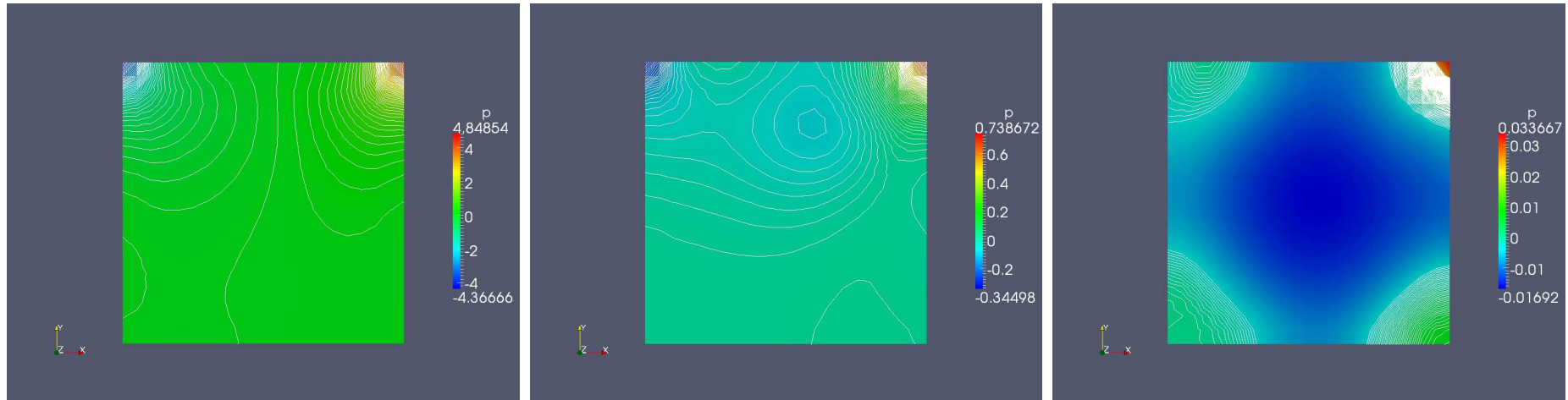


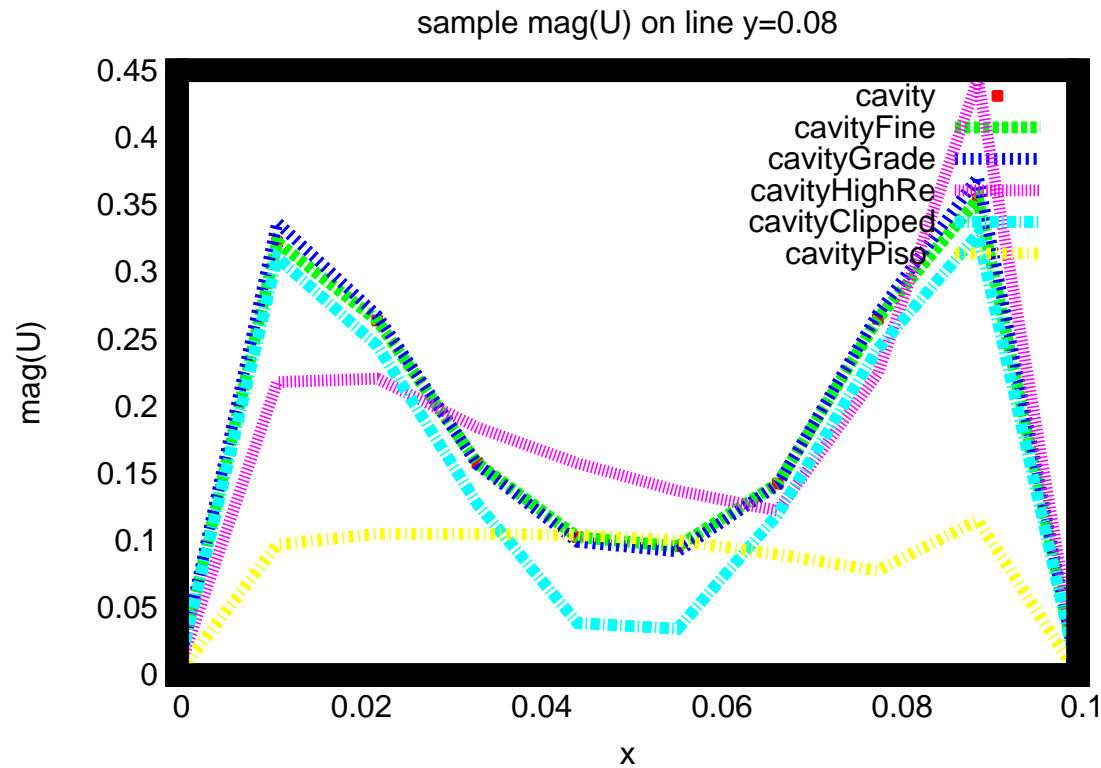
# OpenFOAM Tutorials

## Case: Cavity - Solver: icoFoam/pisoFoam



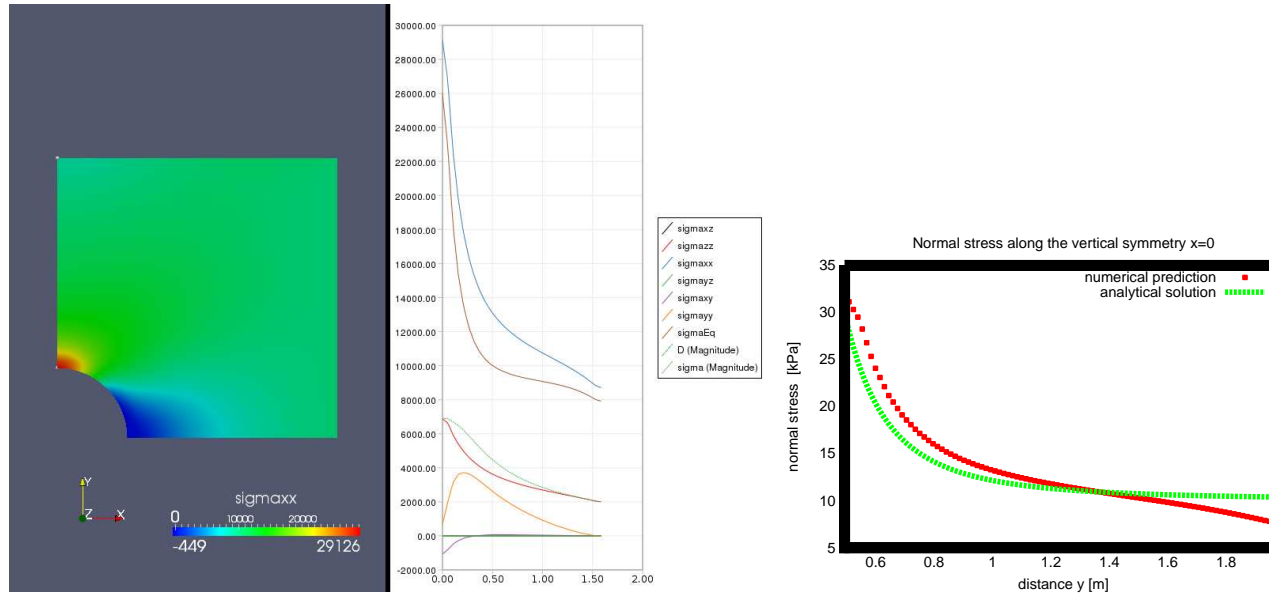
Pressure contour for the cases cavity and cavityHighRe solved with icoFoam and cavityHighRe solved with pisoFoam

## Case: Cavity\*



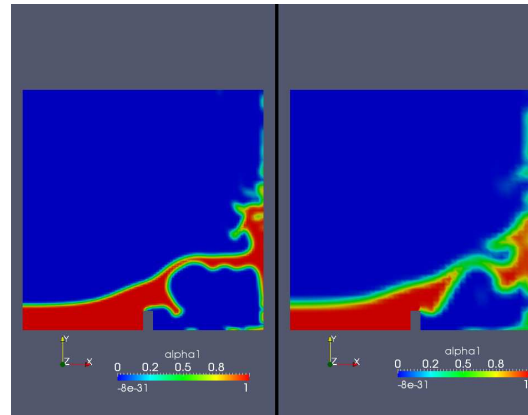
Velocity magnitude along the line  $y=0.08$  for all the cavity cases

## Case: PlateHole - Solver: solidDisplacementFoam

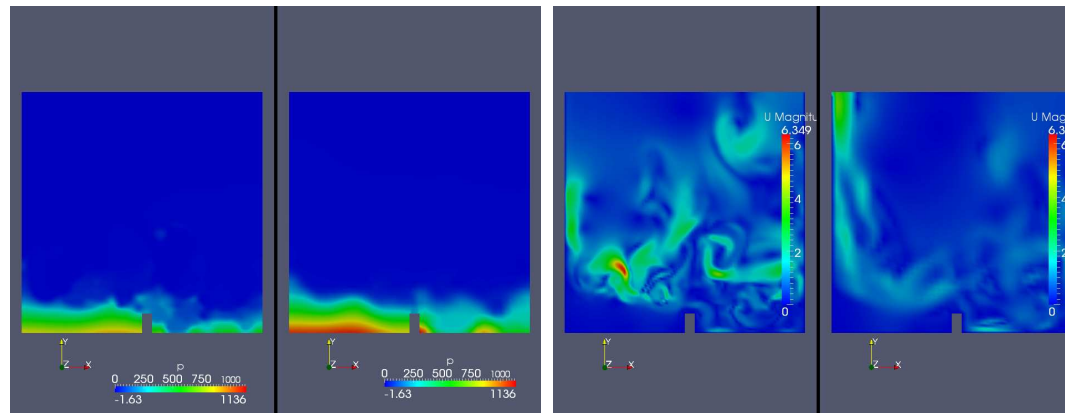


Stress along the line  $x=0$ . postprocessing with Paraview and Gnuplot

## Case: damBreak - Solver :interFoam laminar



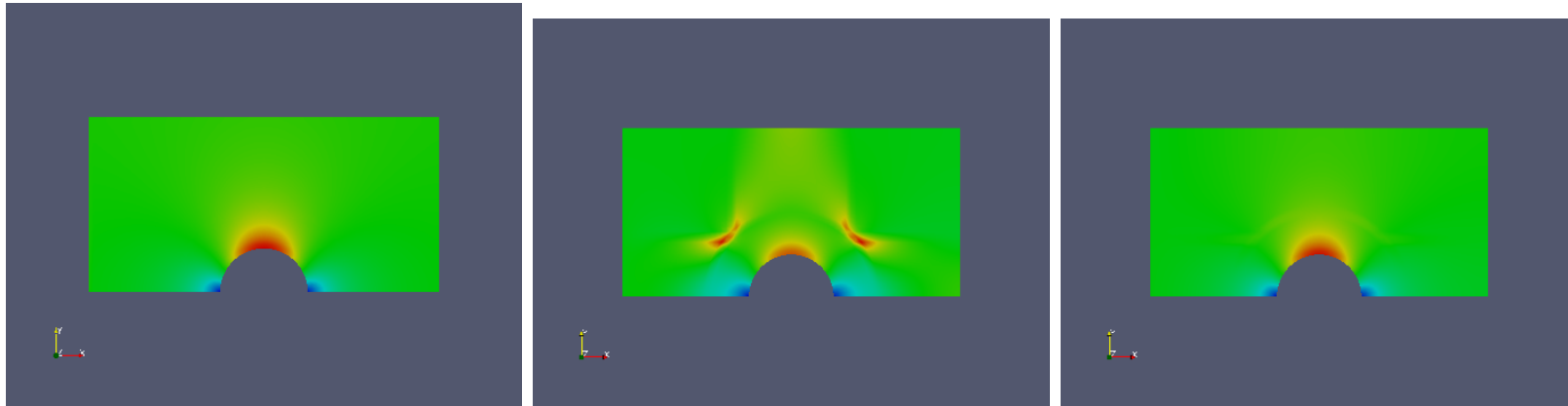
alpha at  $t=0.5$  with a fine and a coarse mesh



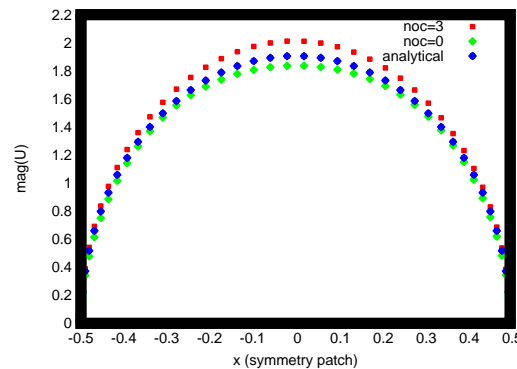
pressure and velocity at  $t=1$  with a fine and a coarse mesh

## Case: Cylinder - Solver: potentialFoam

Add `UA.write()` at the end of `analyticalCylinder.C` to write the vector `UA` in each time step directory.

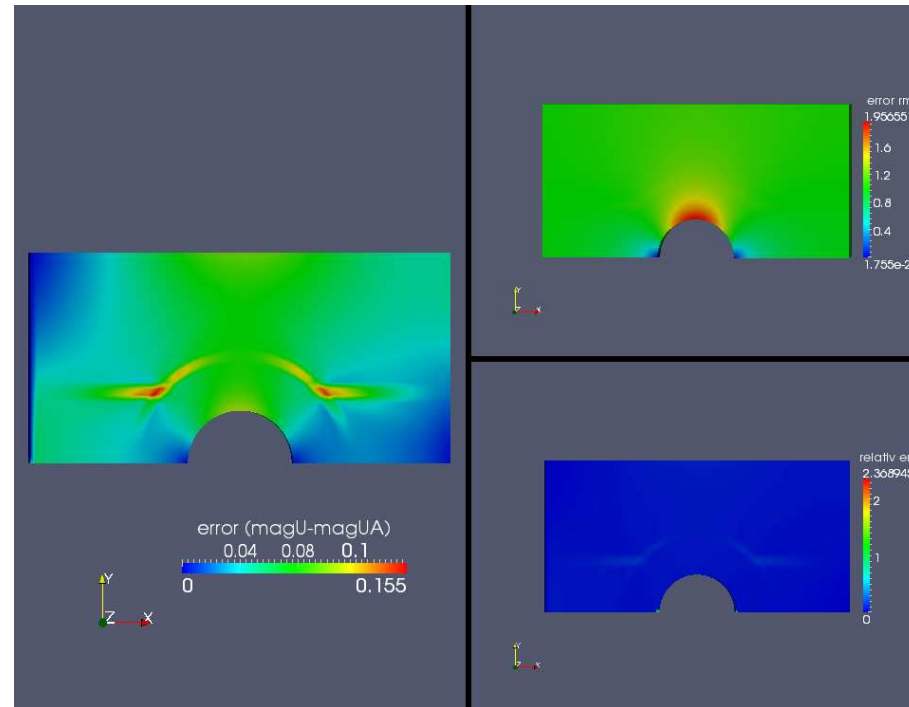


velocity profile of the analytical solution, the solution with 0 (resp 3) non orthogonal corrector



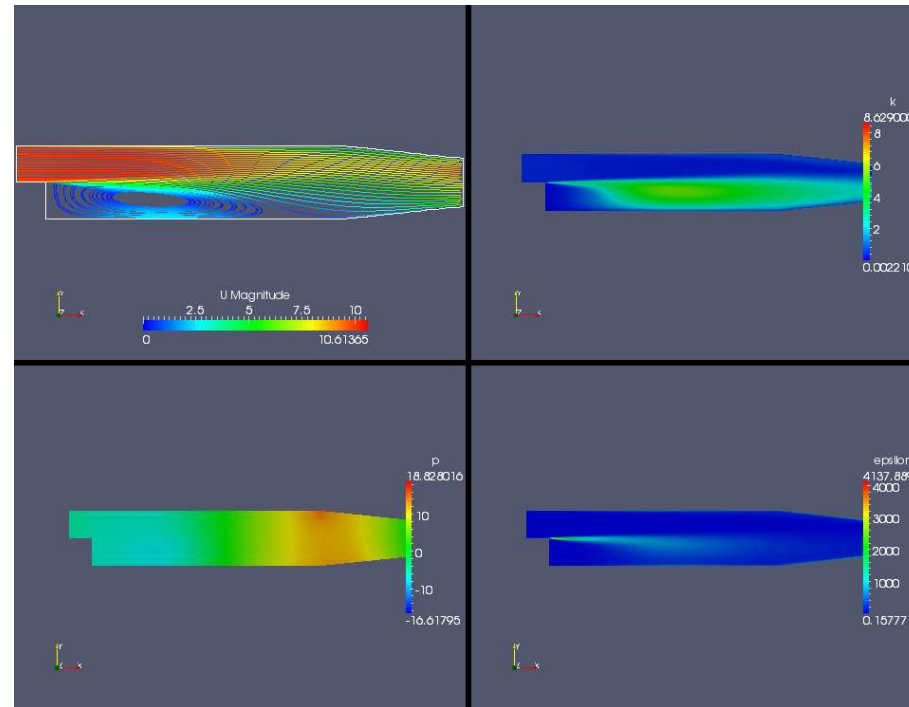
velocity profile on the symmetry patch. Postprocessing with gnuplot

## Case: Cylinder - Solver: potentialFoam



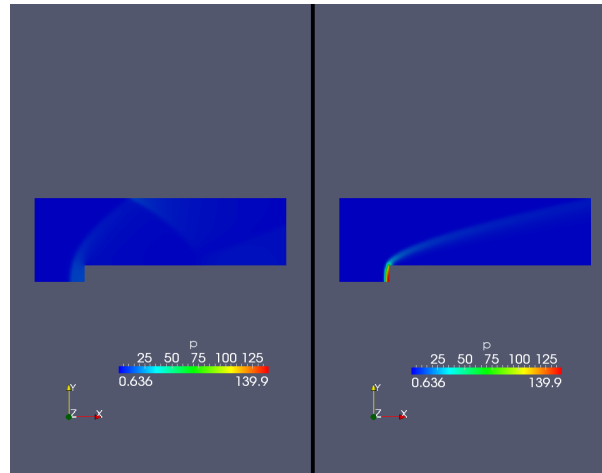
numerical error on the velocity field

## Case: pitzDaily - Solver: simpleFoam



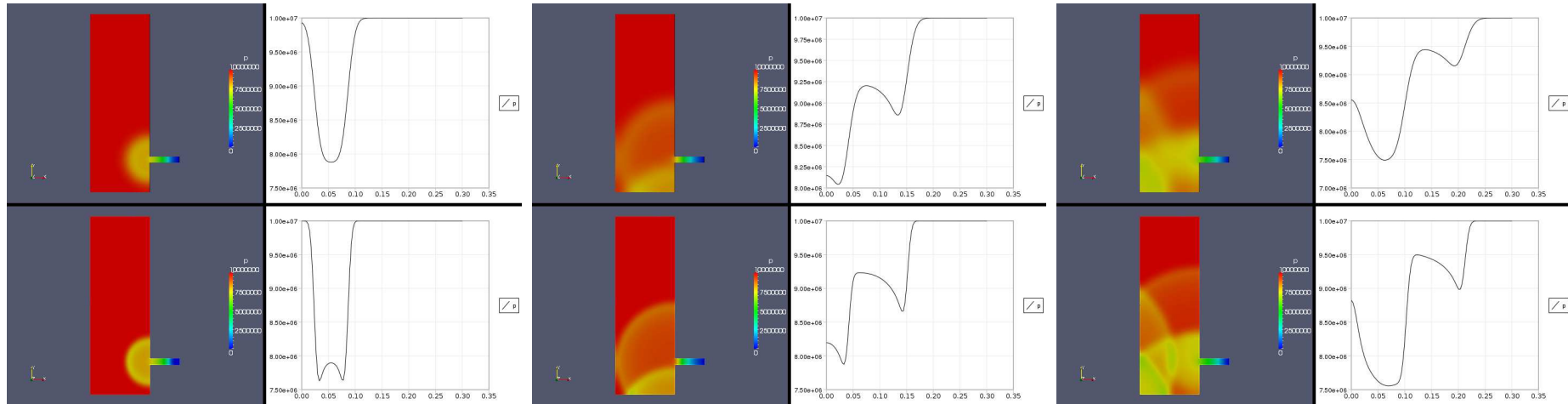


## Case: forwardStep - Solver: sonicFoam



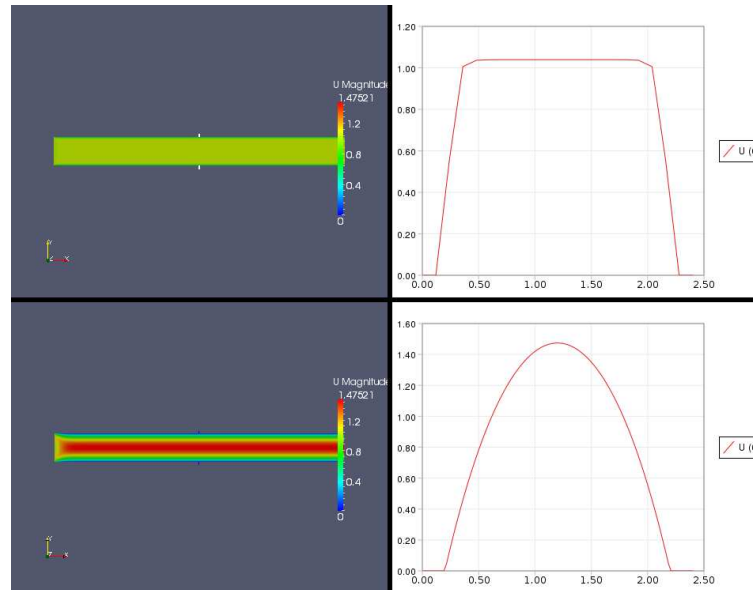
pressure field at  $t=10s$  with inlet velocity=3 and 10 m/s

## Case: decompressionTank - Solver: sonicLiquidFoam



fine and coarse grid.  $t=6e-5$ ,  $1e-4$  and  $1.5e-4$ . Pressure along a line  $x=\text{constant}$

## Case: hartmann - Solver: mhdFoam



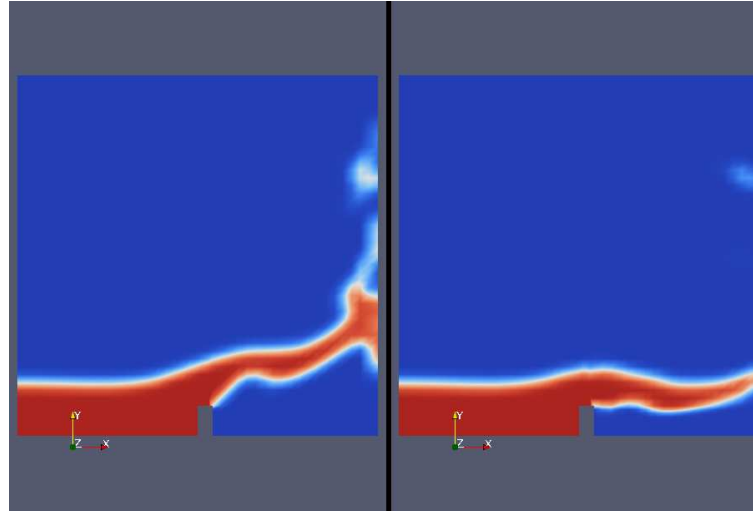
B=1 and 20.  $U_x$  along a line  $y=\text{constant}$

## Case: damBreak modified = damBreakOpen - Solver: interFoam

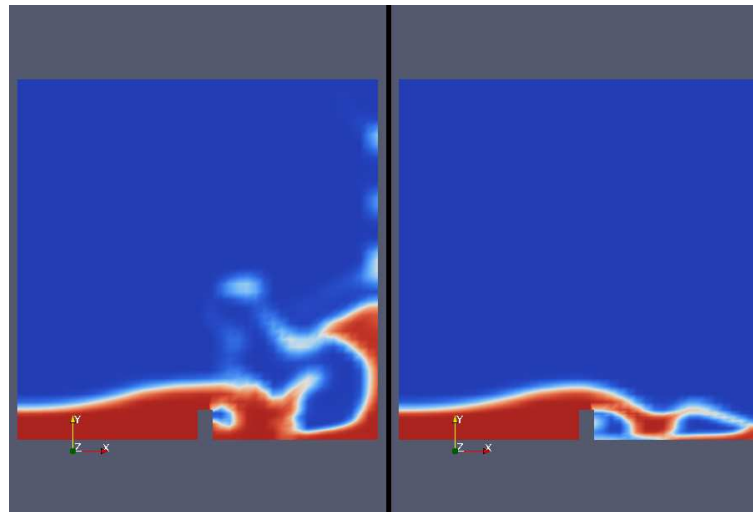
The boundary "rightWall" with type wall is changed to type patch in polyMesh/boundary. The velocity boundary condition in 0/ is changed to zeroGradient, and for the pressure, totalPressure is used, similarly to the upper patch called "atmosphere". Now the liquid phase can escape the domain. The total volume fraction of the liquid phase in the domain is computed at each time step. We simply write an utility to print out alphaTot/volume

```
forAll(mesh.cells(),celli)
{
    alphaTot=alphaTot+alpha[celli]*mesh.V()[celli];
    volume=volume+mesh.V()[celli];
}
```

The results are in the table. We clearly see that the liquid phase escapes the domain for the case damBreakOpen as the volume fraction of the liquid phase decreases. It should be constant for the initial case damBreak. It is actually constant until  $t = 0.4$ , when the liquid phase hits the boundary "rightWall" which produces small bubbles and numerical errors. VOF method introduces some values of  $\alpha < 0$  and  $> 1$  that are later bounded in  $[0, 1]$ .



Liquid phase at  $t=0.4$ . Case damBreak and damBreakOpen



Liquid phase at  $t=0.65$ . Case damBreak and damBreakOpen

Time	damBreak	damBreakOpen
0	0.130194	0.130194
0.1	0.130194	0.130194
0.2	0.130194	0.130194
0.3	0.130194	0.130194
0.4	0.130185	0.113
0.5	0.129592	0.0986771
0.6	0.129562	0.085936
0.7	0.129557	0.0764507
0.8	0.129556	0.0717916
0.9	0.129556	0.0650988
1	0.129497	0.0600475

Liquid phase total volume fraction