id2) / (d_PAH(id1) + d_PAH(id2));
6      // reduced dimer mass
7      const dimensionedScalar m_reduced = m_PAH(id1) * m_PAH(id2) / (m_PAH(id1) + m_PAH(id2));
8      return tmp<volScalarField>
9      (
10         new volScalarField
11         (
12             "k_FWD",
13             (1.0 * 2.2 * 0.1 * Av_ * d_reduced * d_reduced * pow(8.0 * pi_ * kB_ * T /
14 m_reduced, 0.5))
15         );
16     };

```

3.13.4 k_REV(id1, id2) funtion

This function calculates the reverse rate constant for physical dimerization of two PAHs according to Equations 2.35 and 2.36.

```

lamiarSoot.H
1  virtual tmp<volScalarField> k_REV(label id1, label id2)
2  {
3      // Constants
4      dimensionedScalar a_k_REV("a_k_REV", dimensionSet(0,0,0,0,0,0,0), scalar(0.115));
5      dimensionedScalar b_k_REV("b_k_REV", dimensionSet(0,0,0,0,0,0,0), scalar(1.8));

```

```

6      dimensionedScalar c_k_REV("c_k_REV", dimensionSet(0,2,-2,0,0,0,0), scalar(933420.0));
7      dimensionedScalar d_k_REV("d_k_REV", dimensionSet(1,2,-2,0,-1,0,0), scalar(34069.0));
8
9      const volScalarField& T = this->thermo().T();
10     label index1 = PAH_indicies_[id1];
11     label index2 = PAH_indicies_[id2];
12     const dimensionedScalar W_reduced = W(index1) * W(index2) / (W(index1) + W(index2));
13     const dimensionedScalar epsilon = c_k_REV * W_reduced - d_k_REV;
14
15     return tmp<volScalarField>
16     (
17         new volScalarField
18         (
19             "k_REV",
20             (k_FWD(id1, id2) * pow(10.0, -b_k_REV) * exp(-a_k_REV * epsilon * 2.3025851/(Ru_ *
T))))
21         )
22     );
23 };

```

3.13.5 k_REAC() function

This function calculates the rate constant for chemical dimerization of two PAHs according to Equation (2.37).

lamiarSoot.H

```

1      virtual tmp<volScalarField> k_REAC()
2      {
3          // Chemical dimerization rate constants
4          dimensionedScalar Ea_k_REAC("Ea_k_REAC", dimensionSet(1,2,-2,0,-1,0,0), scalar(96232.0));
5          dimensionedScalar A_k_REAC("A_k_REAC", dimensionSet(0,3,-1,0,-1,0,0), scalar(5.0e6));
6          const volScalarField& T = this->thermo().T();
7
8          return tmp<volScalarField>
9          (
10             new volScalarField
11             (
12                 "k_REAC",
13                 (A_k_REAC * exp(-Ea_k_REAC/(Ru_ * T)))
14             )
15          );
16      }

```

3.14 Updating soot growth rates

3.14.1 updateGrowth() function

updateGrowth() calculates the growth source terms for transport equations of C_{tot} and H_{tot} in two steps. First, it calculates the HACA rate by HACAGrowthRate(), and adds the contribution of HACA to growth source terms to Equations 2.19 and 2.20. Then, it loops over PAH_names_, calculates adsorption rate by PAHAdsorptionRate() for each PAH, and incorporates it into growth source terms. After each step, SR_ is updated for relevant fields to account for addition/removal of species to/from gas mixtures.

lamiarSoot.C

```

1      template<class ReactionThermo>
2      void Foam::combustionModels::lamiarSoot<ReactionThermo>::updateGrowth()
3      {
4          S_grow_C_tot_ *= 0.0;
5          S_grow_H_tot_ *= 0.0;
6      }

```



```

7   if (HACA_growth_enabled_)
8   {
9       volScalarField rho = this->thermo().rho();
10      volScalarField HACAGrowthRateField(HACAGrowthRate());
11      S_grow_C_tot_ += 2 * HACAGrowthRateField / rho;
12      S_grow_H_tot_ += 2 * HACAGrowthRateField * (0.25 / 2.00) / rho;
13
14      if (scrubbing_enabled_){
15          // C2H2
16          label C2H2_id = speciesIds_["C2H2"];
17          label C2H2_index = speciesIndices_["C2H2"];
18          SR_[C2H2_id] -= HACAGrowthRateField * W(C2H2_index);
19
20          // H
21          label H_id = speciesIds_["H"];
22          label H_index = speciesIndices_["H"];
23          SR_[H_id] += HACAGrowthRateField * W(H_index) * (1.75 / 2.00);
24      }
25  }
26  if (PAH_growth_enabled_)
27  {
28      volScalarField rho = this->thermo().rho();
29      forAll(PAH_names_, id)
30      {
31          volScalarField PAHAdsorptionRateField(PAHAdsorptionRate(id));
32          S_grow_C_tot_ += PAH_n_C_[id] * PAHAdsorptionRateField / rho;
33          S_grow_H_tot_ += (PAH_n_H_[id] - 2) * PAHAdsorptionRateField / rho;
34
35          if (scrubbing_enabled_){
36              // PAH
37              // species id
38              label spid = speciesIds_[PAH_names_[id]];
39              // species index
40              label spindex = speciesIndices_[PAH_names_[id]];
41              SR_[spid] -= PAHAdsorptionRateField * W(spindex);
42
43              // H
44              label H_id = speciesIds_["H"];
45              label H_index = speciesIndices_["H"];
46              SR_[H_id] += PAHAdsorptionRateField * W(H_index) * 2;
47          }
48      }
49  }
50
51 }

```

3.14.2 HACAGrowthRate() function

This function computes the rate of addition of C_2H_2 molecules to soot particle surface via HACA according to Equation (2.17).

lamiaSoot.H

```

1   virtual tmp<volScalarField> HACAGrowthRate()
2   {
3       label C2H2_i = speciesIndices_["C2H2"];
4       return tmp<volScalarField>
5       (
6           new volScalarField
7           (
8               max
9               (
10                  alpha() * k_4_HACA() * C(C2H2_i) * C_soot_0(),
11                  dimensionedScalar(dimensionSet(0,-3,-1,0,1,0,0), scalar(0.0))
12              )
13          )

```

```

14     );
15 }

```

3.14.3 Other HACA-growth-related functions

The rest of functions related to growth rate via HACA defined in `laminarSoot.H` are given in Table 3.2 with parameter name and a references to equation(s) from the soot model used in each function. The source code for these functions are provided in Appendix A.1.

Table 3.2: The description of other HACA-growth-related functions

Function	Parameter	Reference
<code>k_4_HACA()</code>	k_{f4}	Table 2.1 No.4-f
<code>k_5_HACA()</code>	k_{f5}	Table 2.1 No.5-f
<code>k_6_HACA()</code>	k_{f6}	Table 2.1 No.1-f
<code>alpha()</code>	α	Equation (2.21)
		Equation (2.22)
<code>C_soot_0()</code>	$[C_{soot}^o]$	Table 2.1 No.1-f
		Table 2.1 No.1-r
		Table 2.1 No.2-f
		Table 2.1 No.1-r
		Table 2.1 No.3-f

3.14.4 PAHAdsorptionRate(id) function

This function takes the PAH id and calculates the adsorption rate for the given PAH. The forward ($k_{fw,ad}$) and reverse ($k_{rv,ad}$) rates for PAH and soot collision, and chemical bond formation ($k_{rc,ad}$) between soot and PAH molecules are computed inside the function.

```

                                laminarSoot.H
1  virtual tmp<volScalarField> PAHAdsorptionRate(label id)
2  {
3
4      // PAH Index and Id
5      label index = PAH_indicies_[id];
6      // Temperature
7      const volScalarField& T = this->thermo().T();
8      // Density
9      const volScalarField rho = this->thermo().rho();
10     // Viscosity of gas
11     volScalarField mu = this->thermo().mu();
12     // beta fm coag PAH-soot
13     volScalarField beta_fm_soot_PAH
14     (
15         2.2 * pow(pi_ * kB_ * T / 2.0 * (1.0/m_agg() + 1.0/m_PAH(id)), 0.5) * pow(d_g_ + d_PAH
(id), 2.0)
16     );
17     // beta cont coag PAH-soot
18     volScalarField C_s_soot_d_m
19     (
20         1.0 + (2.0 * lambda_gas() / d_m_) * (1.21 + 0.4*exp(-0.78 * d_m_ / lambda_gas()))
21     );
22     volScalarField C_s_soot_d_PAH
23     (
24         1.0 + (2.0 * lambda_gas() / d_PAH(id)) * (1.21 + 0.4*exp(-0.78 * d_PAH(id) /
lambda_gas()))
25     );
26     volScalarField beta_cont_soot_PAH
27     (

```

```

28         2.0 * kB_ * T / (3.0 * mu) * (C_s_soot_d_m / d_g_ + C_s_soot_d_PAH / d_PAH(id)) * (
29         d_g_ + d_PAH(id))
30     );
31     // Forward reaction rate
32     volScalarField k_FWD_soot_PAH
33     (
34         beta_fm_soot_PAH * beta_cont_soot_PAH / (beta_fm_soot_PAH + beta_cont_soot_PAH) * Av_
35     );
36     // W reduced
37     // Constants
38     dimensionedScalar a_k_REV_soot_PAH(dimensionSet(0,0,0,0,0,0,0), scalar(0.115));
39     dimensionedScalar b_k_REV_soot_PAH(dimensionSet(0,0,0,0,0,0,0), scalar(1.8));
40     dimensionedScalar c_k_REV_soot_PAH(dimensionSet(0,2,-2,0,0,0,0), scalar(933420.0));
41     dimensionedScalar d_k_REV_soot_PAH(dimensionSet(1,2,-2,0,-1,0,0), scalar(34053.0));
42     // W soot
43     volScalarField W_soot(C_tot() * W_carbon_ / N_agg());
44     volScalarField epsilon_soot_PAH
45     (
46         c_k_REV_soot_PAH * (W(index) * W_soot) / (W(index) + W_soot) - d_k_REV_soot_PAH
47     );
48     // The reverse rate of physical dimerization
49     volScalarField k_REV_soot_PAH
50     (
51         k_FWD_soot_PAH * pow(10.0, -b_k_REV_soot_PAH) * exp(-a_k_REV_soot_PAH *
52         epsilon_soot_PAH * 2.3025851/(Ru_ * T))
53     );
54     // Chemical adsorption rate
55     dimensionedScalar Ea_k_REAC_soot_PAH(dimensionSet(1,2,-2,0,-1,0,0), scalar(96232.0));
56     dimensionedScalar A_k_REAC_soot_PAH(dimensionSet(0,3,-1,0,-1,0,0), scalar(2.0e10));
57     volScalarField k_REAC_soot_PAH
58     (
59         A_k_REAC_soot_PAH * exp(-Ea_k_REAC_soot_PAH / (Ru_ * T))
60     );
61     return tmp<volScalarField>
62     (
63         new volScalarField
64         (
65             max
66             (
67                 k_REAC_soot_PAH * k_FWD_soot_PAH * C(index) * (N_agg() * rho) / (
68                 k_REAC_soot_PAH + k_REV_soot_PAH),
69                 dimensionedScalar(dimensionSet(0,-3,-1,0,1,0,0), scalar(0.0))
70             )
71         );
72     );
73 }

```

3.15 Updating oxidation rates

3.15.1 updateOxidation() function

This function calculates the rate of oxidation of soot particles by O_2 (HACA02OxidationRate) and OH (HACA0HOxidationRate) and adds their contribution to oxidation source term. Also, the rate of removal of O_2 and OH and addition of CO to the gas mixture are added to SR_- .

lamiarSoot.C

```

1 template<class ReactionThermo>
2 void Foam::combustionModels::lamiarSoot<ReactionThermo>::updateOxidation()
3 {
4     S_ox_C_tot_ *= 0.0;
5     if (HACA_oxidation_enabled_){
6         volScalarField rho(this->thermo().rho());
7         volScalarField HACA02OxidationRateField(HACA02OxidationRate());

```

```

8   volScalarField HACA0H0xidationRateField(HACA0H0xidationRate());
9   S_ox_C_tot_ += -1 * (HACA020xidationRateField + HACA0H0xidationRateField) / rho;
10
11  if (scrubbing_enabled){
12      // O2
13      label O2_id = speciesIds_["O2"];
14      label O2_index = speciesIndices_["O2"];
15      SR_[O2_id] -= 0.5 * HACA020xidationRateField * W(O2_index);
16
17      // CO2
18      label CO_id = speciesIds_["CO"];
19      label CO_index = speciesIndices_["CO"];
20      SR_[CO_id] += (HACA020xidationRateField + HACA0H0xidationRateField) * W(CO_index);
21
22      // OH
23      label OH_id = speciesIds_["OH"];
24      label OH_index = speciesIndices_["OH"];
25      SR_[OH_id] -= HACA0H0xidationRateField * W(OH_index);
26  }
27 }
28 }

```

3.15.2 HACA020xidationRate() function

This function returns the rate of oxidation by O₂ according to Equation (2.25).

```

                                lamiaSoot.H
1   virtual tmp<volScalarField> HACA020xidationRate()
2   {
3       label O2_i = speciesIndices_["O2"];
4       volScalarField rho (this->thermo().rho());
5       return tmp<volScalarField>
6       (
7           new volScalarField
8           (
9               max
10              (
11                  2 * alpha() * k_5_HACA() * C(O2_i) * C_soot_0(),
12                  dimensionedScalar(dimensionSet(0,-3,-1,0,1,0,0), scalar(0.0))
13              )
14          );
15      );
16  }

```

3.15.3 HACA0H0xidationRate() function

This function returns the rate of oxidation by OH according to Equation (2.26).

```

                                lamiaSoot.H
1   virtual tmp<volScalarField> HACA020xidationRate()
2   {
3       label O2_i = speciesIndices_["O2"];
4       volScalarField rho (this->thermo().rho());
5       return tmp<volScalarField>
6       (
7           new volScalarField
8           (
9               max
10              (
11                  2 * alpha() * k_5_HACA() * C(O2_i) * C_soot_0(),
12                  dimensionedScalar(dimensionSet(0,-3,-1,0,1,0,0), scalar(0.0))
13              )
14          );

```

```

15     );
16 }

```

3.16 Updating coagulation rate by updateCoagulation()

updateCoagulation() determines the coagulation source term S_{coag}^N . First, it calculates the collision frequency in free molecular (β_{fm}) and continuum (β_{cont}) regime using Equations 2.15 and 2.16, respectively. Then, it uses harmonic mean of collision frequencies considering 82% enhancement factor (Equation (2.14)) and returns the rate coagulation (Equation (2.13)).

lamiarSoot.C

```

1  template<class ReactionThermo>
2  void Foam::combustionModels::laminarSoot<ReactionThermo>::updateCoagulation()
3  {
4      const volScalarField& T = this->thermo().T();
5      volScalarField mu (this->thermo().mu());
6      volScalarField rho (this->thermo().rho());
7      // Free Molecule
8      volScalarField beta_fm
9      (
10         4 * pow(pi_ * kB_ * T / m_agg(), 0.5) * d_g_ * d_g_
11     );
12     // Continuum
13     volScalarField beta_cont(
14         (8 * kB_ / (3 * mu)) * T * ( 1.0 + (2.0 * lambda_gas() / d_m_) * (1.21 + 0.4*exp(-0.78*d_m_/
15             lambda_gas()))))
16     );
17     // Coagulation source term
18     if (coagulation_enabled_){
19         S_coag_N_agg_ = 0.5 * 1.82 * beta_fm * beta_cont / (beta_fm + beta_cont) * pow(N_agg(), 2.0) *
20         Av_ * rho;
21     }
22 }

```

3.17 Solving the transport equations

3.17.1 diffusionCoeff function

This function returns the diffusion coefficient of soot particles used in transport equations of tracked fields. The calculations are based on Equations 2.9-2.11.

lamiarSoot.H

```

1  virtual tmp<volScalarField> diffusionCoeff()
2  {
3      volScalarField mu (this->thermo().mu());
4      const volScalarField& T = this->thermo().T();
5      volScalarField f_gas_particle
6      (
7          3.0 * pi_ * mu * d_m_ /
8          ( 1.0 + 2.0 * lambda_gas() / d_m_ * (1.21 + 0.4*exp(-0.78*d_m_/lambda_gas()))))
9      );
10
11     f_gas_particle.max(SMALL);
12
13     return tmp<volScalarField>
14     (
15         new volScalarField
16         (
17             kB_ * T / f_gas_particle
18         )
19     )

```

```

19     );
20 }

```

3.17.2 updateSoot() function

This function deals with the transport equation of tracked fields by defining `tmp<fvScalarMatrix>` for each field and solving them. Below only `N_aggEqn` is shown, and the rest equations are treated in a similar way. Note that, `S_coag_N_agg_` is always negative, so this source term is added implicitly using `fvm::Sp` function to the equation matrix, but `S_inc_N_` is positive and added explicitly.

lamiarSoot.C

```

1  template<class ReactionThermo>
2  void Foam::combustionModels::laminarSoot<ReactionThermo>::updateSoot()
3  {
4      const surfaceScalarField& phi = this->phi();
5      const volScalarField D(diffusionCoeff());
6      volScalarField rho (this->thermo().rho());
7      fv::options& fvOptions(fv::options::New(this->mesh_));
8
9      // N_agg Equation
10     {
11         Info<< "N_agg Equation \n" << endl;
12         tmp<fvScalarMatrix> N_aggEqn
13         (
14             fvm::ddt(rho, N_agg_)
15             + fvm::div(phi, N_agg_)
16             - fvm::laplacian(D*rho, N_agg_)
17             ==
18             - fvm::Sp(rho * S_coag_N_agg_ /N_agg_, N_agg_)
19             + rho * S_inc_N_
20         );
21
22         N_aggEqn.ref().relax();
23         fvOptions.constrain(N_aggEqn.ref());
24         solve(N_aggEqn);
25         fvOptions.correct(N_agg_);
26     }
27     ...

```

3.18 Compiling the library

`wmake` compiles the library by building `laminarSoot.o` and linking it to the share combustion models library.

terminal output

```

1  wmake
2  ...
3  laminarSoot/laminarSoots.C -o /home/mo/OpenFOAM/OpenFOAM-v2006/build/linux64GccDPInt32Opt/src/
   combustionModels/laminarSoot/laminarSoots.o
4  ...
5  -L/home/mo/OpenFOAM/OpenFOAM-v2006/platforms/linux64GccDPInt32Opt/lib \
6  -lfiniteVolume -lmeshTools -lcompressibleTransportModels -lspecie -lfluidThermophysicalModels -
   lreactionThermophysicalModels -lchemistryModel -lturbulenceModels -lcompressibleTurbulenceModels
   -o /home/mo/OpenFOAM/OpenFOAM-v2006/platforms/linux64GccDPInt32Opt/lib/libcombustionModels.so

```

Chapter 4

Tutorial set up

4.1 Physics and Geometry

A 0D constant volume reactor case is designed to test `laminarSoot` combustion model. The geometry is a 2D $0.1\text{m} \times 0.1\text{m}$ closed box. The walls are assumed to be insulated ($\partial T / \partial x = 0$). The gas mixture inside the box is initially $T=1800\text{ K}$ and $P=10^5\text{ kPa}$ with the composition of $Y_{\text{C}_2\text{H}_4} = 0.2$, $Y_{\text{N}_2} = 0.8$. At this temperature, C_2H_4 decomposes through a set of chemical reactions and forms PAHs that generate soot particles inside the box. The residence time of gas is 400 ms (0.4 s). In other words, the simulation continues for 400 ms. There are no spatial gradients throughout the domain. Figure 4.1 shows schematics of the reactor with boundary names. The simple physics and small number of grid points offer advantages in term of (i) computational cost that could be enormous for reacting mixture considering 101 species transport equations (in case of ABF mechanism), and (ii) validation that will be done against the results of *EPTLSOOT* code developed by the author for modelling soot using low dimensional reactors based on Cantera [13] kinetic solver and Scipy [21] ODE integration libraries.

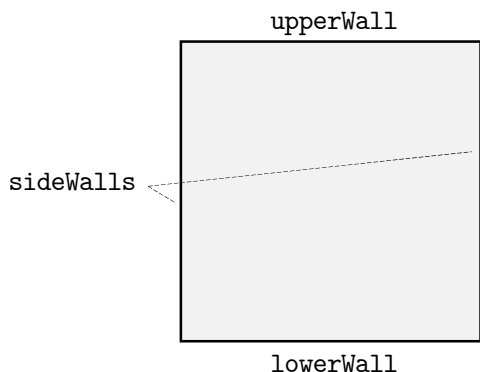


Figure 4.1: The schematics of reactor with boundary names

The mesh file, `reactor.msh`, is created by *Gambit*, and should be placed inside the case directory.

4.2 Combustion Model, Chemistry, and Thermophysical Properties

To utilize the new combustion model, user needs to set `combustionModel` to `laminarSoot` in `constant/combustionProperties`.

```
constant/combustionProperties
```

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "constant";
14     object        combustionProperties;
15 }
16 // ***** //
17
18 combustionModel  laminarSoot;
19
20 active  true;
21
22 laminarCoeffs
23 {
24 }
25
26 // ***** //

```

sootProperties also must be added to constant directory. The name of soot precursors, PAHs, is the only mandatory keyword, which is provided in the file.

constant/sootProperties

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "constant";
14     object        sootProperties;
15 }
16 // ***** //
17
18 PAHs (A2 A3 A4);
19
20 // ***** //

```

ABF mechanism [16] will be used for this simulation. The chemistry and thermodynamic files of this mechanism are available in Chemkin format, and need to be converted to foam chemistry and thermodynamic files using `chemkinToFoam` command. The mechanism conversion might pose challenges of its own such as duplicate species and discontinuous temperature ranges leading to errors in using `chemkinToFoam` that sometimes are not easy to interpret. Since the new combustion model library is the focus of this work, the details of mechanism conversion are not covered here and only the final files are provided in the project files. The chemistry (reaction) and thermodynamic properties are `reactions.ABF` and `thermo.ABF-mod`, respectively, and they are placed in `constant` directory. `thermophysicalProperties` contains the path to chemistry and thermodynamic files under `foamChemistryFile`, and `foamChemistryThermoFile`, respectively.

constant/thermophysicalProperties


```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "<constant>";
14     object        thermophysicalProperties;
15 }
16 // ***** //
17
18 thermoType
19 {
20     type          hePsiThermo;
21     mixture        reactingMixture;
22     transport      sutherland;
23     thermo         janaf;
24     energy         sensibleEnthalpy;
25     equationOfState perfectGas;
26     specie         specie;
27 }
28
29 inertSpecie N2;
30
31 chemistryReader foamChemistryReader;
32 foamChemistryFile "<constant>/reactions.ABF";
33 foamChemistryThermoFile "<constant>/thermo.ABF-mod";
34
35 // ***** //

```

4.3 Time Directory

4.3.1 Soot Fields

The first time directory, 0, must contain `N_agg`, `N_pri`, `C_tot`, and `H_tot` files that `laminarSoot` reads to determine initial and boundary conditions. The type of boundary conditions for soot fields are similar to species, which is `zeroGradient` on walls. The initial values are computed for one spherical soot particle per kg of gas mixture, which 2nm in diameter (with 378 carbon and 20 hydrogen atoms), as

$$N_{agg}^i = N_{pri}^i = \frac{1}{Av} = 1.66054 \times 10^{-24} \frac{mol}{kg}. \quad (4.1)$$

$$C_{tot}^i = \frac{378}{Av} = 6.27684 \times 10^{-22} \frac{mol}{kg}. \quad (4.2)$$

$$H_{tot}^i = \frac{20}{Av} = 3.32108 \times 10^{-23} \frac{mol}{kg}. \quad (4.3)$$

The contents of `N_agg` is provided below. `N_pri`, `C_tot`, and `H_tot` files are similar except for the object name and initial value, so they are included in Appendix B.

0/N_agg

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |

```

```

4 |  \ \  /  O peration   | Version:  v2006           |
5 |  \ \  /  A nd         | Website:  www.openfoam.com    |
6 |  \ \ /  M anipulation |                               |
7 |*-----*|
8 FoamFile
9 {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        N_agg;
15 }
16 // *****
17
18 dimensions      [-1 0 0 0 1 0 0];
19
20 internalField    uniform 1.66054e-24;
21
22 boundaryField
23 {
24     sideWalls
25     {
26         type      zeroGradient;
27     }
28     upperWall
29     {
30         type      zeroGradient;
31     }
32     lowerWall
33     {
34         type      zeroGradient;
35     }
36     frontAndBack
37     {
38         type empty;
39     }
40 }
41
42 // *****
43

```

4.3.2 Species

C2H4 and N2 contain the initial and boundary condition for mass fraction of C_2H_4 and N_2 , respectively. **zeroGradient** condition is applied on walls. The initial value is 0.2 for C_2H_4 , and 0.8 for N_2 consistent with the physics of the case explained in Section 4.1. The contents of *C2H4* and *N2* are given below.

0/C2H4

```

1 |*-----* C++ -*-----*|
2 |=====|
3 | \ \  /  F ield        | OpenFOAM: The Open Source CFD Toolbox |
4 | \ \  /  O peration    | Version:  v2006           |
5 | \ \  /  A nd          | Website:  www.openfoam.com    |
6 | \ \ /  M anipulation  |                               |
7 |*-----*|
8 FoamFile
9 {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        CH4;
15 }
16 // *****

```

```

17
18 dimensions      [0 0 0 0 0 0];
19
20 internalField    uniform 0.2;
21
22 boundaryField
23 {
24     sideWalls
25     {
26         type      zeroGradient;
27     }
28     upperWall
29     {
30         type      zeroGradient;
31     }
32     lowerWall
33     {
34         type      zeroGradient;
35     }
36     frontAndBack
37     {
38         type empty;
39     }
40 }
41
42
43 // *****

```

O/N2

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F ield | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O peration | Version: v2006 |
5  | \ \ / A nd | Website: www.openfoam.com |
6  | \ \ / M anipulation |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        N2;
15 }
16 // *****
17 dimensions      [0 0 0 0 0 0];
18 internalField    uniform 0.8;
19 boundaryField
20 {
21     sideWalls
22     {
23         type      zeroGradient;
24     }
25     upperWall
26     {
27         type      zeroGradient;
28     }
29     lowerWall
30     {
31         type      zeroGradient;
32     }
33     frontAndBack
34     {
35         type empty;
36     }
37 }

```

Table 4.1: The initial values and boundary conditions for temperature, pressure and velocity

Quantity	Filename	Initial Value	Boundary condition
Temperature	T	1800	zeroGradient
Velocity	U	(0 0 0)	zeroGradient
Pressure	p	1e5	zeroGradient
C ₂ H ₄	C2H4	0.2	zeroGradient
N ₂	N2	0.8	zeroGradient

The solver uses `Ydefault` as initial and boundary condition for all the rest of species that are not included in `O` directory. The boundary conditions are identical to C₂H₄ and N₂, but the initial value is `uniform 0`. `Ydefault` is included in Appendix B.

4.3.3 Temperature, Pressure, and Velocity

The initial values for `T` and `p` are 1800 and 1e5, respectively. `U` is uniformly zero. The boundary condition is `zeroGradient` on walls for all three fields. The initial values and boundary conditions are listed in Table 4.1

4.4 System Directory

`controlDict` is modified to set `endTime` to 0.04s according to the residence time discussed in Section 4.1. The simulation time step, `deltaT`, is set to 10^{-5} s.

```

system/controlDict
1  /*-----* C++ *-----*/
2  | ===== |
3  | \ \      / F ield      | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \      / O peration  | Version: v2006 |
5  | \ \      / A nd        | Website: www.openfoam.com |
6  | \ \      / M anipulation | |
7  \*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "system";
14     object        controlDict;
15 }
16 // *****
17 application      reactingFoam;
18 startFrom        latestTime;
19 startTime        0;
20 stopAt           endTime;
21 endTime          0.04;
22 deltaT           1e-5;
23 writeControl      adjustable;
24 writeInterval     0.001;
25 purgeWrite       0;
26 writeFormat       ascii;
27 writePrecision    7;
28 writeCompression off;
29 timeFormat        general;
30 timePrecision     6;
31 runTimeModifiable true;
32 adjustTimeStep    no;
33 maxCo             0.1;
34 functions{
35     #include "probes"

```

```

36 }
37 // *****

```

`probe` object functions are included are the end of `controlDict` to collect data for validation with the benchmark code.

system/probes

```

1 probes
2 {
3     type          probes;
4     libs          (sampling);
5     name          probes;
6     writeControl   outputTime;
7     writeInterval  1;
8     fields         (N_agg N_pri C_tot H_tot);
9     interpolationScheme cellPoint;
10    probeLocations
11    (
12        ( 0.05 0.05 0.005 )
13    );
14    sampleOnExecute yes;
15 }

```

The convection terms in transport equations of soot fields are discretized using `limitedLinear` scheme. The soot fields are solved using `PBiCGStab` solver with `DILU` preconditioner and tolerance of 10^{-6} and relative tolerance of 0.1 (see `fvSchemes` and `fvSolution` in Appendix B).

4.5 Running and Post-processing

`Allrun` takes care of all running step including (i) sourcing OpenFOAM (ii) converting `reactor.msh` to OpenFOAM-readable format mesh (iii) decomposing the domain for six processor (iv) running `reactingFoam`, (iv) reconstructing the processor data, and (v) post processing using `postProcess.py` that reads benchmark data of EPTLSOOT and generates the plots and saves them in `figures` directory. As shown in Figure 4.2, the soot fields obtained by `laminarSoot` are in excellent agreement with the results of EPTLSOOT indicating the accuracy of the developed library. The mass fraction of key species involved in soot formation is shown Figure 4.3 that demonstrates a good agreement between OpenFOAM and EPTLSOOT results.

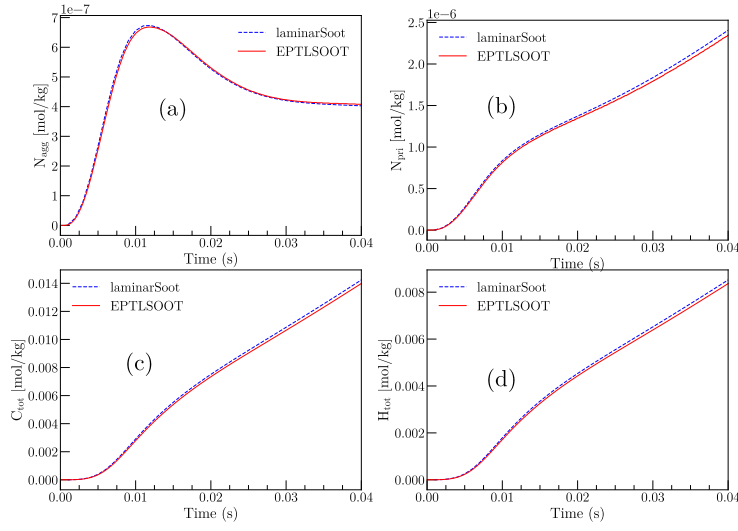


Figure 4.2: The comparison of (a) N_{agg} (b) N_{pri} (c) C_{tot} (d) H_{tot} obtained by laminarSoot with those of EPTLSOOT code

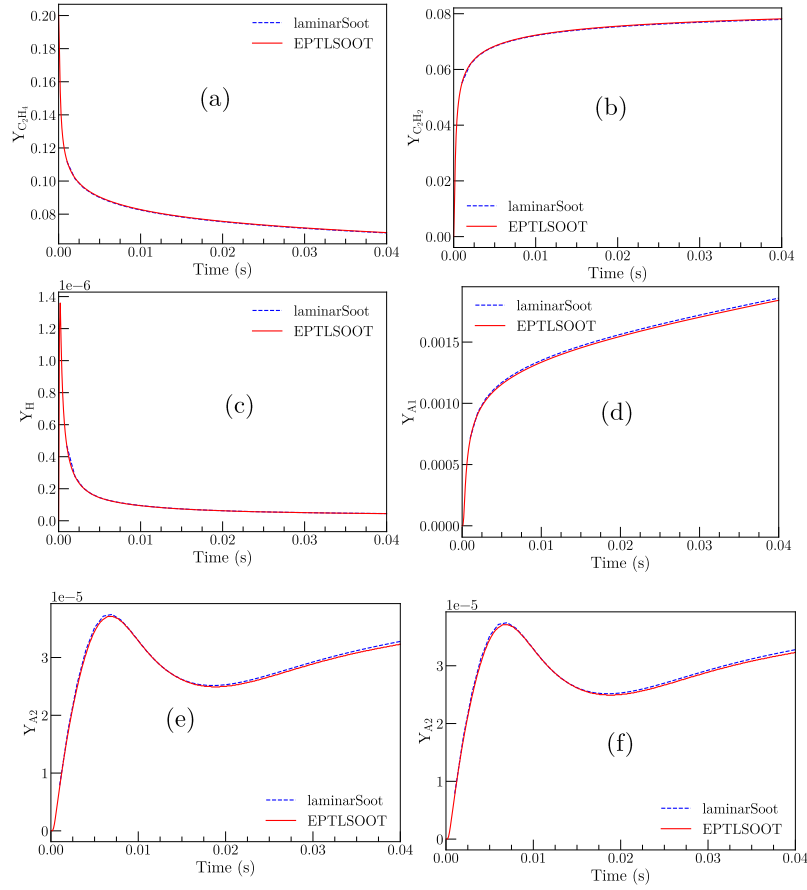


Figure 4.3: The comparison of mass fraction of a) C_2H_4 (b) C_2H_2 (c) H (d) Al (e) A_2 (f) A_4 obtained by laminarSoot with those of EPTLSOOT code

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Study questions

1. What information are transferred from `laminar` combustion model to `reactingFoam` solver?
2. How reaction rates and heat release from chemical reactions in gas mixture are modified to consider the impact of soot formation?
3. How `laminarSoot` library is selected in a case?
4. What is the purpose of `correct()` function in the combustion model?

Appendix A

Appendix: Source Code

A.1 HACA-growth functions

```
laminarSoot.H

1  // HACA Rate
2  virtual tmp<volScalarField> k_4_HACA()
3  {
4      const volScalarField& T = this->thermo().T();
5      dimensionedScalar oneKelvin(dimTemperature, scalar(1.0));
6      dimensionedScalar k_unit(dimensionSet(0,3,-1,0,-1,0,0), scalar(1.0));
7      return tmp<volScalarField>
8      (
9          new volScalarField
10         (
11             "k_4_HACA",
12             (k_unit * 8.00e1 * pow(T/oneKelvin, 1.56) * exp(oneKelvin * (-1912.43) / T))
13         )
14     );
15 }
16 virtual tmp<volScalarField> k_5_HACA()
17 {
18     const volScalarField& T = this->thermo().T();
19     dimensionedScalar oneKelvin(dimTemperature, scalar(1.0));
20     dimensionedScalar k_unit(dimensionSet(0,3,-1,0,-1,0,0), scalar(1.0));
21     return tmp<volScalarField>
22     (
23         new volScalarField
24         (
25             "k_5_HACA",
26             (k_unit * 2.20e6 * exp(oneKelvin * (-3774.53) / T))
27         )
28     );
29 }
30 virtual tmp<volScalarField> k_6_HACA()
31 {
32     const volScalarField& T = this->thermo().T();
33     dimensionedScalar oneKelvin(dimTemperature, scalar(1.0));
34     dimensionedScalar k_unit(dimensionSet(0,3,-1,0,-1,0,0), scalar(1.0));
35     return tmp<volScalarField>
36     (
37         new volScalarField
38         (
39             "k_6_HACA",
40             (k_unit * 0.13e0 * pow(T/oneKelvin, 0.0))
41         )
42     );
43 }
44 virtual tmp<volScalarField> C_soot_0()
```

```

45     {
46         // Species indicies
47         label H_i = speciesIndicies_["H"];
48         label OH_i = speciesIndicies_["OH"];
49         label H2_i = speciesIndicies_["H2"];
50         label H2O_i = speciesIndicies_["H2O"];
51         label C2H2_i = speciesIndicies_["C2H2"];
52         label O2_i = speciesIndicies_["O2"];
53
54         const volScalarField& T = this->thermo().T();
55         volScalarField rho (this->thermo().rho());
56
57         dimensionedScalar oneKelvin(dimTemperature, scalar(1.0));
58         dimensionedScalar k_unit(dimensionSet(0,3,-1,0,-1,0,0), scalar(1.0));
59
60         // Forward Reaction Rates
61         // Units : m3/mol-s
62         volScalarField k_1(k_unit * 4.17e7 * exp(oneKelvin * (-6542.52) / T));
63         volScalarField k_2(k_unit * 1.00e4 * pow(T/oneKelvin, 0.734) * exp(oneKelvin * (-719.68) /
T));
64         volScalarField k_3(k_unit * 2.00e7 * pow(T/oneKelvin, 0.0));
65
66         // Reverse Reaction Rates
67         // Units : m3/mol-s
68         volScalarField k_r_1(k_unit * 3.9e6 * exp(oneKelvin * (-5535.98) / T));
69         volScalarField k_r_2(k_unit * 3.68e2 * pow(T/oneKelvin, 1.139) * exp(oneKelvin *
(-8605.94) / T));
70
71         // chi_soot_0
72         // dimensionedScalar chi_soot_0_denum_limit("chi_soot_0_denum_limit",dimless/dimTime,
scalar(1e-20));
73         volScalarField chi_soot_0_denum
74         (
75             max
76             (
77                 k_r_1 * C(H2_i) + k_r_2 * C(H2O_i) + k_3 * C(H_i) + k_4_HACA() * C(C2H2_i) +
k_5_HACA() * C(O2_i) + k_1 * C(H_i) + k_2 * C(OH_i),
78                 dimensionedScalar(dimless/dimTime, SMALL)
79             )
80         );
81
82         dimensionedScalar chi_soot_CH(dimensionSet(0,-2,0,0,0,0,0), scalar(2.3e19));
83         //
84         volScalarField chi_soot_0
85         (
86             (k_1 * C(H_i) + k_2 * C(OH_i)) / chi_soot_0_denum * chi_soot_CH
87         );
88
89         // C_soot_0
90         // unit: mol/m3
91         return tmp<volScalarField>
92         (
93             new volScalarField
94             (
95                 "C_soot_0",
96                 (A_tot_ / Av_ * chi_soot_0) * rho
97             )
98         );
99     }
100
101     virtual tmp<volScalarField> alpha()
102     {
103         dimensionedScalar oneKelvin(dimTemperature, scalar(1.0));
104         dimensionedScalar alpha_min(dimless, scalar(0.0));
105         dimensionedScalar alpha_max(dimless, scalar(1.0));
106         const volScalarField& T = this->thermo().T();
107         return tmp<volScalarField>
108         (

```

```
109         new volScalarField
110         (
111             min
112             (
113                 max
114                 (
115                     tanh
116                     (
117                         (12.56 - 0.00563 * T / oneKelvin) / log10 ( rho_soot_ * pi_ / 6.0 *
pow(d_p_, 3.0) * Av_ / W_carbon_ ) -
118                         1.38 + 0.00068 * T / oneKelvin
119                     ),
120                     alpha_min
121                 ),
122                 alpha_max
123             )
124         );
125     }
126 }
```

Appendix B

Appendix: Simulation case files

B.1 0 directory

```
                                O/N_pri
1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        N_pri;
15 }
16 // ***** //
17
18 dimensions      [-1 0 0 0 1 0 0];
19
20 internalField    uniform 1.66054e-24;
21
22 boundaryField
23 {
24     sideWalls
25     {
26         type      zeroGradient;
27     }
28     upperWall
29     {
30         type      zeroGradient;
31     }
32     lowerWall
33     {
34         type      zeroGradient;
35     }
36     frontAndBack
37     {
38         type      empty;
39     }
40 }
41
42
43 // ***** //
```

0/C_tot

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        C_tot;
15 }
16 // ***** //
17
18 dimensions      [-1 0 0 0 1 0 0];
19
20 internalField    uniform 6.27684e-22;
21
22 boundaryField
23 {
24     sideWalls
25     {
26         type      zeroGradient;
27     }
28     upperWall
29     {
30         type      zeroGradient;
31     }
32     lowerWall
33     {
34         type      zeroGradient;
35     }
36     frontAndBack
37     {
38         type empty;
39     }
40 }
41
42
43 // ***** //

```

0/H_tot

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ M a n i p u l a t i o n |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         volScalarField;
13     location      "0";
14     object        H_tot;
15 }
16 // ***** //
17
18 dimensions      [-1 0 0 0 1 0 0];
19
20 internalField    uniform 3.32108e-23;

```

```

21
22 boundaryField
23 {
24     sideWalls
25     {
26         type            zeroGradient;
27     }
28     upperWall
29     {
30         type            zeroGradient;
31     }
32     lowerWall
33     {
34         type            zeroGradient;
35     }
36     frontAndBack
37     {
38         type empty;
39     }
40 }
41
42
43 // ***** //

```

0/Ydefault

```

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n | |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format       ascii;
12     class        volScalarField;
13     location     "0";
14     object       Ydefault;
15 }
16 // ***** //
17
18 dimensions      [0 0 0 0 0 0 0];
19
20 internalField    uniform 0.0;
21
22 boundaryField
23 {
24     sideWalls
25     {
26         type            zeroGradient;
27     }
28     upperWall
29     {
30         type            zeroGradient;
31     }
32     lowerWall
33     {
34         type            zeroGradient;
35     }
36     frontAndBack
37     {
38         type empty;
39     }
40 }
41
42

```

```
43 // ***** //
```

B.2 system directory

```

                                system/fvSchemes
1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n | |
7  /*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "system";
14     object        fvSchemes;
15 }
16 // ***** //
17
18 ddtSchemes
19 {
20     default      Euler;
21 }
22
23 gradSchemes
24 {
25     default      Gauss linear;
26 }
27
28 divSchemes
29 {
30     default      none;
31
32     div(phi,U)    Gauss limitedLinearV 1;
33     div(phi,Yi_h) Gauss limitedLinear 1;
34     div(phi,K)    Gauss limitedLinear 1;
35     div(phiid,p)  Gauss limitedLinear 1;
36     div(phi,epsilon) Gauss limitedLinear 1;
37     div(phi,k)    Gauss limitedLinear 1;
38     div(phi,N_agg) Gauss limitedLinear 1;
39     div(phi,N_pri) Gauss limitedLinear 1;
40     div(phi,C_tot) Gauss limitedLinear 1;
41     div(phi,H_tot) Gauss limitedLinear 1;
42     div(((rho*nuEff)*dev2(T(grad(U))))) Gauss linear;
43 }
44
45 laplacianSchemes
46 {
47     default      Gauss linear orthogonal;
48 }
49
50 interpolationSchemes
51 {
52     default      linear;
53 }
54
55 snGradSchemes
56 {
57     default      orthogonal;
58 }
59
```



```

60 // *****
61 // *****

system/fvSolutions

1  /*----- C++ -----*/
2  | ===== |
3  | \ \ / F i e l d | OpenFOAM: The Open Source CFD Toolbox |
4  | \ \ / O p e r a t i o n | Version: v2006 |
5  | \ \ / A n d | Website: www.openfoam.com |
6  | \ \ / M a n i p u l a t i o n | |
7  \*-----*/
8  FoamFile
9  {
10     version      2.0;
11     format        ascii;
12     class         dictionary;
13     location      "system";
14     object        fvSolution;
15 }
16 // *****
17
18 solvers
19 {
20     "rho.*"
21     {
22         solver      diagonal;
23     }
24
25     p
26     {
27         solver      PCG;
28         preconditioner DIC;
29         tolerance    1e-6;
30         relTol       0.1;
31     }
32
33     pFinal
34     {
35         $p;
36         tolerance    1e-6;
37         relTol       0.0;
38     }
39
40     "(U|h|k|epsilon|N_agg|N_pri|C_tot|H_tot)"
41     {
42         solver      PBiCGStab;
43         preconditioner DILU;
44         tolerance    1e-6;
45         relTol       0.1;
46     }
47
48     "(U|h|k|epsilon|N_agg|N_pri|C_tot|H_tot)Final"
49     {
50         $U;
51         relTol       0;
52     }
53
54     Yi
55     {
56         $hFinal;
57     }
58 }
59
60 PIMPLE
61 {
62     momentumPredictor no;
63     nOuterCorrectors 1;

```

```
64     nCorrectors      2;  
65     nNonOrthogonalCorrectors 0;  
66 }  
67  
68 // ***** //  

```